

Annual Surmont SAGD Performance Review Approvals 9426 and 9460

May 17, 2017 Calgary, Alberta, Canada

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Introduction, Overview and Highlights

Subsection 3.1.1 (1)

Ownership and Approvals

Ownership

 The Surmont In Situ Oil Sands Project is a 50/50 joint venture between ConocoPhillips Canada Resources Corp. and TOTAL E&P Canada Ltd; Operated by ConocoPhillips Canada.

Project History

- 1997 First steam at pilot project
- 2007 First steam at Phase 1
- 2010 Construction start at Phase 2
- 2015 Start-up of Phase 2, solvent soak on well pairs 7&8 on pad 103
- 2016 Start-up of liquid scavenging system

Approval Update - AER Approval No. 9426

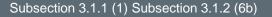
Approval 9426KK – September 15, 2016

- Application No. 1857927 Increase of MOP at DAs 261-3and 262-3
- Application No. 1862673 Extension of well pair lengths at Pad 267 and cancellation of three outboard well pairs at DA 264-2

Approval 9426LL – October 19, 2016

• Application No. 1867584 – to correct MOP value for DA 267-1

Application No. 1880767 (submitted February 28)– Temporary increase of MOP at DA 262-3 to address problem wells



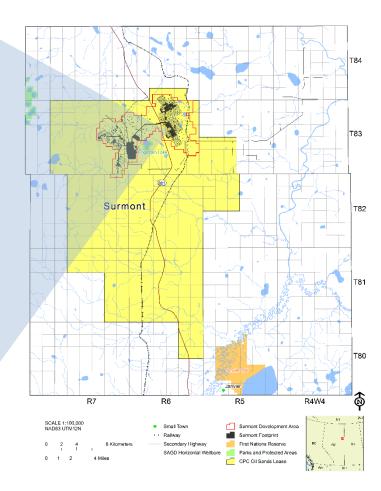


Surmont Overview





Surmont combined approved capacity is 29,964 m³/cd (188,700 bbl/cd)* *(where cd is calendar day on an annual average basis)





Phase 1 production recovery

- Initial results from tubing deployed flow control devices at Pad 101/102 illustrate an increase in total emulsion/bitumen rates
- Liner installed flow control devices at Pad 103 continue to outperform slotted liners (SL) wells
- Instantaneous Steam Oil Ratio (iSOR) continues to improve and trend lower
- Steam splitters were installed on 6 wells

Phase 2 continued ramp-up

- Tubing deployed flow control devices installed on 8 wells in 2016 and have shown an improvement in oil rates
- Liner deployed flow control devices have shown to promote faster development of the wells compared to typical slotted liner wells
- Some wells are still challenged with injectivity/productivity issues, which translates into a slower ramp-up or underperformance based on expectations. Evaluation of optimization opportunities continues.
- Start up of remaining pads from circulation to SAGD except for 266-2.

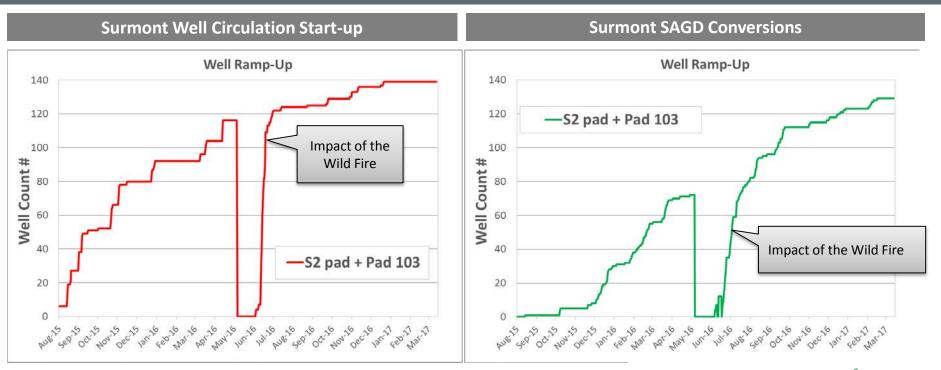
Sustaining pads

- Surmont 1 infill program deferred
- Pad 267 start-up in 2019

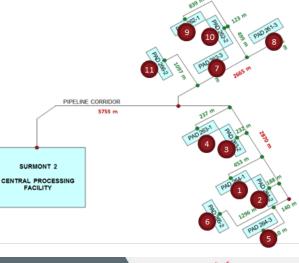
2016 Fort McMurray Wildfire Emergency Shutdown and Re-start



Surmont 2 Ramp-up



- Well pads 261-3, 262-2, 262-1 and 266-2 brought online before end of 2016.
- Convert last 11 wells in circulation to SAGD when ready.
- The well start up base plan was primarily based on a conventional circulation pre-heat period of 90 days. Actual performance has taken longer.
- Futures FCD start up plans are anticipated to recover these poorer performances



Surmont Performance

Historical Steam Injection and Bitumen Production Steam (cwebpd) Oil (boepd) MBPD 400 350 2007-2008 2009 2010-2012 2013+ 2015 S2 300 Unstable Steam Gen Stable operations Continuous Ramp-up reaching "capacity" Improvement Ramp-Up Issues begins 250 200 150 100 50 0 Jan-07 Jan-08 Jan-09 Jan-10 Jan-11 Jan-12 Jan-13 Jan-14 Jan-15 Jan-16 Jan-17

2015 Key Challenges

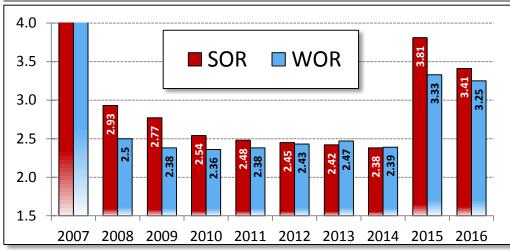
- OTSG fouling
- Front-end treatment
- Pressure drop from 2014 T/A
- Steam constraints (PAD 103 accelerated S/U)

2016 Key Challenges

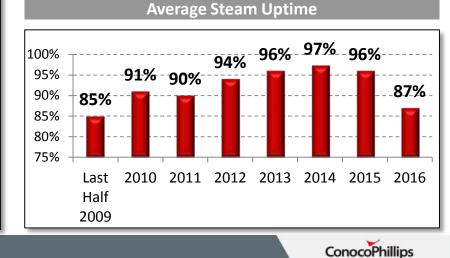
- Slotted liner Ramp-up performance
- Horizontal liner deformation
- Increased performance on S1 base due to re-pressurization
- Fort McMurray Wildfire Recovery

2017 Key Focus Items

- ESP conversions
- TDFCD installations
- Steam allocation

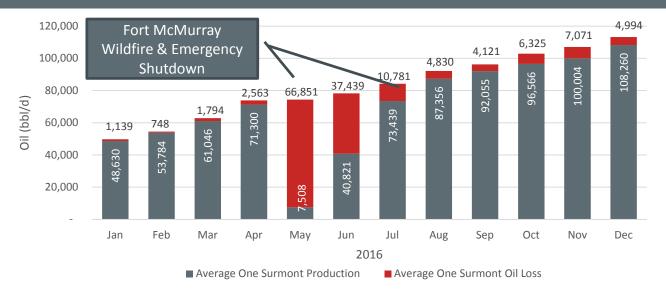


SOR and WOR



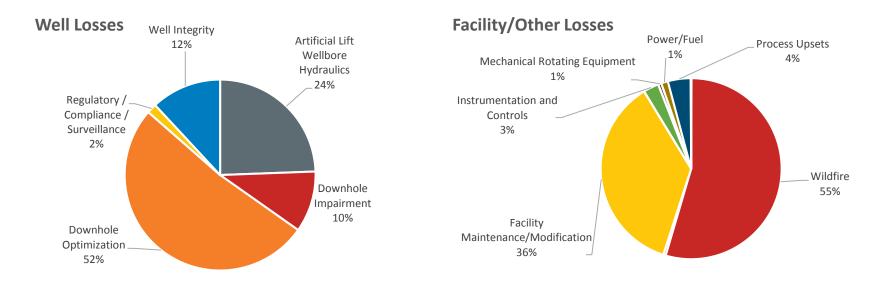
Subsection 3.1.1 (1)

2016 Loss Production Summary



Average Performance	
Oil Average Production (bbl/d)	70,088
Average Oil Loss (bbl/d)	13,666
DOE (Excl. Wildfire)	94%
DOE (Incl. Wildfire)	84%
Steam Uptime (exclusive of wildfires in May 2016)	86.8%

