Cenovus Christina Lake In-situ oil sands scheme 8591 2015 update

Subsurface June 15, 2016





Oil & gas and financial information

Oil & gas information

The estimates of reserves and contingent resources were prepared effective December 31, 2015 and the estimates of bitumen initially-in-place were prepared effective December 31, 2012. All estimates were prepared by independent qualified reserves evaluators, based on definitions contained in the Canadian Oil and Gas Evaluation Handbook and in accordance with National Instrument 51-101. Additional information with respect to the significant factors relevant to the resources estimates, the specific contingencies which prevent the classification of the contingent resources as reserves, pricing and additional reserves and other oil and gas information, including the material risks and uncertainties associated with reserves and resources estimates, is contained in our AIF and Form 40-F for the year ended December 31, 2015, available on SEDAR at www.sedar.com, EDGAR at www.sec.gov and on our website at cenovus.com.

There is uncertainty that it will be commercially viable to produce any portion of the contingent resources. There is no certainty that any portion of the prospective resources will be discovered. If discovered, there is no certainty that it will be commercially viable to produce any portion of those resources. Actual resources may be greater than or less than the estimates provided.

Total bitumen initially-in-place (BIIP) estimates, and all subcategories thereof, including the definitions associated with the categories and estimates, are disclosed and discussed in our July 24, 2013 news release, available on SEDAR at sedar.com and at cenovus.com. BIIP estimates include unrecoverable volumes and are not an estimate of the volume of the substances that will ultimately be recovered. Cumulative production, reserves and contingent resources are disclosed on a before royalties basis. All estimates are best estimate, billion barrels (Bbbls). *Total BIIP* (143 Bbbls); *discovered BIIP* (143 Bbbls); *discovered BIIP* equals the *cumulative production* (0.1 Bbbls) plus *reserves* (2.4 Bbbls); *sub-commercial discovered BIIP* equals economic contingent resources (9.6 Bbbls); prospective resources (8.5 Bbbls); *unrecoverable portion of discovered BIIP* (42 Bbbls). Any contingent resources as at December 31, 2012 that are sub-economic or that are classified as being subject to technology under development have been grouped into the unrecoverable portion of discovered BIIP. Petroleum initially-in-place (PIIP) estimates for Pelican Lake are effective December 31, 2012 and were prepared by McDaniel. All estimates are best estimate discovered PIIP volumes as follows: *Mobile Wabiskaw* total PIIP (2.11 Bbbls); cumulative production (0.11 Bbbls); reserves (0.25 Bbbls); unrecoverable protucion (0.11 Bbbls); unrecoverable discovered PIIP (1.72 Bbbls); undiscovered PIIP (1.62 Bbbls); unrecoverable resources (0.03 Bbbls); unrecoverable discovered PIIP (1.72 Bbbls); undiscovered PIIP (0 Bbbls). *Mobile Wabiskaw development area* total PIIP (0 Bbbls). *Immobile Wabiskaw* total PIIP (1.33 Bbbls); unsecoverable PIIP (1.33 Bbbls); unculative production (0 Bbbls); reserves (0 Bbbls); undiscovered PIIP (0 Bbbls); uncoverable discovered PIIP (1.33 B

Certain natural gas volumes have been converted to barrels of oil equivalent (BOE) on the basis of one barrel (bbl) to six thousand cubic feet (Mcf). BOE may be misleading, particularly if used in isolation. A conversion ratio of one bbl to six Mcf is based on an energy equivalency conversion method primarily applicable at the burner tip and does not represent value equivalency at the well head.

Non-GAAP measures

Certain financial measures in this document do not have a standardized meaning as prescribed by IFRS such as, Operating Cash Flow, Cash Flow, Operating Earnings, Free Cash Flow, Debt, Net Debt, Capitalization and Adjusted Earnings before Interest, Taxes, Depreciation and Amortization ("Adjusted EBITDA") and therefore are considered non-GAAP measures. These measures may not be comparable to similar measures presented by other issuers. These measures have been described and presented in order to provide shareholders and potential investors with additional measures for analyzing our ability to generate funds to finance our operations and information regarding our liquidity. This additional information should not be considered in isolation or as a substitute for measures prepared in accordance with IFRS. Readers are encouraged to review our most recent Management's Discussion and Analysis, available at cenovus.com for a full discussion of the use of each measure.

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Advisory

This presentation contains information in compliance with:

AER Directive 054 - Performance Presentations, Auditing, and Surveillance of In Situ Oil Sands Schemes

This document contains forward-looking information prepared and submitted pursuant to Alberta regulatory requirements and is not intended to be relied upon for the purpose of making investment decisions, including without limitation, to purchase, hold or sell any securities of Cenovus Energy Inc. The resources estimates contained herein are not reported in accordance with National Instrument 51-101 and are provided solely for the purpose of complying with Alberta regulatory requirements.

Additional information regarding Cenovus Energy Inc., including information regarding contingent resources, is available in our Annual Information Form for the year ended December 31, 2015 and in our Statement of Contingent and Prospective Resources for the year ended December 31, 2015 at cenovus.com.





Subsection 3.1.1-1) Brief background





About Cenovus

TSX, NYSE | CVE

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Enterprise value	C\$18 billion
Shares outstanding	833 million
2016F production	
Oil sands	151 Mbbls/d
Conventional	54 Mbbls/d
Total liquids	205 Mbbls/d
Natural gas	385 MMcf/d
Total production	269 MBOE/d
••	
2015 proved & probable reserves	3.8 BBOE
2015 proved & probable reserves Bitumen	3.8 BBOE
2015 proved & probable reserves Bitumen Economic contingent resources*	3.8 BBOE 9.3 Bbbls
2015 proved & probable reserves Bitumen Economic contingent resources* Lease rights**	3.8 BBOE 9.3 Bbbls 2.0 MM net acres
2015 proved & probable reserves Bitumen Economic contingent resources* Lease rights** P&NG rights	3.8 BBOE 9.3 Bbbls 2.0 MM net acres 4.1 MM net acres

Values are approximate. Forecast production based on February 11, 2016 guidance. *See advisory. **Includes an additional 0.5 million net acres of exclusive lease rights to lease on our behalf and our assignee's behalf.



Major scheme/project updates

- Q1 2000 EUB project approval
- Q2 2002 First steam of phase A pilot
- Q4 2005 Approval of phase B expansion
- Q2 2008 Phase B expansion first steam
- Q3 2008 Approval of phase C/D amendment
- Q2 2011 Approval of phase E/F/G EIA application
- Q2 2011 Phase C expansion first steam
- Q2 2012 Phase D expansion first steam
- Q4 2012 Approval of phase F and G amendment
- Q4 2013 CDE Debottleneck amendment
- Q4 2015 Approval of phase H and eastern expansion amendment
- Q4 2015 CDE Debottleneck first steam



Recovery process

- The Christina Lake Thermal Project uses the dual-horizontal well SAGD (steam-assisted gravity drainage) process to recover oil from the McMurray formation
- Two horizontal wells one above the other approximately 5 m apart
- Steam is injected into the upper well where it heats the oil and allows it to drain into the lower well
- Oil and water emulsion pumped to the surface and treated





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Area Map



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Scheme Map



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AER Approved Project Area

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Drilled SAGD Wells as of March 31, 2016





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Commercial SAGD Wells as of March 31, 2016





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Source and Disposal Wells as of March 31, 2016



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Note: MW1 & MW4 are not in use yet, but will be by year end for Phase F

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Subsection 3.1.1 – 2) Geology and Geoscience

Brant Skibsted Geologist





SAGD Pay Iso- CHLK Proper



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AER Approved Project Area

Reservoir Properties (project area)

Reservoir depth:	350m TVD	
Original reservoir pressure:	2500 kPa	
Original reservoir temperature:	12°C	
Average Vertical permeability:	4.2 Darcies	
Average Horizontal permeability:	7.0 Darcies	
Average SAGD pay:	21 meters	
Average porosity (Ø):	33%	
Average oil saturation:	80%	
<i>Rock Volume: 1,925 x 10</i> ⁶ m ³		
<i>SOIP: 508 x 10</i> ⁶ m ³		
Note: CVE Volumetric Estimates, not IQRE estimates		

SOIP = Rock Volume in Project area x phi (.33) x So (.80)

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AER Approved Project Area

Reservoir Properties (project area)

Reservoir depth:	350m TVD	
Original reservoir pressure:	2500 kPa	
Original reservoir temperature:	12°C	
Average Vertical permeability:	4.2 Darcies	
Average Horizontal permeability:	7.0 Darcies	
Average SAGD pay:	21 meters	
Average porosity (Ø):	32%	
Average oil saturation:	70%	
<i>Rock Volume: 875 x 10</i> ⁶ m ³		
<i>SOIP: 196 x 10</i> ⁶ m ³		
Note: CVE Volumetric Estimates, not IQRE estimates		

SOIP = Rock Volume in Project area x phi (.32) x So (.70)

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Analysis: ✓ Routine core analysis ✓ Photos

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Geological Maps



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SAGD Pay Iso: SAGD Pay Top – SAGD Base



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SAGD Top Structure, SSTVD



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SAGD Base Structure, SSTVD



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McMurray Iso, McM. - Paleo



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Paleozoic Structure, SSTVD



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Composite type log: Phase B

- Pervasive basal mud layer often separates bitumen and McMurray water
- Basal mud is discontinuous and ranges from 0-4 metres in thickness
- Provides a good marker during SAGD operations





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Composite type log: Phase CDE

- Pervasive basal mud layer often separates bitumen and McMurray water
- Basal mud is discontinuous and ranges from 0-4 metres in thickness
 Lithology
- Provides a good marker during SAGD operations

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Wabiskaw McMurray Shales





Representative Cross Sections





Cross section A-A' (saturation)





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Cross section B-B' (saturation)



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Cross section B-B' (lithology)





Sand Mud

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Geomechanical and surface heave

- Integrated InSAR (Synthetic Aperture Radar) Land Deformation Monitoring took place between October 2014 – October 2015 by MDA Geospatial Services Inc.
- The measurements were successfully made on 98 active corner reflector (CR) locations installed since April 2008
- In addition to the corner reflectors, the deformation profiles at 19,710 point targets were estimated (coherent target monitoring-CTM). The location of these points coincides directly with pad, pipeline and plant structures

Refer to Appendix 1 for detailed heave data



Corner reflector (CR) locations:







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Strain Monitoring



1AC/07-10-076-06W4 ~250 m (185-435 m TVD)

- Strain monitoring gauges were installed winter 2016. No data has been acquired yet, but a baseline will be conducted prior to first steam on H03 Pad.
- The strain monitoring data gathered will be used in models and simulations that will improve our understanding of mechanisms that cause casing impairments.



Subsection 3.1.1 – 3) Drilling and Completions

Mike Ellis Production Engineer





SAGD Summary to Date



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Flow Control Devices

- Currently testing 3 flow control devices
 - 1 liner deployed ICDs
 - 2 tubing deployed ICDs
- Production from wells commenced in 2015
- ICD effectiveness
 review ongoing

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Well Name	Well Type	Production Date	Deployment
F01P08	Producer	08/09/2015	Tubing Deployed
F01P10	Producer	08/03/2015	Tubing Deployed
B07P10	Producer	12/10/2015	Liner Deployed

Subsection 3.1.1 – 4) Artificial Lift

Mike Ellis Production Engineer





Review of artificial lift by well

Pad	Start date	Total producers	Total gas lift producer wells	Total ESP producer wells	Total wells using Wedge Well [™] technology and ESP
A Pad	2002	10	0	7	3
A02 Pad	2008	2	0	2	0
B01 Pad	2008	13	0	7	6
B02 Pad	2006	8	0	4	4
B02c Pad*	2013	6	0	6	0
B03 Pad	2011	16	0	8	8
B04 Pad	2011	16	0	8	8
B05 Pad	2012	18	0	9	9
B06 Pad	2012	8	0	8	0
B07 Pad	2012	8	0	8	0
B07b Pad	2015	11	0	11	0
B08 Pad	2013	10	0	10	0
B09 Pad	2014	11	0	11	0
B11 Pad	2013	12	0	12	0
F01 Pad	2015	12	0	12	0

*Note: B02C refers to the 6 well pairs on the north side of the B02 Pad Approved Drainage Box, which were drilled at a 50m

lateral downhole spacing

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Artificial lift performance

Gas lift (0 current wells):

- Typical operating pressure 4,000 5,000 kPag
- No temperature limitations, go as hot as ~263°C
- Average emulsion flow rate ~ 600-1600 m³/d

ESP (150 current wells):

- Majority of wells were converted to ESP after a gas lift phase
- ESP conversion occurs when thief zone intersected or other optimization purposes
- Typical operating pressure 1,800 4,000 kPag
- No temperature limitations, go as hot as ~235°C BHT
- Average emulsion flow rate ~ 200-1600 m³/d

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Subsection 3.1.1 – 5) Instrumentation

Mike Ellis Production Engineer





SAGD Well Pressure Instrumentation

At Christina Lake all production wells are equipped with bubble tubes to measure downhole pressures.