ConocoPhillips

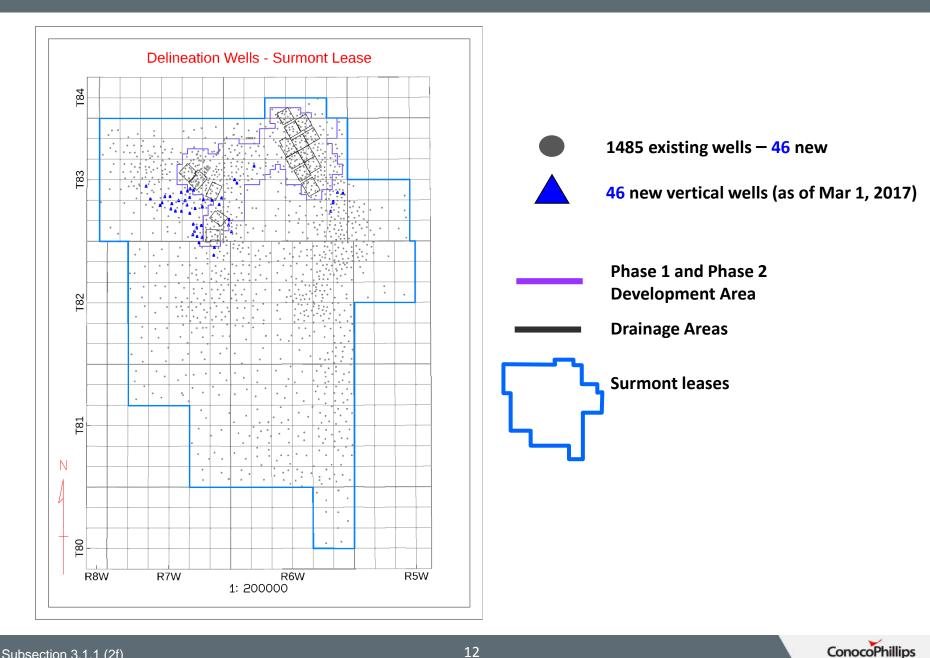


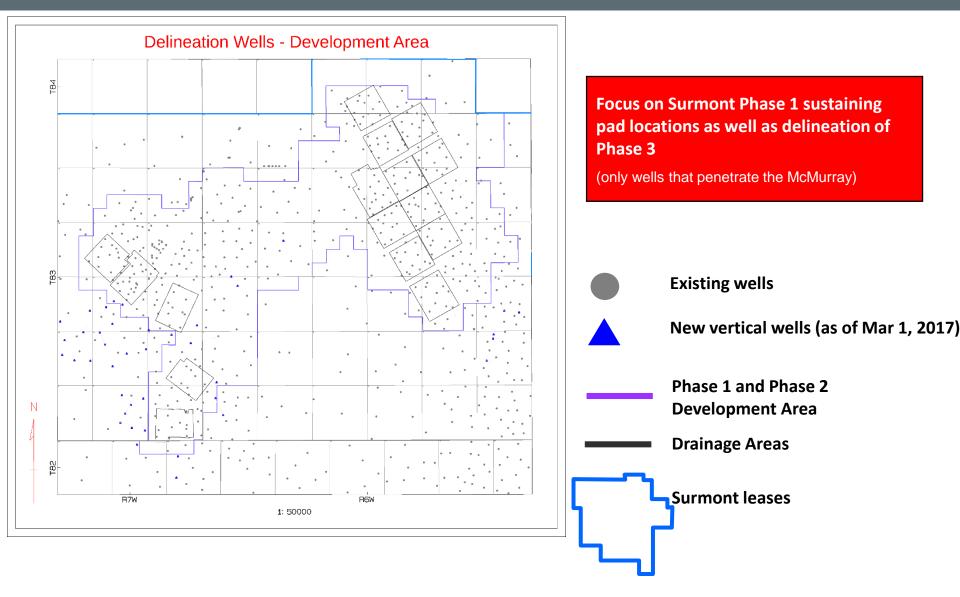
Subsection 3.1.1 (1)



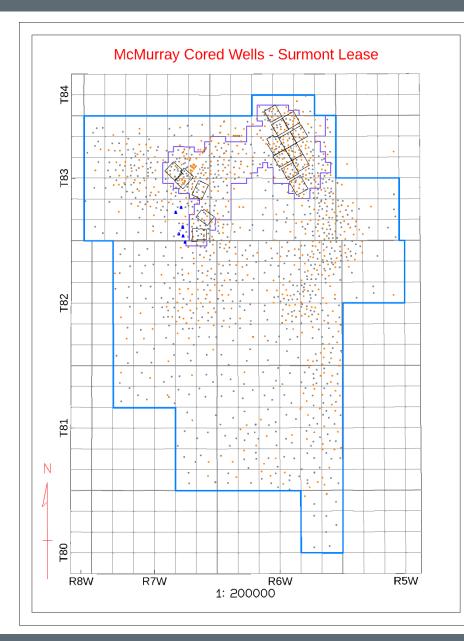
Subsurface Resource Evaluation and Recovery

Geology and Geophysics Subsection 3.1.1 (2)

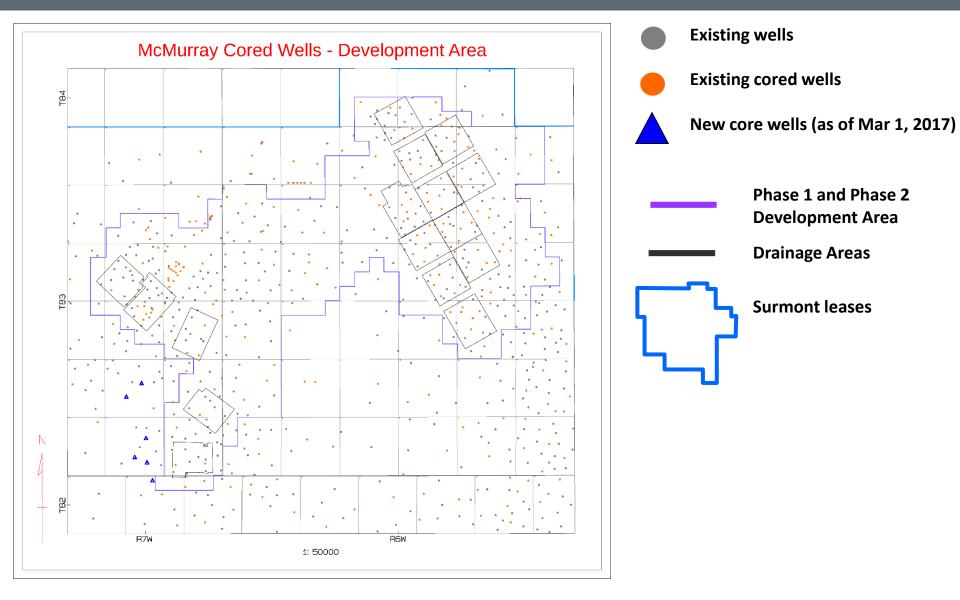




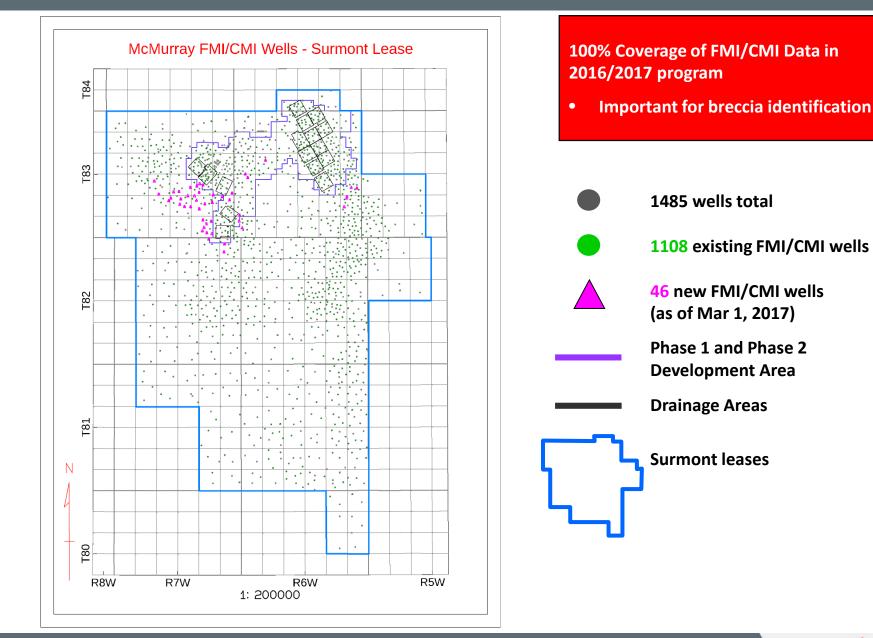




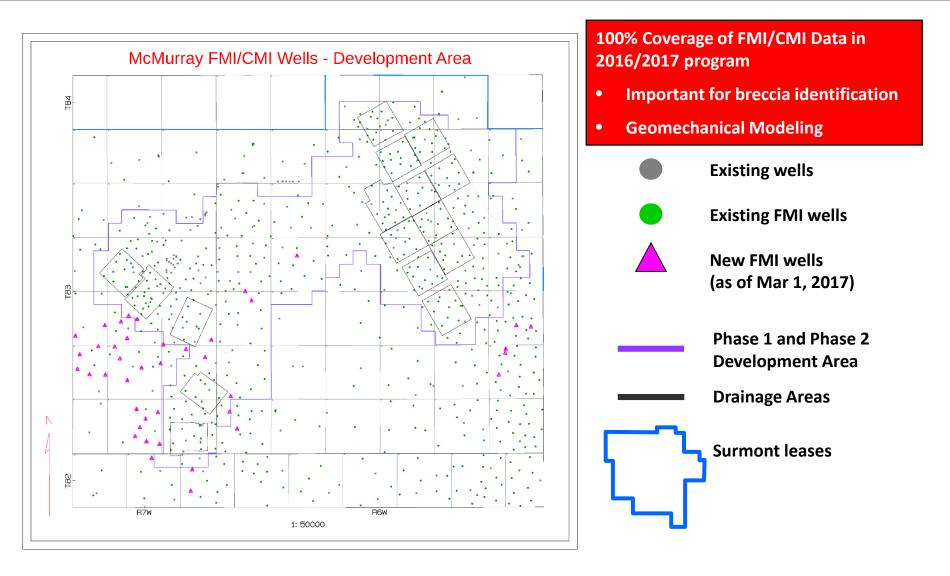




2016-2017 Delineation Campaign and FMI/CMI Logs



2016-2017 Delineation Campaign and FMI/CMI Logs



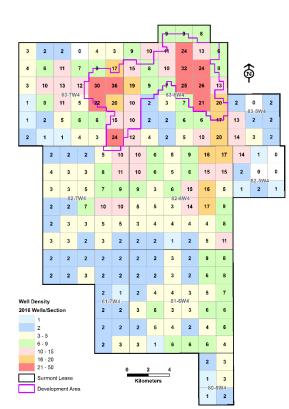


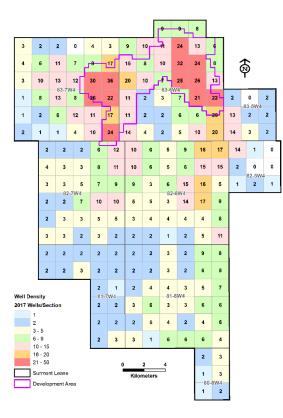
Delineation across Phases 1, 2, and 3

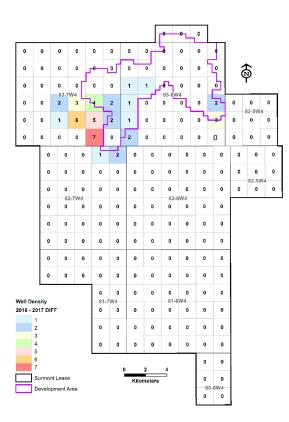
Delineation Well Density Map - 2016

Delineation Well Density Map - Mar 2017

Density Map Difference







McMurray penetrated wells only

ConocoPhillips

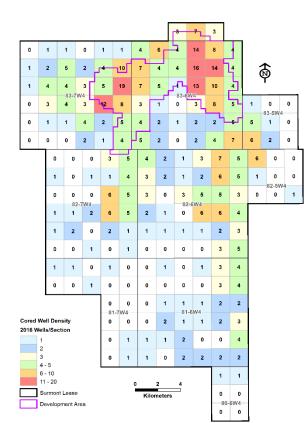
Subsection 3.1.1 (2f)