Currently there are 2 sizes of bubbles tubes:

- $3/_8$ inch
- $1/_2$ inch

We are replacing all $\frac{3}{8}$ inch bubble tubes with $\frac{1}{2}$ inch to increase reliability and to accommodate encapsulated thermocouples, where desired.

Fiber pressure gauges have been trialed with poor results

Moving forward bubble tubes will continue to be the pressure instrumentation of choice at Christina Lake.



SAGD Well Temperature Instrumentation

At Christina Lake, production wells currently use 1 of 2 technologies to measure downhole temperatures.

• Type 'K' Thermocouples

- Single point installed at the heel
- 6 point that is installed along the producer horizontal
- Distributed Temperature Sensing (DTS)
 - fiber optic instrumentation provides temperature measurement at any point from surface to the toe of the producer horizontal section

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Instrumentation in Observation Wells (typical completions)



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Observation Well Equipment Reliability

Type 'K' Thermocouples

Piezometers

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Communications

- Reliability has been very good
- Easy to replace if failed
- Thermocouple failures arise when the mineral insulated (MI) cable is compromised downhole.
- Reliability has been good since 2013 when the switch was made to high temperature vibrating wire piezometers rated to 250°C
- Cemented piezometers are impossible to replace in kind. Need to install hanging piezometer to replace
- Have seen failures as a result of improper installation and well securement issues

- Migration to a new radio network has increased reliability substantially
- Ongoing upgrades to SCADA equipment increases dependability and lowers future maintenance costs



Observation Wells



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Subsection 3.1.1–5c) & d) instrumentation data

Requirements under subsection 3.1.1 5c) and d) are located in Appendices 2 & 3



Subsection 3.1.1 – 6) 4D Seismic

Amin Fardi Reservoir Engineer





Subsection 3.1.1 – 6) a)





a) seismic lines location map

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Subsection 3.1.1 - 6) b)



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b) Interpreted steam-affected chamber thickness

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Subsection 3.1.1 – 7) Scheme performance

Amin Fardi Reservoir Engineer





Scheme performance prediction

- Predict well pair performance based on modified Butler's equation
- Predict well pair CSOR using published CSOR correlations (Edmunds & Chhina 2002)
- Generate overall scheme production performance by adding individual well forecasts over time to honor predicted steam capacity and water treating availability



Wellpair Type Curve



SAGD summary to date

161 total production wells in operation to date:

- 122 standard well pairs
 - all on ESP, no gas lift
- one offset toe producer well
 - ESP
 - increase recovery from A01-3 well pair
- 38 wells using patented Wedge Well[™] technology
 - all on ESP
 - 3 located in A01 pad
 - 1 in between B01 and B02 pad
 - 6 located in B01 pad
 - 3 located in B02 pad
 - 8 located in B03 pad
 - 8 located in B04 pad
 - 9 located in B05 pad







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SAGDable vs. producible OIP (SOIP VS. POIP)

We are presenting two tables

SAGDable OIP & producible OIP

We define SAGDable OIP as:

- (Planned length) x (Spacing) x (Net SAGD pay: <u>Base</u> to top SAGD) x (S_o) x (Ø)
- Used during the planning phase
- Doesn't change after well pair plans finalized
- Used to plan additional wells (Wedge Well[™] technology, bypassed pay producers, re-drills, new pairs)
- We aim to drill the full planned length (typically 800m), and drill the producer well as low as possible in relation to Base SAGD

We define producible OIP as:

- (Effective length) x (Spacing) x (Effective pay: <u>Producer</u> to top SAGD) x (S_o) x (Ø)
- An "after-drilling" OOIP, based on well pair potential
- Changes with time and interpretation (obs. wells, 4D seismic, MWD error, etc.)
- Used to plan blowdown strategy
- This reflects actual well pair performance
 - incorporates actual overlapping slotted liner lengths initially (including blank sections <100m)
 - incorporates actual elevation of the producing well
 - incorporates lithology

Producible OIP is always < SAGDable OIP



SAGDable vs. producible OIP (definition)



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OIP and RF per pad

Oil in Place (OIP) and % Recovery						
Pad	Cumulative Oil Production (Mm ³)*	SOIP (Mm ³)	SOIP Recovery*	POIP (Mm ³)	POIP Recovery*	Ultimate Recovery
Α	2,198	5,054	43.5%	4,332	50.7%	60-85%
A02	373	4,056	9.2%	3,583	10.4%	60-85%
B01	3,323	5,830	57.0%	4,817	69.0%	60-85%
B02	2,256	3,081	73.2%	2,694	83.8%	60-85%
B02C	1,229	2,461	49.9%	1,851	66.4%	60-85%
B03	3,857	7,296	52.9%	5,742	67.2%	60-85%
B04	4,347	7,369	59.0%	6,295	69.1%	60-85%
B05	3,359	8,325	40.3%	7,080	47.4%	60-85%
B06	2,638	5,694	46.3%	4,522	58.3%	60-85%
B07	3,590	6,929	51.8%	6,043	59.4%	60-85%
B07b	166	6,528	2.5%	5,275	3.1%	60-85%
B08 Pad	1,751	5,593	31.3%	4,603	38.0%	60-85%
B09 Pad	1,207	7,063	17.1%	5,999	20.1%	60-85%
B11 Pad	2,639	5,887	44.8%	5,266	50.1%	60-85%
F01 Pad	447	5,954	7.5%	4,668	9.6%	60-85%

Expect to recover 60-85% of oil in place (OIP) depending on the quality of pay. OIP volumes increased by 10% in 2015 compared to previous year's estimates. In certain cases significant non-rich pay was added, which has a lower expected ultimate recovery than the original highly rich pay, thus lowering overall expected ultimate recovery.

A02 OIP volumes encompass the entire standard size drainage box intended for 8-12 SAGD production well pairs. Currently only two producing well pairs.

*As of March 31, 2016

Note: Resource estimates in this table are based on Cenovus volumetric calculations, and are not in accordance with National Instrument 51-101 guidelines. They are provided solely for the purpose of complying with Alberta regulatory requirements.