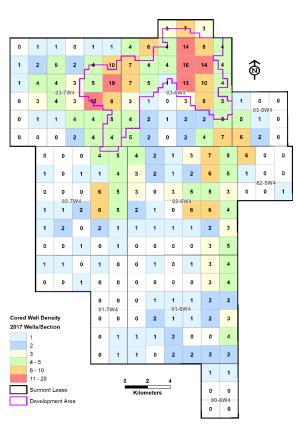
Increased core density with latest drilling

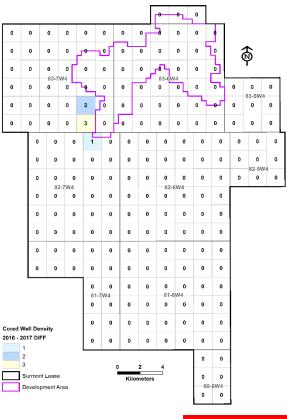
Cored Wells Density Map - 2016



Cored Density Map Difference







McMurray penetrated wells only

ConocoPhillips

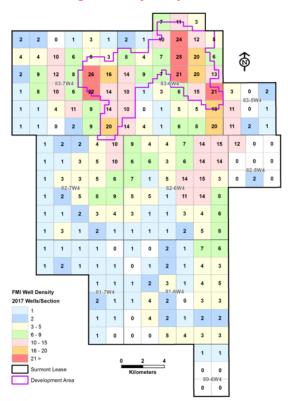
Subsection 3.1.1 (2f)

Increased Formation Micro Imaging density with latest drilling

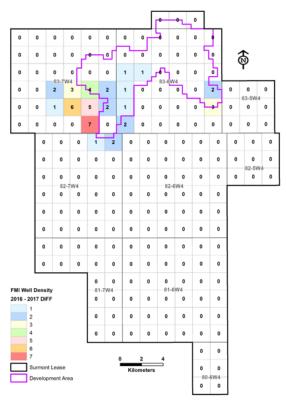
ø -5--T-83-7W4 83-6W4 83-5W4 -15 11 0 1 82-5W4 0 2 0 82-7W 82-6W4 1 2 1 **FMI Well Density** 81-7W4 81-6W4 2016 Wells/Section 2 1 3 3 2 2 3 - 5 6-9 0 5 4 3 10 - 15 16 - 20 21 > Surmont Lease 0 0 Kilometer Development Area 80-6W4 0 0

FMI Well Log Density Map – 2016

FMI Well Log Density Map – Mar 2017

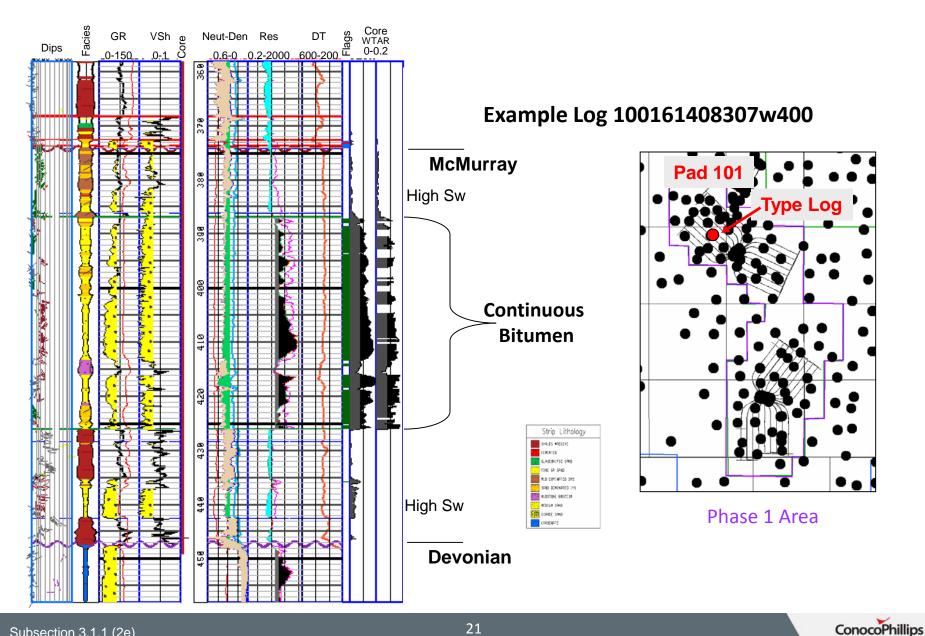


FMI Density Map Difference

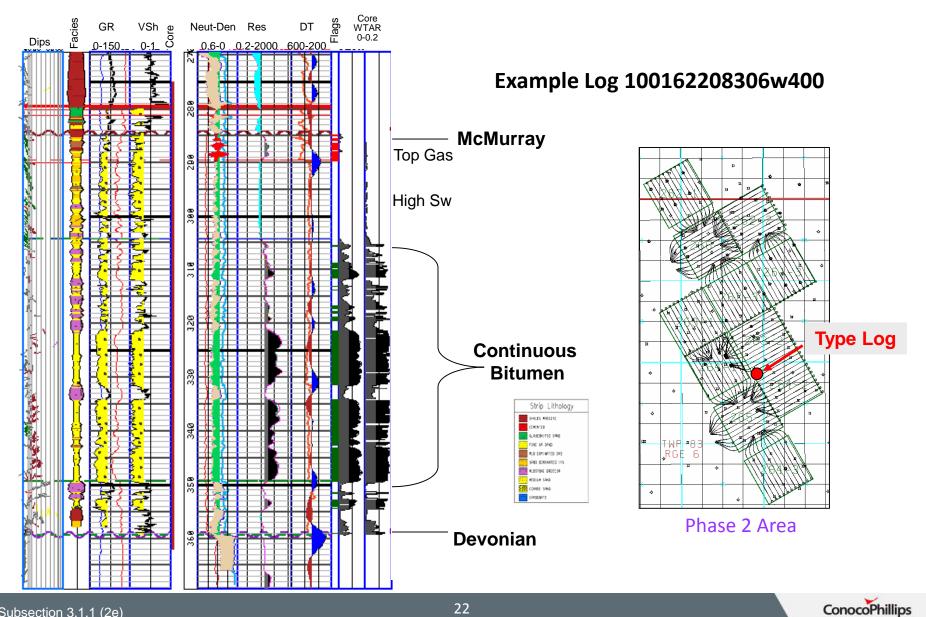


McMurray penetrated wells only

Phase 1 Type Log Well Pad 101



Phase 2 Type Log – Well Pad 264-2



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Special Core Analyses Bitumen Viscosity Sampling

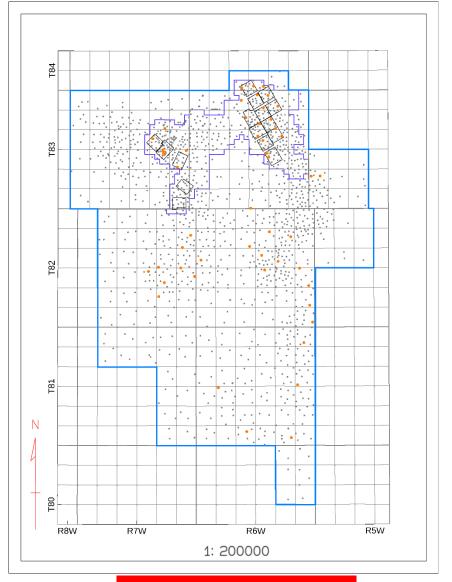
• Objectives:

- Characterize vertical and lateral variance in viscosity at different temperatures.
- Model the variance in bitumen properties and its implications for bitumen production rates during SAGD.
- Characterize relationship between viscosity, density and geochemical composition.

Viscosity increases with depth in the McMurray Formation.