Average Reservoir Parameters

Pad	Well Spacing (m)	Net SAGD Pay (m)	Pad Area	Average (ø)	Average (S _o)
Α	116	32	800m x 800m	0.31	0.76
A02	100	31	800m x 800m	0.31	0.80
B01	100	37	700m x 850m	0.32	0.80
B02	100	37	375m x 850m	0.32	0.84
B02C	50	28	300m x 1000m	0.32	0.83
B03	100	43	800m x 800m	0.32	0.84
B04	100	43	800m x 800m	0.31	0.81
B05	100	42	800m x 800m	0.31	0.78
B06	100	35	800m x 800m	0.31	0.80
B07	100	40	800m x 800m	0.31	0.81
B07b	67*	29	800m x 800m	0.30	0.75
B08 Pad	67	33	800m x 800m	0.34	0.83
B09 Pad	67	47	800m x 800m	0.31	0.83
B11 Pad	67	39	800m x 800m	0.30	0.82
F01 Pad	67	35	800m x 800m	0.30	0.75

* Pairs 17-19 drilled at 100 m spacing

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Varying Reservoir Quality Pad Patterns

Two example well pairs provided in Subsection 3.1.1 – 7b) illustrate:

- B05-6: High reservoir quality
- B02-1: Medium reservoir quality
- Expect the same ultimate recovery long-term

Variation in well performance is the result of several years of operational learnings between pad start dates.







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B05-6 Well Pair



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B05-6 Toe



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B02-1 Well Pair



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*Rampdown trial at B02-1 interrupted by VFD failure in late 2015, causing steam to be shut-off prematurely.



B02-1 Mid



No baseline data for this well - high water saturations in the pay zone are steam


Five year outlook – pad abandonments

 There are no anticipated pad abandonments for any of the Christina Lake wells in the next five years.



Wellhead steam quality

- Steam quality will be impacted by pipeline size and distance
- Current steam quality injected into all pads is calculated to be greater than 95%
- Currently steam head pressure is operated at 8.5 MPag with a corresponding steam temperature of 300°C
- Steam quality is not expected to impact well performance at this time



Subsection 3.1.1 – 7e) Injected fluids

Co-injection and Blowdown Trials





Full-blowdown on A01 pad

- Full blowdown as of November 2014
 - November 2014: steam ramp down began on the entire pad
 - February 2015: full steam shut-in to all wells on the pad. Pressure maintenance continued through natural gas injection.
 - current chamber average operating pressure ~ 2,000 kPa_q
 - no negative impact has been observed with the pad operations as a result of full methane injection.
 - average concentration for Jan 2015 March 2016
 - average methane injection rate 40 e3m3/d
 - CSOR has been maintained at 2.50



B01/B02 pad rampdown/blowdown pilot

Temporary wind-down test on B01 and B02 pads started June 2015

- timeframe: 1 year
- well pairs: B01-1 to B01-4 including WWs 01-03; B02-1 to B02-4 included.
- steam will be brought back on after test is complete

B01-1 to B01-4: Blowdown test (6 month test, extended to 1 year in Jan 2016)

- shut-in steam on all four wells
 - using gas cap (top down blowdown) to maintain pressure
- CSOR has been maintained at 1.67
 B02-1 to B02-4: Steam ramp-down test (1 year test)
- cut steam by 25% every 3 months (75%, 50%, 25%, 0%)
- CSOR has been maintained at 1.92

Key learnings thus far:

- Increased gas production observed during blowdown
- Neighboring SAGD pads appear unaffected by blowdown at this time



Subsection 3.1.1 – 7e) Injected fluids

A02-2 SAP Project





A0202 SAP



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A0202 SAP (solvent aided process)

- Started butane co-injection in November 2009
- Cumulative SOR of 1.81
- Cumulative solvent recovery factor of 70.6%
- SAP has shown benefit of oil uplift and reducing SOR
- Acid job on producer well in September 2015
- Planning to stop butane co-injection and operate A0202 on steam in Q2 2016
- Planning to commence NCG co-injection (25 wt.%) in Q3 2016
- A0201 Early SAP injection (planning to inject butane in Q2/Q3 2016)



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Subsection 3.1.1 – 7e) Injected fluids

Surfactant Steam Process (SSP) pilot





SSP (Surfactant Steam Process)



C1 → B11P09 (control well 1) S1 → B11P10 (surfactant 1) S2 → B11P11 (surfactant 2) C2 → B11P12 (control well 2)

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SSP

- Four wells in SSP trial
- Two wells with different surfactants and two control wells
- First steam in July 2013
- High pressure ESP operation (4000 kPa BHP) in November 2013
- First surfactant co-injection in January 2014
- Low pressure ESP operation (2800 kPa BHP) in June 2014
- Stopped injecting surfactant in Jan/Feb 2015
- Results are inconclusive due to communication with neighboring wells and thief zones



Subsection 3.1.1 – 7f) 2015 key learnings

Operating SAGD with Top Gas, Bottom Water





Operations at Christina Lake

Thief zones:

- B01 to B11 pad are operating under a gas cap
- A01, B01 to B11 and F01 Pads have areas where Regional Bottom Water (BW) present with no shale break separating oil and BW

Well performance of these two situations will be discussed:

- gas cap communication only
- bottom water and gas cap communication



High pressure operations

For high pressure operations, the SAGD chamber has to be isolated from other zones

> no gas cap or bottom water contact





Gas Cap at Christina Lake





B05-3 Gas Cap Communication



Gas influx into the steam chamber as evidence from cooling on thermocouples in adjacent monitoring wells. Effects of gas influx into the steam chamber are reversible.

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Bottom Water With No Isolation



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Regional Bottom Water Pressure Influence



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Regional Bottom Water Pressure Influence



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Source Well **Disposal Well**

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Subsection 3.1.1 – 7f) 2015 key learnings

Patented Wedge Well[™] technology





Patented Wedge Well[™] Technology Locations



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Wedge Well[™] Learnings

- Better parent well pair operation has reduced the necessity of wells using the Wedge Well[™] technology.
- Wedge Well[™] technology use may still be justified given the right conditions and will be evaluated on an individual pad basis going forward.
- Wedge Well[™] vertical offset in relation to neighboring producers is determined by balancing the accessible incremental oil that can be recovered by the Wedge Well[™] with the extent of conductive heating from the existing producing pairs.



Subsection 3.1.1 – 7f) 2015 key learnings

Wabiskaw Zone at Christina Lake





Background

Unexpected Discovery: steam-core drill in April 2013

6,500kPa Overpressure: conductive thermal expansion in WBSK (above 5,400kPa MOP)

4D Seismic Identification

WBSK Producer: 107/06-15, 8,600m³ oil, depressurization

Monitoring: enhanced observation capabilities in the area





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2015-2016 Monitoring Enhancements

- Installed piezometer (00/05-14)
 - 4D seismic anomaly NOT overpressure
- Fixed broken thermocouples (03/05-14)
- Fixed broken piezometer (08/06-15)
- Added WBSK thermocouples (02/11-14)
- Shot 4D seismic in Q1 2016





Conclusion

- None of the Wabiskaw is currently observed to be over MOP.
- Monitoring is in place to detect any future over pressuring before it reaches MOP.
- Potential overpressure in 4D seismic in Zone 2 proved to be low pressure, hints at gas accumulation and McMurray/Wabiskaw communication in this area, which reduces overpressure risk.
- Mitigation plans are in place if pressures climb towards MOP.