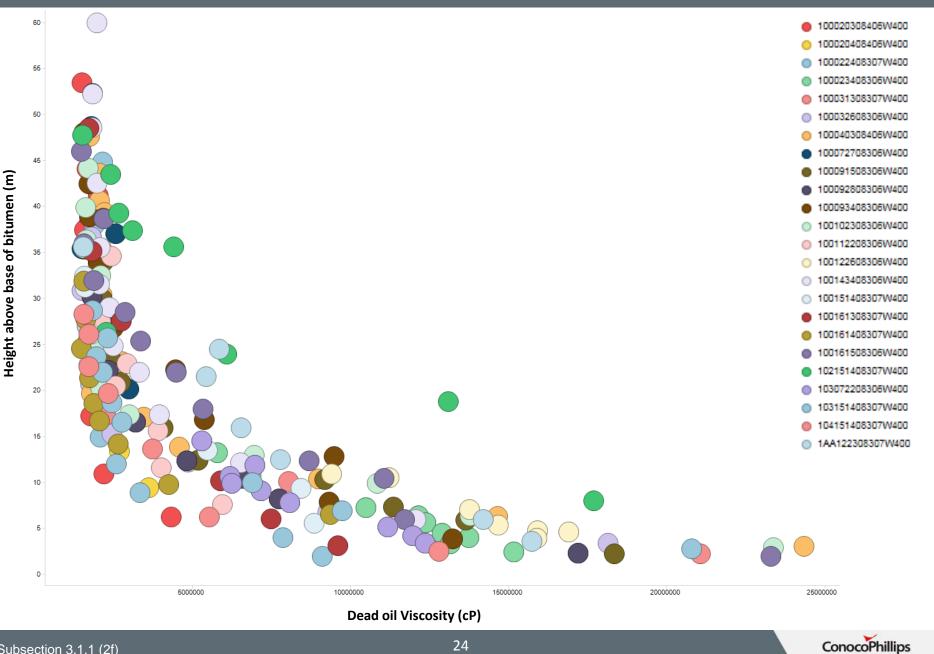
52 existing viscosity sample wells

Delineated Wells - Surmont

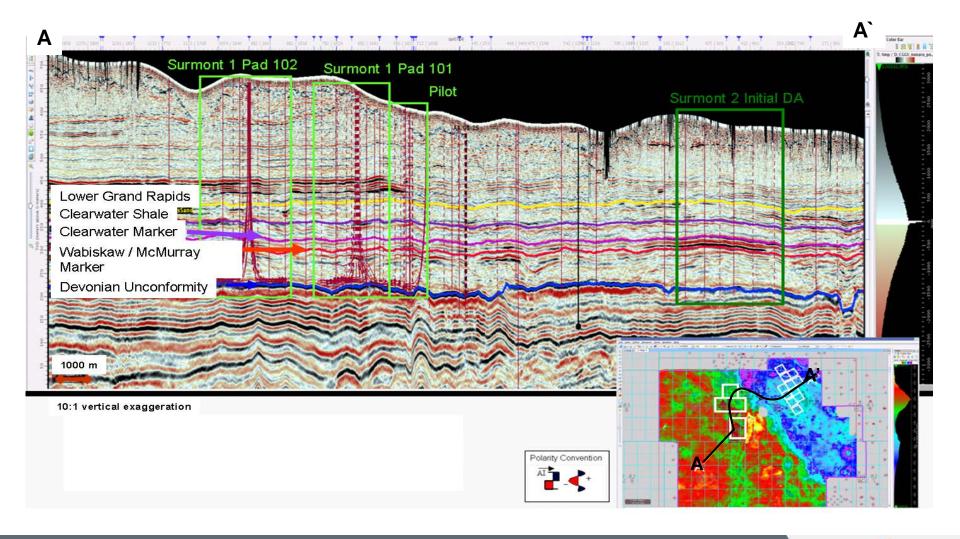


2016 – 2017 Delineation

Viscosity Gradient

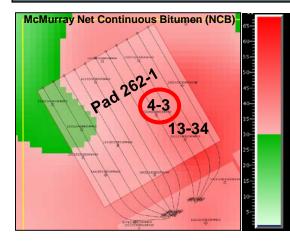


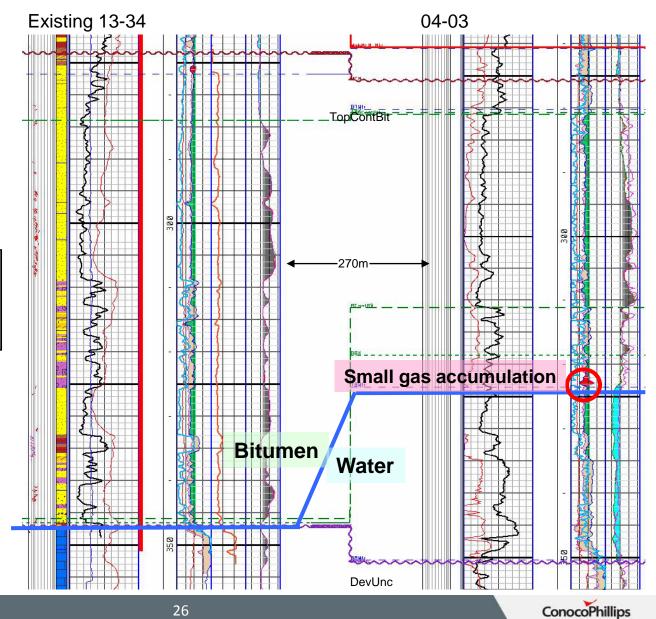
Representative Structural Cross Section



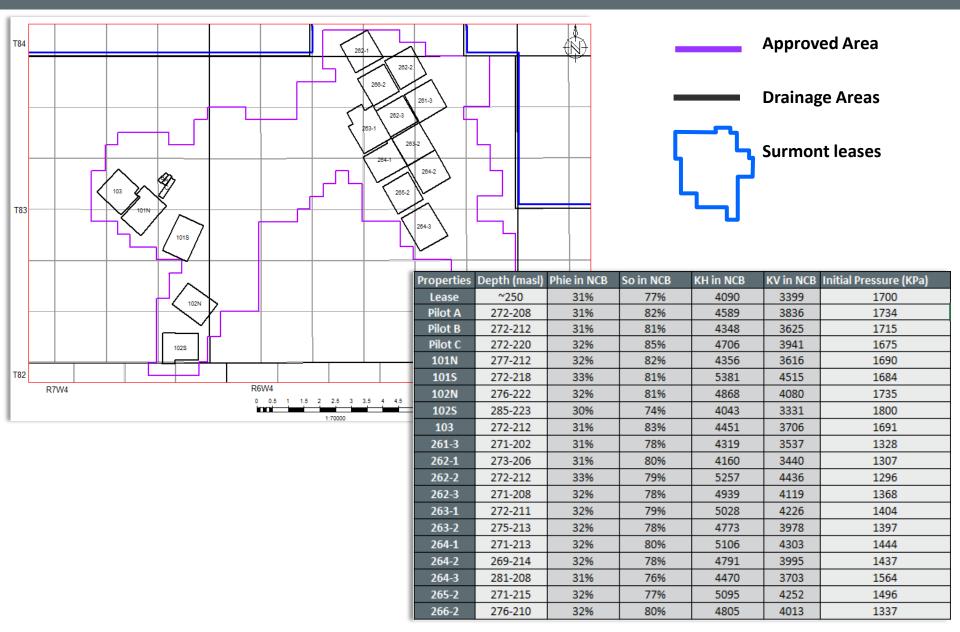
Well Pad 262-1 Variable Bitumen-Water Contact

- A well at 4-3-84-6 W4M intersected a raised bitumen/water contact, the contact is ~ 12 m higher than the nearest offset.
- The well also intersected a small gas pool under the bitumen.
- The presence of basal water becomes a potential impact on production performance on Well Pad 262-1



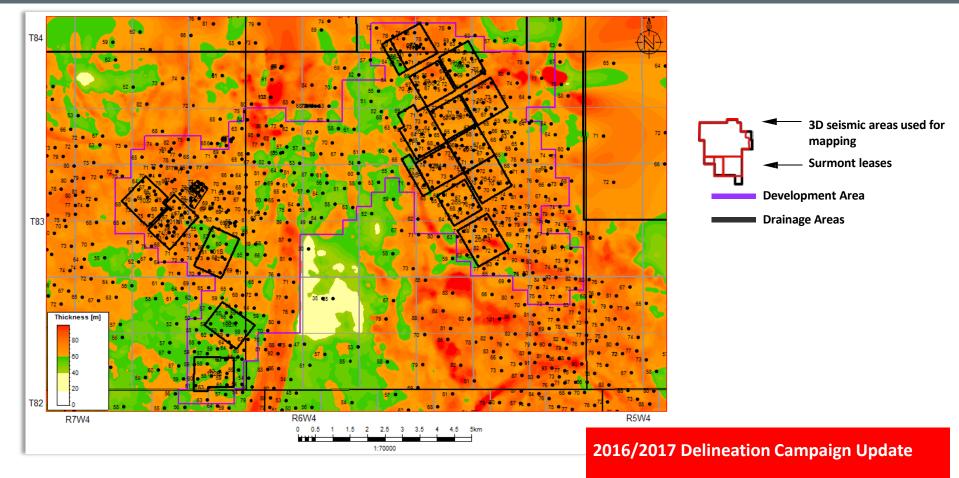


Reservoir Characteristics





McMurray Gross Isopach

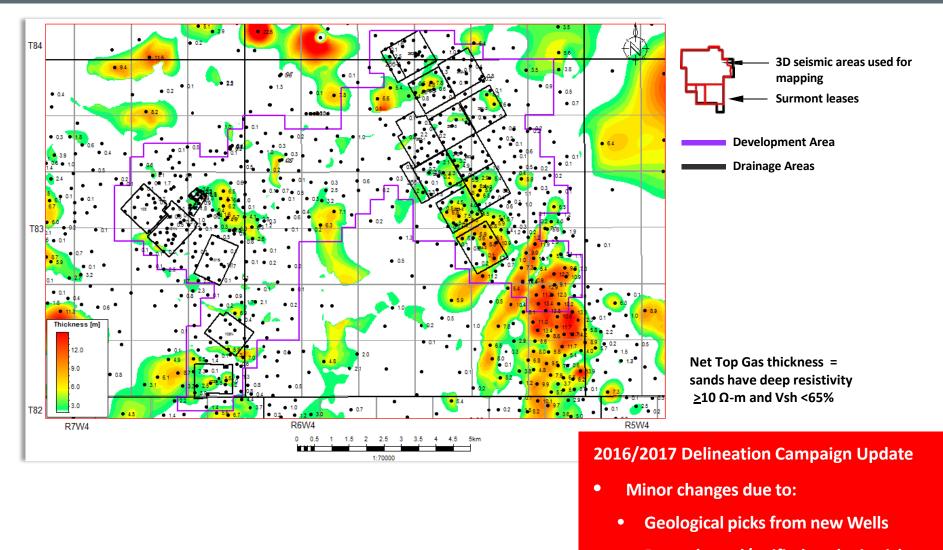


- Minor changes due to:
 - Geological picks from new Wells
 - Re-evaluated/unified geologic picks
 - Revised Seismic Interpretation



McMurray Gross Isopach

McMurray Net Gas Isopach

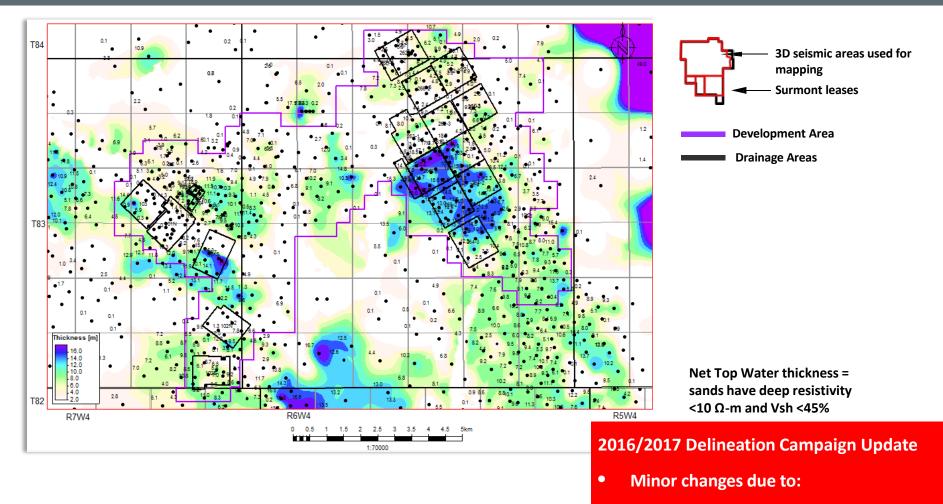


McMurray Net Gas Isopach

- Re-evaluated/unified geologic picks
- Revised Seismic Interpretation



McMurray Net Top Water Isopach

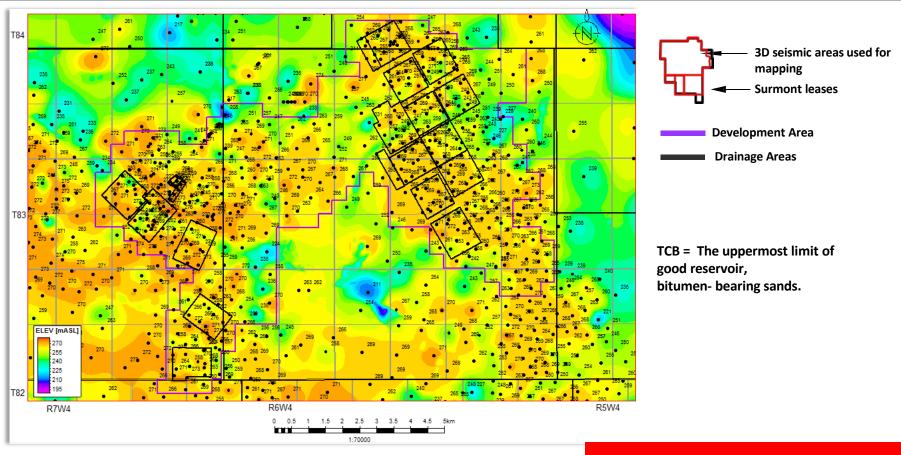


- Geological picks from new Wells
- Re-evaluated/unified geologic picks
- Revised Seismic Interpretation



McMurray Net Top Water Isopach

McMurray Top Continuous Bitumen Structure



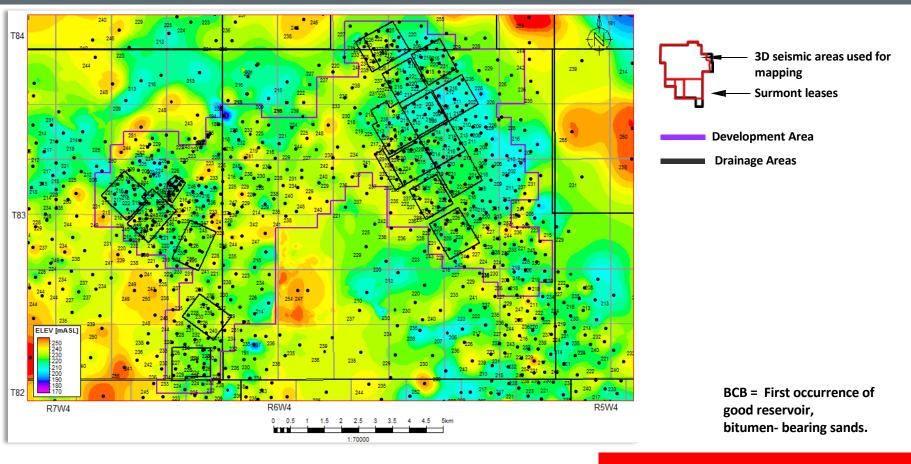
Top Continuous Bitumen Structure

2016/2017 Delineation Campaign Update

- Minor changes due to:
 - Geological picks from new Wells
 - Re-evaluated/unified geologic picks
 - Revised Seismic Interpretation



McMurray Base Continuous Bitumen Structure



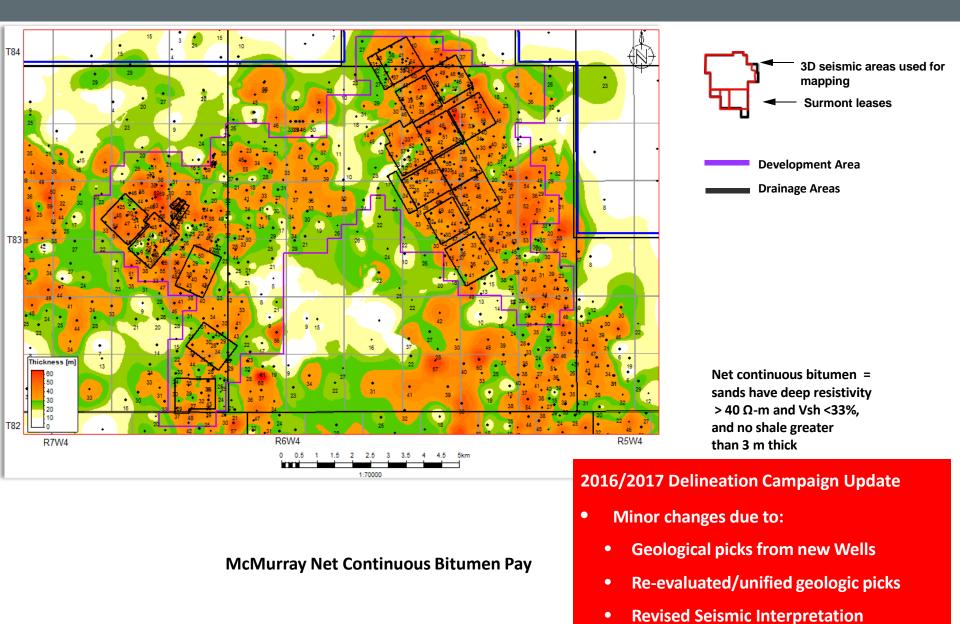
Base Continuous Bitumen Structure

2016/2017 Delineation Campaign Update

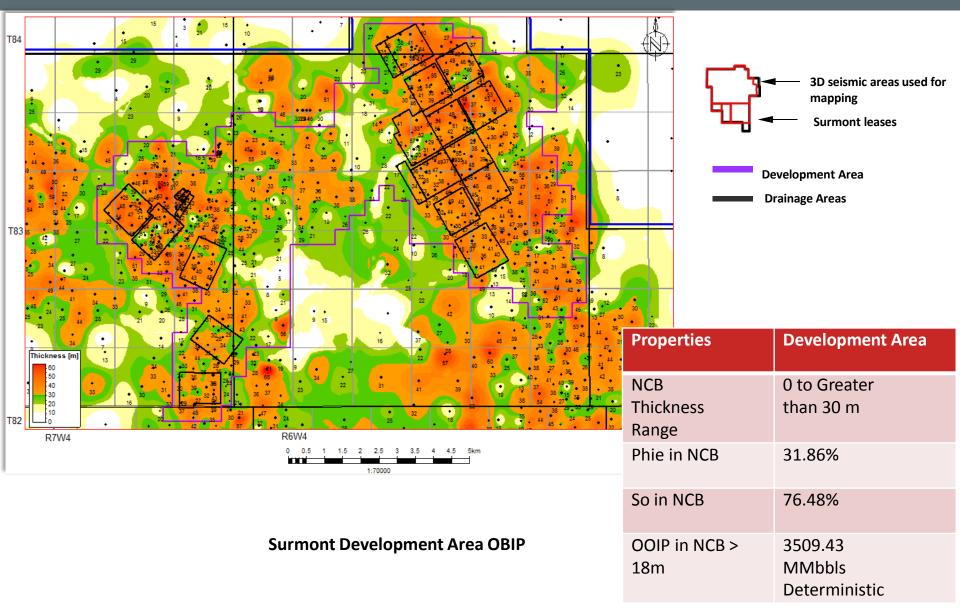
- Minor changes due to:
 - Geological picks from new Wells
 - Re-evaluated/unified geologic picks
 - Revised Seismic Interpretation



McMurray Net Continuous Bitumen Thickness



Surmont Leases OBIP

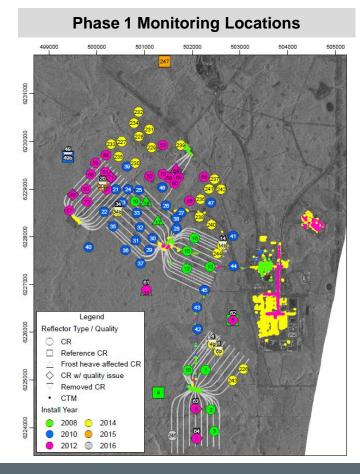


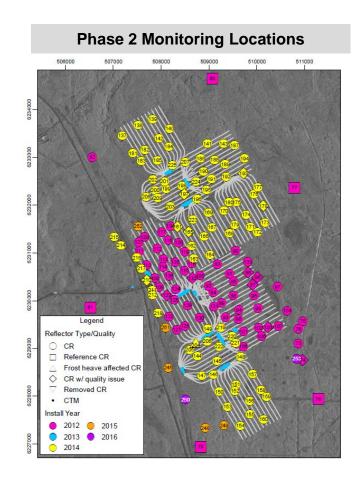
OBIP = Thickness x Phie x So x Area



Surface Deformation Monitoring

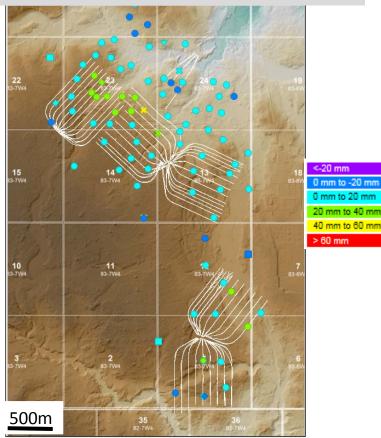
- Satellite (RADARSAT-2) measurements every 24 days
- Interferometric Synthetic Aperture Radar (InSAR):
 - Corner Reflectors (CR) installed over pads and in areas to measure background deformations
 - 256 CR's installed since monitoring program began in 2008





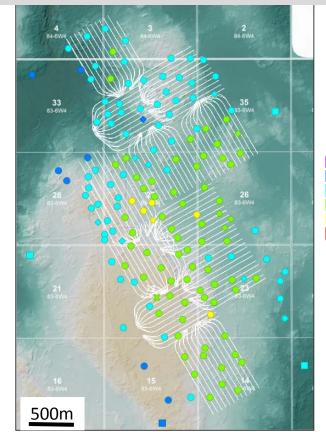
InSAR Surface Deformation Monitoring

Vertical Deformation *Dec 30 2015 to Mar 1 2017* (Surmont 1)



• Deformation currently in line with expectations

Vertical Deformation *Dec 30 2015 to Mar 1 2017* (Surmont 2)



○ Corner Reflector
 □ Reference Corner Reflector
 ◇ Corner Reflector w/quality issue
 ☆ Corner Reflector w/Frost Jacking

<-20 mm

> 60 mm

ConocoPhillips

0 mm to -20 mm

0 mm to 20 mm

20 mm to 40 mm

40 mm to 60 mm

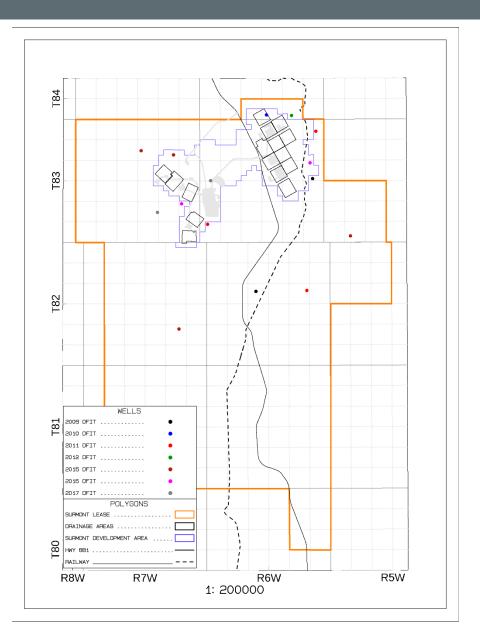
Subsection 3.1.1 (2k; 2j)

Caprock Integrity

- Caprock Core Analysis:
 - 14 caprock cores were drilled and analyzed in 2015-2017.
 - Four rock mechanics testing programs were conducted in 2015-2017.
- Diagnostic Fracture Injectivity Tests (DFITs):
 - 8 DFITs were carried out in 2015-2017
 - DFIT locations were selected based on structural and geomechanical analysis of the caprock.
- The completed analysis verified that
 - The best seals within the cap rock interval are the deeper water deposits occurring on maximum flooding surfaces.
 - The seal over the development area is continuous, consistent and laterally extensive.