Subsection 3.1.1 – 7g) Information requests





Information Requests

No Information requests for 2015



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Subsection 3.1.1 – 7h) Pad production plots





Pad production plots

Requirements under subsection 3.1.1 7h) are located in Appendix 4



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Subsection 3.1.1 – 8) Future plans

Amin Fardi Reservoir Engineer





Resource recovery strategy

Well/pad placement:

- 2016/2017 well pairs will be drilled as per the existing (or future) applications and approvals
- Well spacing/trajectories planned to be submitted for approval prior to construction/drilling

No changes in the overall resource recovery strategy (operating pressure, composition of injected fluid)

Any deviations will be applied for as future amendments



SAGD Drilling Plans 2016/2017

Pad	Pad type	Well count	Timing
J07	Production	9 well pairs	Q1 2016
J09	Production	9 well pairs	Q1 2016
H09	Production	6 well pairs	Q2 2016
H07	Production	9 well pairs	Q4 2016
L02	Production	8 well pairs	Q2 2017
B12	Production	8 well pairs	Q3 2017
G11	Production	8 well pairs	Q4 2017



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Planned Strat Wells for 2016/17



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Steam strategy 2016

- Phase F OTSG adding ~15,000 m³/d incremental capacity. Two additional pads planned to start up with Phase F OTSG: H01, H03
 - total of 24 well pairs
- The following pads are planned to start up for sustaining production: B06 Wedge Well[™] technology, B10, L03, J03, L05, L09, J01, B13
- total of 93 well pairs and 12 wells using Wedge Well[™] technology
- Rampdown/blowdown/co-injection operations:
 - plan to continue blowdown at A01 pad
 - plan to continue at blowdown on B01-1 to B01-4 and rampdown on B02-1 to B02-4
 - Finalize co-injection/blowdown timing on B03, B04, B07 pad
- No steam shortages expected on existing pads



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Steam strategy 2017

- The following pads are planned to start up for sustaining production: J09, J07, H09
- total of 24 well pairs
- Blowdown operations:
 - planned to continue at A01 pad
 - Return steam to B01 and B02 and study reversibility following blowdown/rampdown test
 - Commence co-injection/blowdown on mature pads
- No steam shortages expected on existing pads



Appendix 1 Subsection 3.1.1 – 2)

Heave data





Annual vertical deformation rates:

November 16, 2014 – November 11, 2015 (1 year)



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Previous Annual vertical deformation rates:

November 21, 2014 – November 16, 2016





Geomechanical and surface heave (Coherent Targets)





Appendix 2 Subsection 3.1.1 – 5d)

Piezometer data









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100/07-10-076-06W4

Broken Downhole







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100/15-11-076-06W4

Broken Downhole



102/06-12-076-06W4

Broken Downhole









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102/05-14-076-06W4

Broken Downhole







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100/09-15-076-06W4

Broken Downhole












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100/10-03-076-06W4

Broken Downhole



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Appendix 3 Subsection 3.1.1 – 5d)

Observation Well Temperature Data







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Appendix 4 Subsection 3.1.1 – 7h) Pad Production Data












































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Cenovus Christina Lake In-situ Oil Sands Scheme 8591 2015 Update

Surface June 16, 2016

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Oil & gas and financial information

Oil & gas information

The estimates of reserves and contingent resources were prepared effective December 31, 2015 and the estimates of bitumen initially-in-place were prepared effective December 31, 2012. All estimates were prepared by independent qualified reserves evaluators, based on definitions contained in the Canadian Oil and Gas Evaluation Handbook and in accordance with National Instrument 51-101. Additional information with respect to the significant factors relevant to the resources estimates, the specific contingencies which prevent the classification of the contingent resources as reserves, pricing and additional reserves and other oil and gas information, including the material risks and uncertainties associated with reserves and resources estimates, is contained in our AIF and Form 40-F for the year ended December 31, 2015, available on SEDAR at www.sedar.com, EDGAR at www.sec.gov and on our website at cenovus.com.

There is uncertainty that it will be commercially viable to produce any portion of the contingent resources. There is no certainty that any portion of the prospective resources will be discovered. If discovered, there is no certainty that it will be commercially viable to produce any portion of those resources. Actual resources may be greater than or less than the estimates provided.

Total bitumen initially-in-place (BIIP) estimates, and all subcategories thereof, including the definitions associated with the categories and estimates, are disclosed and discussed in our July 24, 2013 news release, available on SEDAR at sedar.com and at cenovus.com. BIIP estimates include unrecoverable volumes and are not an estimate of the volume of the substances that will ultimately be recovered. Cumulative production, reserves and contingent resources are disclosed on a before royalties basis. All estimates are best estimate, billion barrels (Bbbls). *Total BIIP* (143 Bbbls); *discovered BIIP* (143 Bbbls); *discovered BIIP* equals the *cumulative production* (0.1 Bbbls) plus *reserves* (2.4 Bbbls); *sub-commercial discovered BIIP* equals economic contingent resources (9.6 Bbbls); prospective resources (8.5 Bbbls); *unrecoverable portion of discovered BIIP* (42 Bbbls). Any contingent resources as at December 31, 2012 that are sub-economic or that are classified as being subject to technology under development have been grouped into the unrecoverable portion of discovered BIIP. Petroleum initially-in-place (PIIP) estimates for Pelican Lake are effective December 31, 2012 and were prepared by McDaniel. All estimates are best estimate discovered PIIP volumes as follows: *Mobile Wabiskaw* total PIIP (2.11 Bbbls); cumulative production (0.11 Bbbls); reserves (0.25 Bbbls); unrecoverable protucion (0.11 Bbbls); unrecoverable discovered PIIP (1.72 Bbbls); undiscovered PIIP (1.62 Bbbls); unrecoverable resources (0.03 Bbbls); unrecoverable discovered PIIP (1.72 Bbbls); undiscovered PIIP (0 Bbbls). *Mobile Wabiskaw development area* total PIIP (0 Bbbls). *Immobile Wabiskaw* total PIIP (1.33 Bbbls); unsecoverable PIIP (1.33 Bbbls); unculative production (0 Bbbls); reserves (0 Bbbls); undiscovered PIIP (0 Bbbls); uncoverable discovered PIIP (1.33 B

Certain natural gas volumes have been converted to barrels of oil equivalent (BOE) on the basis of one barrel (bbl) to six thousand cubic feet (Mcf). BOE may be misleading, particularly if used in isolation. A conversion ratio of one bbl to six Mcf is based on an energy equivalency conversion method primarily applicable at the burner tip and does not represent value equivalency at the well head.