Conclusions from the study:

- Best Seal: Deeper water deposits
- Muds are more than 80% clay and are correlated throughout and beyond the Surmont lease.
- The mechanical properties of the caprock allow for providing a continuous seal over the steam chamber.





Maximum Operating Pressure

- ConocoPhillips Canada continues to propose a flexible tapered strategy envelope bound by the cap rock integrity study and the associated Maximum Operating Pressure (MOP) on one side and economic achievable pressures on the other side.
- The DFITs are strategically placed to characterize stress changes due to structural changes while measuring the baseline stresses in the caprock.
- Wellbore image log and other open-hole logs were analyzed in detail for stress analysis and natural fractures characterization.
- The results suggest while the previously used value of 18.4 kPa/m is valid, the minimum horizontal stress is higher in several drainage areas.
- In 2016, ConocoPhillips received approval from the AER to increase the MOP in one of the drainage areas.
- ConocoPhillips Canada has submitted an application to temporarily increase MOP in one of the drainage areas at Phase 2.
- In the future, select drainage areas may be investigated for potential application of higher MOP.

Conclusions from the study:

- The results suggest that in many parts of Surmont the caprock minimum horizontal stress is above the used value of 18.4 kPa/m in the MOP calculation.
- While the recommended 15 kPa/m MOP gradient is verified and valid, higher MOP gradient will be requested for select drainage areas.

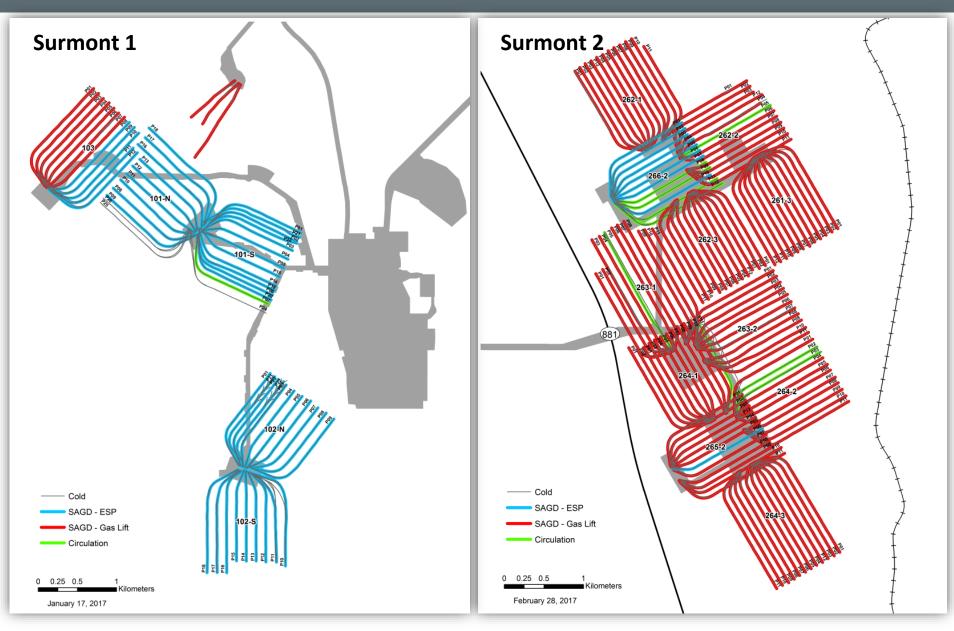




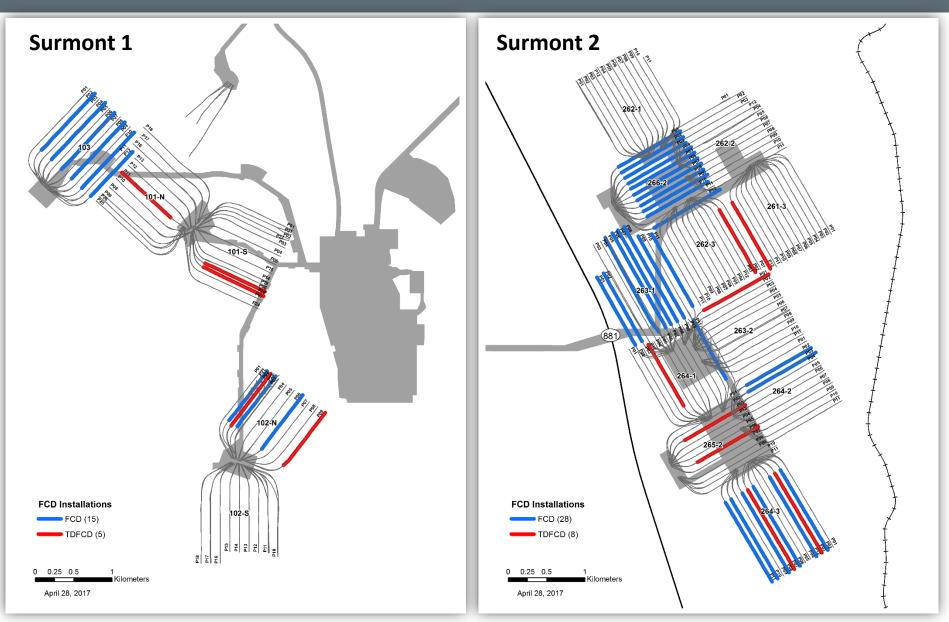
Drilling and Completions

Subsection 3.1.1 (3)

One Surmont Well Summary



FCD Installations





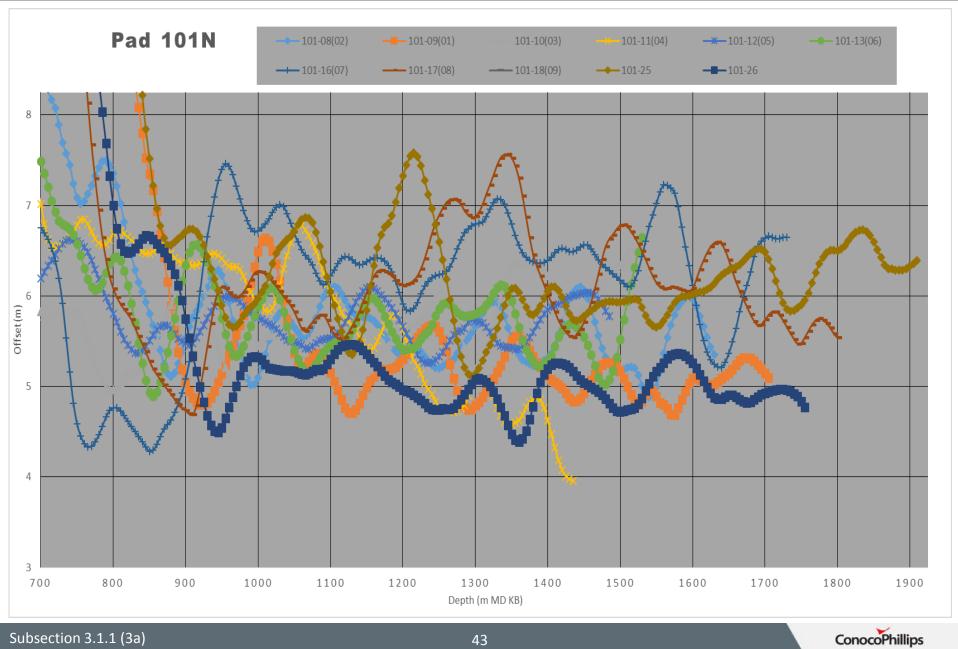
2016 Re-Drills

• In 2016 we had a total of 5 re-drills.

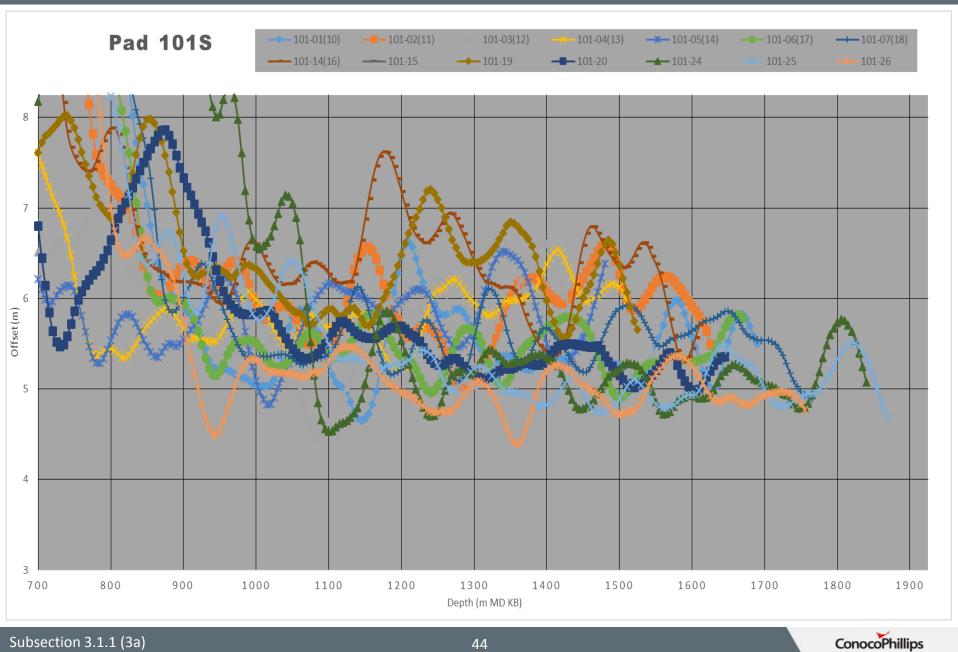
	264-2 P02	264-2 P03	266-2 P12	263-1 105	263-1 P05
Redrill Type	Whipstock	Whipstock	Whipstock	Whipstock	Whipstock
Reason for Redrill	failure during circulation phase. Production tubing was unable to be recovered due to sand.		Intermediate casing was found to be damaged in McMurray formation after initial drilling operation. Attempts to remedy the sand control issue was not successful.	Liner failure during circulation phase discovered at time of P05 Redrill. Production tubing was unable to be recovered due to sand.	Liner failure during circulation phase. Production tubing was unable to be recovered due to sand as well as casing damage in McMurray
Whipstock Depth (mKB)	481	423	734	408	364
Whipstock Depth (mTVD)	339	334	322	328	317
Liner Length (m)	1156	1224	1096	1557	1629
FCD interval Length (m)	952	1035	1002	1369	1402
Completion	7" heel, 4" toe with 5/8" TC string on outside of toe string	Not yet completed.	7" heel, 4" toe with 1.25" Fiber string ran inside toe string	7" heel, 4" toe with no TC's installed	7" heel, 4" toe with 5/8" TC string on outside of toe string
Comments	Successfully drilled, completed and put on steam circulation Dec 2016	Successfully drilled. Completion encountered difficulty with sand incursion. Currently investigating.	Successfully drilled, completed and put on steam circulation Dec 2016	Successfully drilled and completed. Awaiting P05 completion before starting on circulation Q1 2017	Successfully drilled. Completion operation to be executed shortly.



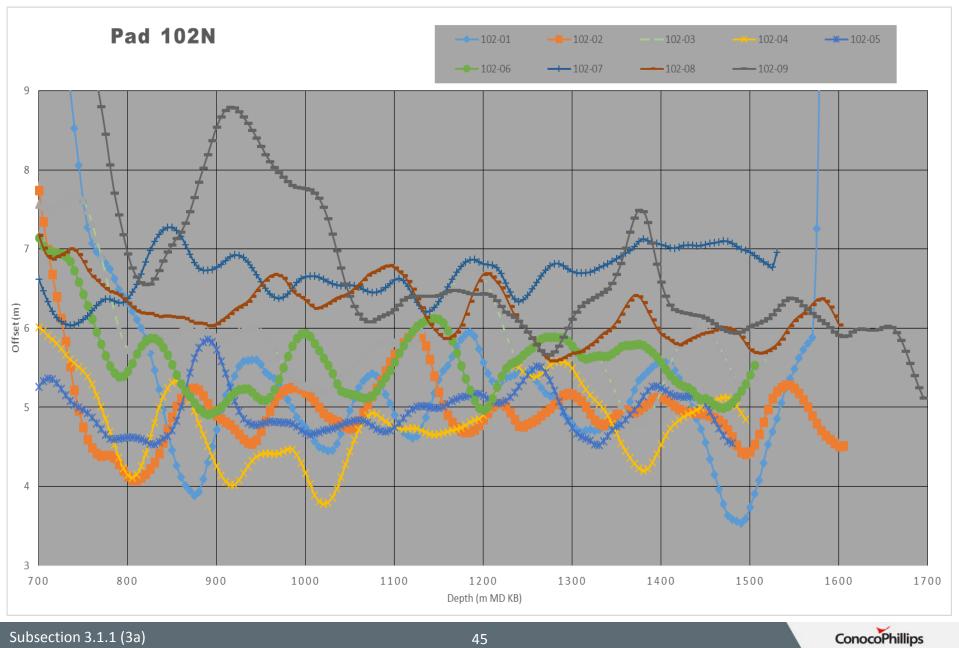
Well Pad 101 North Producer and Injector Vertical Offset



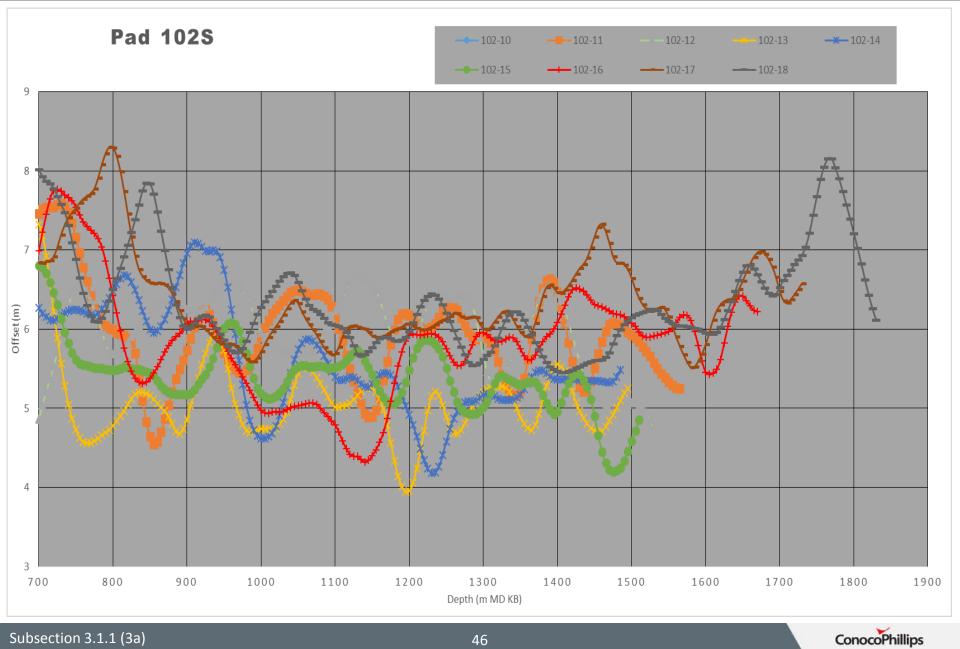
Well Pad 101 South Producer and Injector Vertical Offset



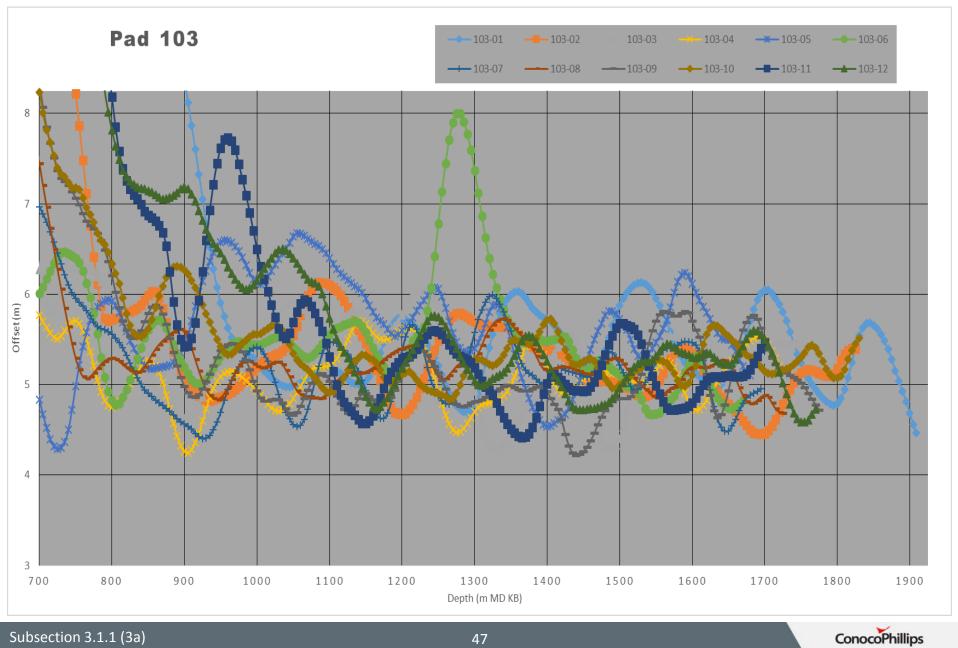
Well Pad 102 North Producer and Injector Vertical Offset



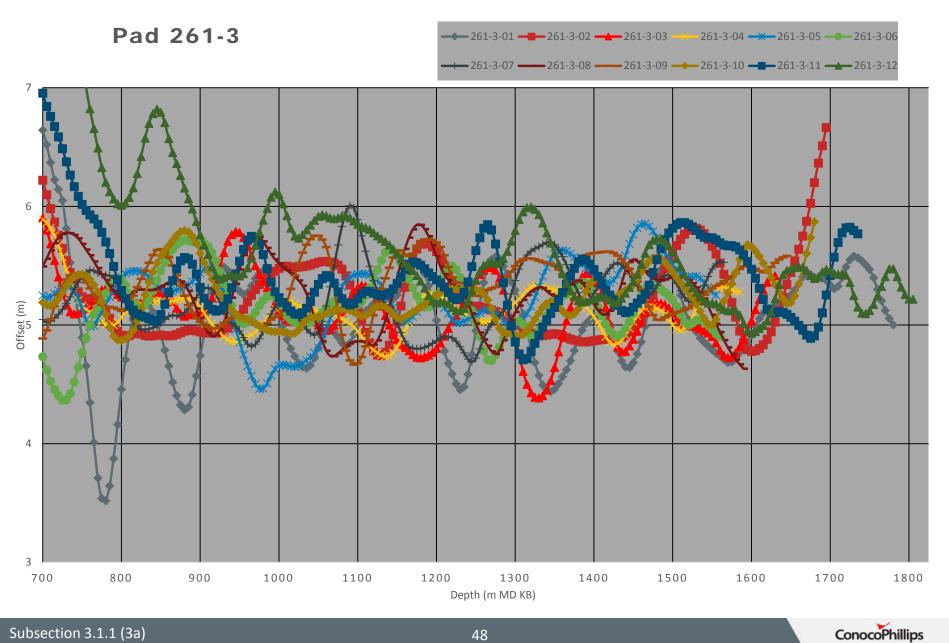
Well Pad 102 South Producer and Injector Vertical Offset