Non-GAAP measures

Certain financial measures in this document do not have a standardized meaning as prescribed by IFRS such as, Operating Cash Flow, Cash Flow, Operating Earnings, Free Cash Flow, Debt, Net Debt, Capitalization and Adjusted Earnings before Interest, Taxes, Depreciation and Amortization ("Adjusted EBITDA") and therefore are considered non-GAAP measures. These measures may not be comparable to similar measures presented by other issuers. These measures have been described and presented in order to provide shareholders and potential investors with additional measures for analyzing our ability to generate funds to finance our operations and information regarding our liquidity. This additional information should not be considered in isolation or as a substitute for measures prepared in accordance with IFRS. Readers are encouraged to review our most recent Management's Discussion and Analysis, available at cenovus.com for a full discussion of the use of each measure.

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Advisory

This presentation contains information in compliance with:

AER Directive 054 - Performance Presentations, Auditing, and Surveillance of In Situ Oil Sands Schemes

This document contains forward-looking information prepared and submitted pursuant to Alberta regulatory requirements and is not intended to be relied upon for the purpose of making investment decisions, including without limitation, to purchase, hold or sell any securities of Cenovus Energy Inc. The resources estimates contained herein are not reported in accordance with National Instrument 51-101 and are provided solely for the purpose of complying with Alberta regulatory requirements.

Additional information regarding Cenovus Energy Inc., including information regarding contingent resources, is available in our Annual Information Form for the year ended December 31, 2015 and in our Statement of Contingent and Prospective Resources for the year ended December 31, 2015 at cenovus.com.





About Cenovus

TSX, NYSE | CVE

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Enterprise value	C\$18 billion
Shares outstanding	833 million
2016F production	
Oil sands	151 Mbbls/d
Conventional	54 Mbbls/d
Total liquids	205 Mbbls/d
Natural gas	385 MMcf/d
Total production	269 MBOE/d
2015 proved & probable reserves	3.8 BBOE
2015 proved & probable reserves Bitumen	3.8 BBOE
2015 proved & probable reserves Bitumen Economic contingent resources*	3.8 BBOE 9.3 Bbbls
2015 proved & probable reserves Bitumen Economic contingent resources*	3.8 BBOE 9.3 Bbbls
2015 proved & probable reserves Bitumen Economic contingent resources* Lease rights**	3.8 BBOE9.3 Bbbls2.0 MM net acres
2015 proved & probable reserves Bitumen Economic contingent resources* Lease rights** P&NG rights	3.8 BBOE9.3 Bbbls2.0 MM net acres4.1 MM net acres

Values are approximate. Forecast production based on February 11, 2016 guidance. *See advisory. **Includes an additional 0.5 million net acres of exclusive lease rights to lease on our behalf and our assignee's behalf.



Area Map



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Subsection 3.1.2 – 1) Facilities

Mandy Chen Sr. Process Engineer





Facility Summary

2nd Stage Blowdown Boiler Start-Up

- Two blowdown boilers were commissioned in September 2015
- Increase steam capacity by 7,280 t/d and minimize blowdown disposal
- Operated on 100% blowdown as feed water

Addition of Heat Exchangers

- Nine heat exchangers were added in August 2015
- Increased cooling capacity by ~3,180 m³/d



Overall Plot Plan – Existing Plant Plus Phase F/G



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Phase A/B Process De-oiling, Steam & Water System



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Phase C/D/E Process De-oiling



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Phase C/D/E Steam & Water System





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Facility Modifications

- No additional major modifications made to Phase A-E outside of Phase C/D/E optimization already mentioned
- Commissioning of Produced Water / Boiler Feed Water crossover line to enable water sharing across Phase A-E and Phase F expected May 2016
- Commissioning of CL1F expansion expected in August 2016
 Includes addition of cogeneration
- Addition of three blend coolers and commissioning expected in June 2016



Subsection 3.1.2 – 2) Facility performance

Bailey Gould Process Engineer





Plant performance

Exceeded design performance:

- Steam plant has achieved higher rates than nameplate design (103%, 50,000 t/d vs nameplate 48,400 t/d)
- Oil treating has achieved higher rates than nameplate design (101%, 25,755 m³/d vs 25,437 m³/d)

Debottlenecking Completed:

- Successful commissioning and start up of CDE Optimization project
- Debottleneck included 2 x OTSGs and additional cooling equipment



Bitumen treatment

Process

- Capacity of 25,437 m³/d, consistently achieving nameplate production in Q1 2016 as new pads ramp up
- Have reduced issues with treating and water quality due to:
 - Further improvements to chemical treating program
 - Improved operating procedures and monitoring programs
 - Modifications to control logic and increased automation
- Continued success of treating program to minimize slop production
- Slop handling is internalized within the facility, with little to no offsite management



Water treatment

De-oiling

- Capacity of 49,146 t/d of water
- Flowed up to 51,032 t/d of water
- Issues in de-oiling are:
 - Water cooling at high flow rates
 - Fouling of heat exchangers

Water treatment

- Blowdown recycle into the produced water treatment trains and boiler feed water tank with no adverse impacts up to 50% of total blowdown volumes produced
- Chemical optimization continues to be a focus in water treatment



Steam generation

Steam generation via 17 OTSGs

- Original design capacity of 48,400 m³/d CWE dry steam
- Re-rated design capacity of 50,800 m³/d CWE dry steam
- Have achieved rates in excess of 50,000 m³/d CWE dry steam
- Typical operation: 82% quality
 - Worked with vendor to re-rate CDE OTSGs
 - Rigorous monitoring program including continuous boiler performance monitoring
 - 2 x OTSGs were operated on 100% blowdown as feed water and 75% steam quality for 2 months with slightly higher scaling rate in the radiant section observed



Power usage



*Note – Plot represents monthly power imports. No operating power generation facilities at Christina Lake.

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Gas usage



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Gas flared





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Greenhouse gas emissions

Greenhouse gas emissions are reported to AER on yearly basis for review

- Q1 2016 total direct emissions by gas type
 - CO₂ 548,976 tonnes CO₂e
 - CH₄ 5,907 tonnes CO₂e
 - N₂O 905 tonnes CO₂e
- 2015 total direct emissions by gas type
 - CO₂ –1,968,254 tonnes CO₂e
 - CH₄ 29,843 tonnes CO₂e
 - N₂O 3,164 tonnes CO₂e

*Note – Only the 2015 GHGs have been verified and submitted, the 2016 numbers are preliminary.

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Subsection 3.1.2 – 3) Measurement and reporting (MARP)

Mandy Chen Sr. Process Engineer




Simplified MARP schematic



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Production Volumes

Bitumen Production

- Estimate by well tests (2 phase test separators with BSW%)
 - 8-12 wells per separator
 - ~10 hour cycles + purges
 - 1 hour of testing for every 40 hours of well operations, or about 2 x 10 hour tests per month

Gas Production

- The produced gas is "measured by difference" based on the gas balance.
- This "measured by difference" monthly volume is used to calculate the facility gas-to-oil ratio (GOR) and then be used to estimate gas production from each well since October 2015.



Injection Volumes

Steam Injection

- Steam to wells measured by nozzles or V-cone
- Prorate well steam to plant steam metered by flow nozzle off steam separators

Gas Co-Injection

Co-injected gas monitored and reported on a well basis



Water Balance

- Two RD1 disposal water meters were found to be inaccurate due to improper meter configurations in the Distributed Control System (DCS).
- This measurement issue was addressed after the problem was found in December 2014.
- Overall water balance had been improved in 2015. The average monthly water imbalance is 2.99%.

Note:

 Correction factors were applied to disposal volumes reported by the MARP meters. A letter of self disclosure for the water imbalance was submitted to AER in February 2015.



Water Balance





Proration factors



Courtesy of AER

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Oil Proration Factor



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Water Proration Factor



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Gas Proration Factor



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Steam Proration Factor



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Subsection 3.1.2 – 4) Water production (injection and uses)

Bailey Gould Process Engineer Kayley Moule Production Engineer







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Produced water to steam ratio





Produced water volumes





Water recycle ratio



Produced-Water Recycle (%) = [(Produced Water In – Disposal Total) / (Produced Water In)] x 100





Note: Blowdown recycle rates vary depending on Produced Water: Steam ratio and make-up water demand, in addition to BFW quality.



Brackish water use



Uses:

Make-up water for steam generation

• Produced water and produced emulsion cooling in Phase ABCDE

• Softened water used for slurry make-up, seal flushes etc.



Brackish water intensity





Fresh water use



Uses:

• Was used for make-up water for steam generation during commissioning and start up of CDE Optimization OTSGs.

• Includes camp and domestic use, utilities, etc. All attempts are made to minimize fresh water usage when not required as make-up water.

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Fresh water intensity



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Total disposal volumes (PW, RW, BD)



Notes: Operating philosophy is to minimize disposal volumes at all times and maximize produced water re-use. Specifically, blowdown recycle, regeneration optimization, and minimizing brackish make-up requirements have been areas of focus to reduce disposal.

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Directive 081 disposal limit





3-16 well reversal

Reversal of the 3-16 Disposal Well



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Fresh wells:

- •Two Quaternary wells (Empress Formation) at 09-17-076-06W4M
- •ESRD Licensed for up to 5,000 m³/day
- •TDS = 500-600 mg/L
- -1 Quaternary well (Empress Formation) at 06-16-076-06W4M with TDL of 20,000 m3 for Feb-Sept 2016

Brackish water source wells:

Historical

- •10-34A 1F1/13-35-075-06W4/00 TDS= 7,400 mg/L
- •10-34B 1F1/13-34-075-06W4/00 TDS= 5,070 mg/L
- •10-34C 1F1/15-27-075-06W4/00 TDS= 7,780 mg/L
- •10-3A 1F1/16-03-076-06W4/00 TDS= 4,600 mg/L
- •10-3B 1F1/02-03-076-06W4/00 TDS= 5,580 mg/L
- •10-27A 100/04-35-075-06W4/00 TDS= 9,730 mg/L
- •10-27B 100/13-27-075-06W4/00 TDS= 8,900 mg/L
- •10-27C 100/02-27-075-06W4/00 TDS= 11,700 mg/L

Disposal reversal well

•3-16 1F5/03-16-076-06W4/00 TDS= 6,6200 mg/L

•2013

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•CW4-A 1F1/01-35-075-06W4	TDS= 13,200 mg/
•CW4-B 1F1/06-01-076-06W4	TDS= 8,800 mg/L

•New in 2015 (MW1 and MW4 wells-not used until Phase F startup)

MW1-A 1F1/07-18-076-05W4 TDS=16,880mg/L
MW1-B 1F1/03-07-076-05W4 TDS=16,520mg/L
MW1-C 1F1/09-07-076-05W4 TDS=16,420mg/L
MW4-A 1F3/11-09-076-06W4 Not sampled yet-expected TDS=>12,000mg/L
MW4-B 1F1/04-08-076-06W4 Not sampled yet-expected TDS=>12,000mg/L
MW4-C 1F1/16-08-076-06W4 Not sampled yet-expected TDS=>12,000mg/L

Fresh and brackish sources



Water disposal operations

Injecting into McMurray water sands at 13-34 since April 2015 Approval No. 9712, 10627C and 10627D (Class 1b Disposal) Sixteen disposal wells (all Class 1b)

- Three disposal wells located near the facility 3-16-1, 4-16, and 7-16 (now abandoned)
- One well located near the facility (3-16-2) has been converted for disposal reversal
- Six disposal wells located at 15-35 utilized for upset scenarios
- Seven disposal wells in service located at 13-34

13-34 disposal is main disposal location with 15-35 and local wells used as back-up



McMurray water disposal wells



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Disposal well head pressures



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Christina Lake Disposal Totals



Note: No local disposal occurred in 2015 / Q1 2016



Water Disposal Operations



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June 16, 2016

Water disposal operations cont'd

Regional McMurray Pressures



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Waste disposal volumes

Reduced slop oil volume due to treating improvements with chemical optimization.

	2015	2014	2013
Slop Oil / Production Fluids (m ³)	31,518	82,241	157,155
Drilling Waste (m ³)	63,664	56,260	37,086
Lime Sludge (m ³)	16,179	15,279	23,759
Contaminated Soils (m ³)	159	187	310
Spent Scavenger (m ³)	6,613	5,346	2,975
Total	118,113	159,313	221,285



Waste disposal sites 2015

Facility	Total (m ³)
Tervita Janvier Landfill	66,951
Tervita Lindbergh Cavern	20,254
Cancen New Sarepta Disposal Well	19,382
Tervita Bonnyville Landfill	8,051
Newalta Elk Point	2,317
Newalta Fort McMurray	2,180
R.B.W. Edmonton	998
TOTAL (m ³)	120,132

Cenovus Christina Lake trucks all disposal waste to licensed third party facilities



Subsection 3.1.2 – 5) Sulphur production

Bailey Gould Process Engineer





Scavenger recovery details

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Quarter	Recovery
Q1 2015	73.8%
Q2 2015	70.5%
Q3 2015	73.7%
Q4 2015	73.3%
Q1 2016	70.6%

Scavenger uptime details



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Sulphur recovery operation

Preventative measures

- Chemical injection continues to be operated in counter current configuration
- Each train is on a 6-12 month PM to be cleaned (contactor, internal distributor, outlet separator demister inspected)
 - Cleaning has been postponed following change in SO₂ emissions limit to daily rather than calendar quarter year average as of Dec 16, 2015.
 - Require Phase F SRU to be operable before a train can be taken down for cleaning to prevent exceeding daily limit.
- Cleaning frequency determined based on process monitoring (pressure drop, spent chemical quality, gas temperature)





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SO₂ emissions



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Ambient air quality monitoring

Passive exposure monitoring

As per the Approval (Table 3.3), Christina Lake is required to maintain a network of twelve passive monitoring exposure stations to obtain monthly static exposures of H_2S and SO_2 .

The passive monitoring results in 2015 did not identify any significant air quality issues related to Plant operations.

Continuous air quality monitoring

CLTP is required in the Approval (Table 3.3) to maintain one continuous ambient air monitoring station 12 months per year to measure ambient levels of SO_2 , H_2S , and NO_2 concentrations in addition to wind speed and wind direction.

In 2015, continuous air quality monitoring was conducted from Jan 1 to December 31 by Maxxam Analytics. The continuous ambient air monitoring station is located at 03-16-076-06-W4M. This location is the same as the passive monitoring station C10.

There were no operational issues relating to the ambient air monitoring equipment during the monitoring period.

The continuous ambient air quality monitoring in 2015 did not identify any significant air quality issues related to Plant operations.

No criteria exceedances were noted in either monitoring program



Ambient air monitoring results - sulphur dioxide





Ambient air monitoring results – nitrogen dioxide





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Subsection 3.1.2 – 6) Environmental issues

Jesse Wong Environmental Advisor





2015 Compliance issues and amendments

Approval number	Amendments	Compliance issues
EPEA Approval 00048522-01-06&07	06 - Phase H approval issued December 16, 2015. 07 – Clerical amendment	No
EPEA Approval 00298224-00-00	No	No
Water Act Approval 00265924-00-02	02 – Surface Water Run-off Ponds amended to 1:10 yr./24hr duration storm event	No
Water Act License 00267617-00-02	No	No
Water Act License 00343057-00-01	Expiry amended to December 12, 2016	No
Water Act License 00293633-00-00	Water level cut-off elevations modified March 3, 2016	No



Monitoring programs

Monitoring program	Progress and results
Air quality monitoring	Air emissions increased slightly in 2015 due to the commissioning of the blowdown boilers. No significant trends in ambient air monitoring observed.
Groundwater monitoring	Monitoring Program to be updated to include Phase H.
Thermal metal mobilization monitoring	Small temperature changes (up to 2C) detected in the deeper Empress and the Ethel Lake formations in 2015. Groundwater chemistry has been consistent since the start of steaming.
Soil monitoring program	Soil Monitoring Program Proposal authorized April 23, 2014. Monitoring and reporting completed.
Wildlife and caribou mitigation and monitoring programs	3 Year comprehensive report completed and sent to AER on May 15 th , 2015. Proposed changes to programs being discussed with the AER.
Wetland monitoring program	Minor changes to program were approved by the AER in April 2016.



Monitoring programs continued

Monitoring program	Progress and results
Reclamation monitoring Program	Deferred until December 31, 2016. No permanent reclamation has occurred to date, however Cenovus continues to evaluate opportunities for permanent reclamation at the Project, including well pads.
Wetland reclamation trial program	Deferred until a candidate site becomes available
Project level conservation, reclamation and closure plan	To be submitted in October 2017, as per Specific Enactment Direction 001 issued March 1, 2016



Environmental initiatives

The regional multi-stakeholder forums that Cenovus was involved with in 2015 include:

- Canadian Oil Sands Innovation Alliance (COSIA): Linear Deactivation Program (LiDEA)
- Alberta Environmental Monitoring, Evaluation and Reporting Agency (AMERA)
 - Wood Buffalo Environmental Association (WBEA)
 - Alberta Biodiversity Monitoring Institute (ABMI)
 - Regional Aquatics Monitoring Program (RAMP)
- Industrial Footprint Reduction Options Group (iFROG)



Subsection 3.1.2 – 7) Statement of compliance

Brent Mitchell Specialist, Regulatory Applications



2015 Compliance status

Maintain and track compliance

- Incident Management System (IMS)
- Centrac Database for commitment management
- Internal Regulatory Compliance Audit Team
- Dedicated onsite Environmental Monitoring and Stewardship Advisors
- Routine inspections and audits
- Raise awareness through training
- Establish consistent management processes

Cenovus FCCL Ltd. believes existing CLTP operations are in compliance with AER approvals and regulatory requirements.



Subsection 3.1.2 - 8) Statement of non-compliance. **Brent Mitchell** Specialist, Regulatory Application



2015 Non-compliance summary – AER

Date	Non compliance/self-disclosure	Follow-up	
2015-02-03	Unsatisfactory High Risk Drilling Waste Inspection @ 11-22-76-6W4 W0471662	Compliance achieved on Feb 4, 2015	
2015-02-13	Disposal water balance exceedance Approval No. 8591	Compliance achieved on Jul 30, 2015	
2015-03-19	A01 MARP Meters (FIT-226A, 226B, 226C, 226D, 227E, 227F) Approval No. 8591	Compliance achieved on Jun 24, 2015	
2015-07-15	Notice of Noncompliance - Outstanding Non-Abandoned OSE Wells (57 CL wells)	Compliance achieved on Sep 14, 2015	
2016-01-13	Unsatisfactory Low Risk Oil Facility Inspection @ 8-17-76-6W4 F27189	Compliance achieved on Jan 22, 2016	



Subsection 3.1.2 – 9) Future plans





Major activities and target dates

Phase	Regulatory			Production capacity (m ³ /d)	
	Filing	Approval	First steam	Incremental	Total
А	Q1 1998	Q1 2000	Q2 2002	1,590	1,590
В	Q2 2005	Q4 2005	Q2 2008	1,400	2,990
С	Q3 2007	Q2 2008	Q2 2011	6,360	9,350
D	Q3 2007	Q2 2008	Q2 2012	6,360	15,710
E	Q3 2009	Q2 2011	Q3 2013	6,360	22,070
F	Q3 2009	Q2 2011	2016	6,360	28,430
G	Q3 2009	Q2 2011		6,360	34,790
FG Amendment	Q4 2012	Q4 2012		3,180	37,970
CDE 2 nd Stage OTSG	Q4 2012	Q3 2013	2015	3,370	41,340
Н	Q1 2013	Q4 2015		7,950	49,290



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