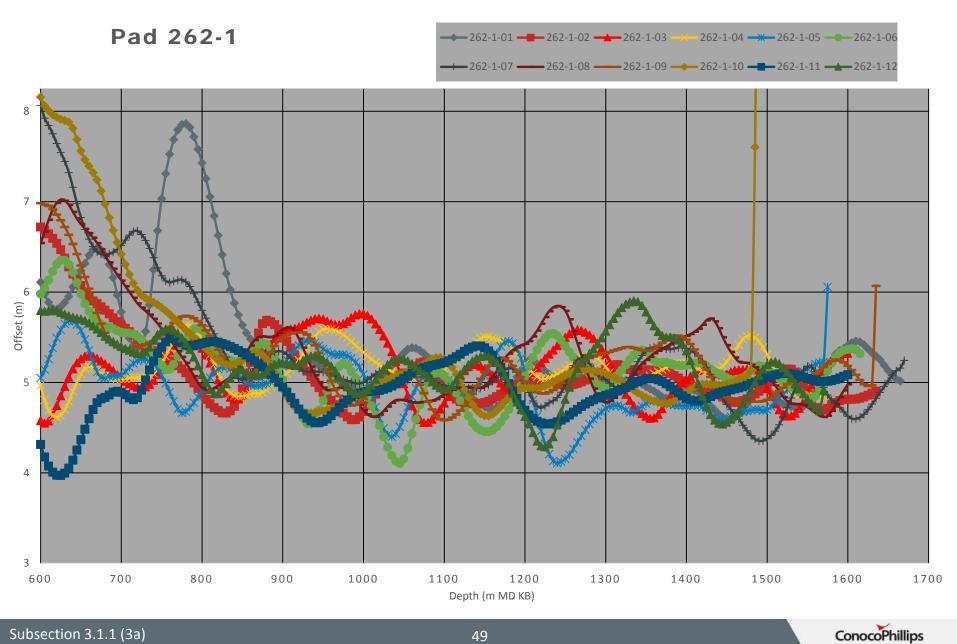
Well Pad 103 Producer and Injector Vertical Offset



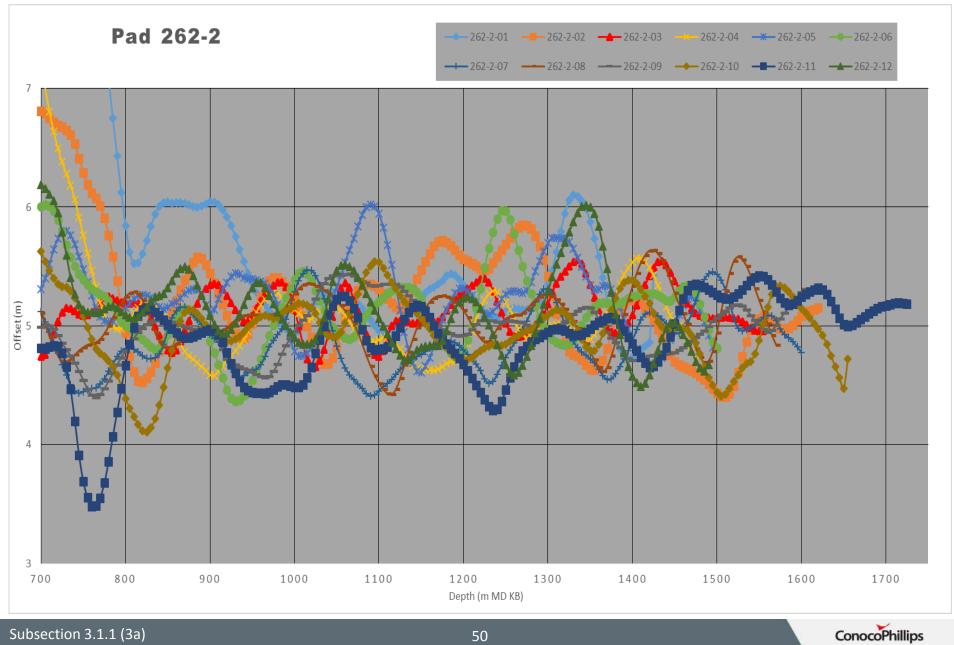
Well Pad 261-3 Producer and Injector Vertical Offset



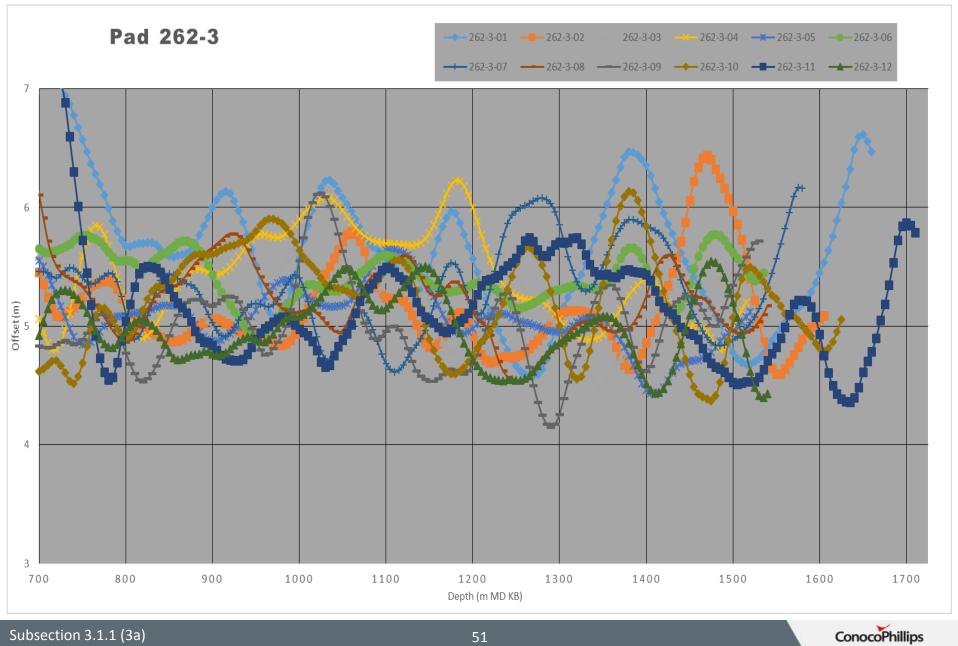
Well Pad 262-1 Producer and Injector Vertical Offset



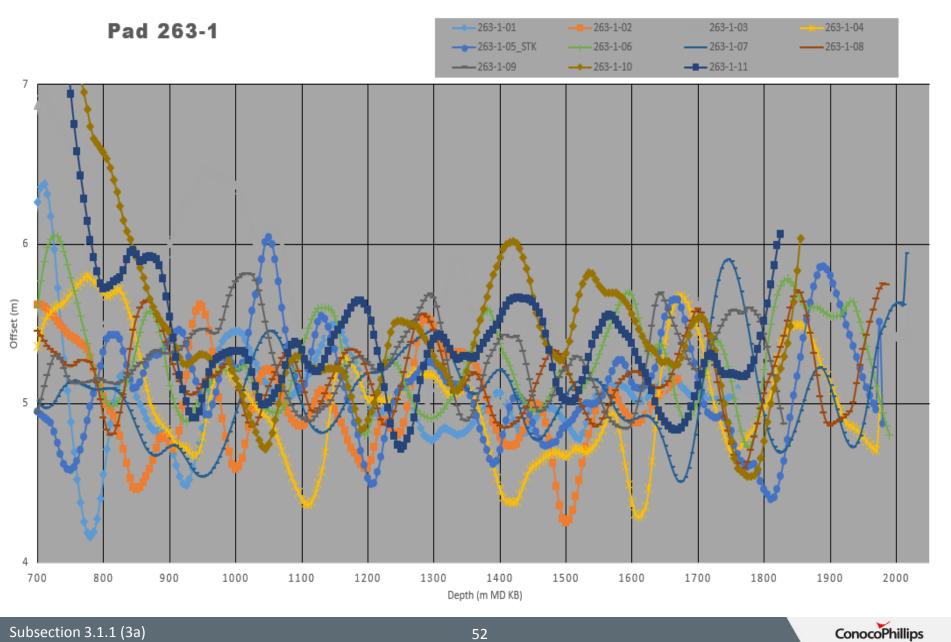
Well Pad 262-2 Producer and Injector Vertical Offset



Well Pad 262-3 Producer and Injector Vertical Offset

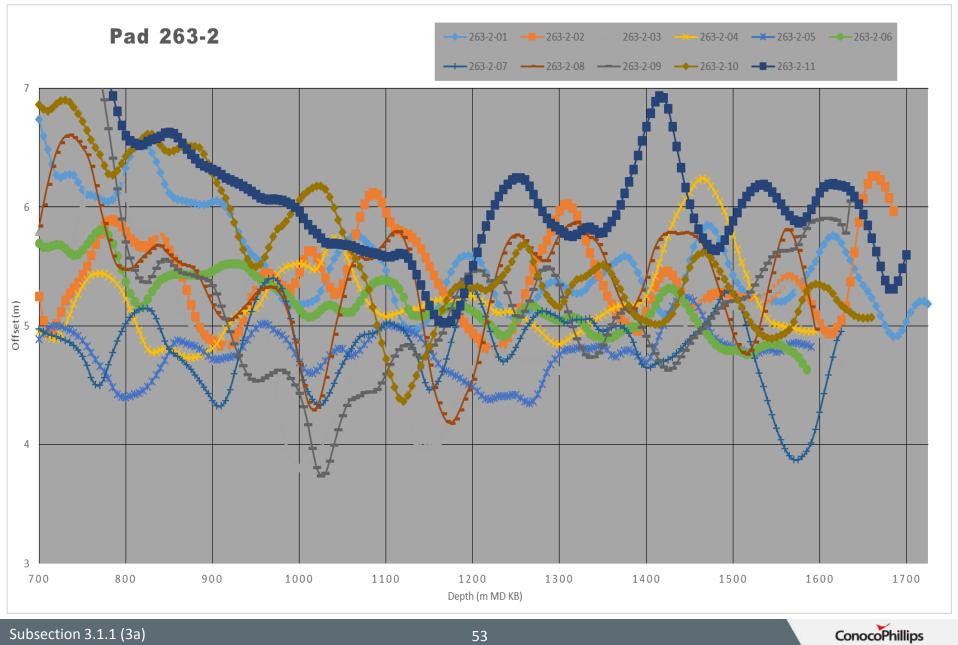


Well Pad 263-1 Producer and Injector Vertical Offset

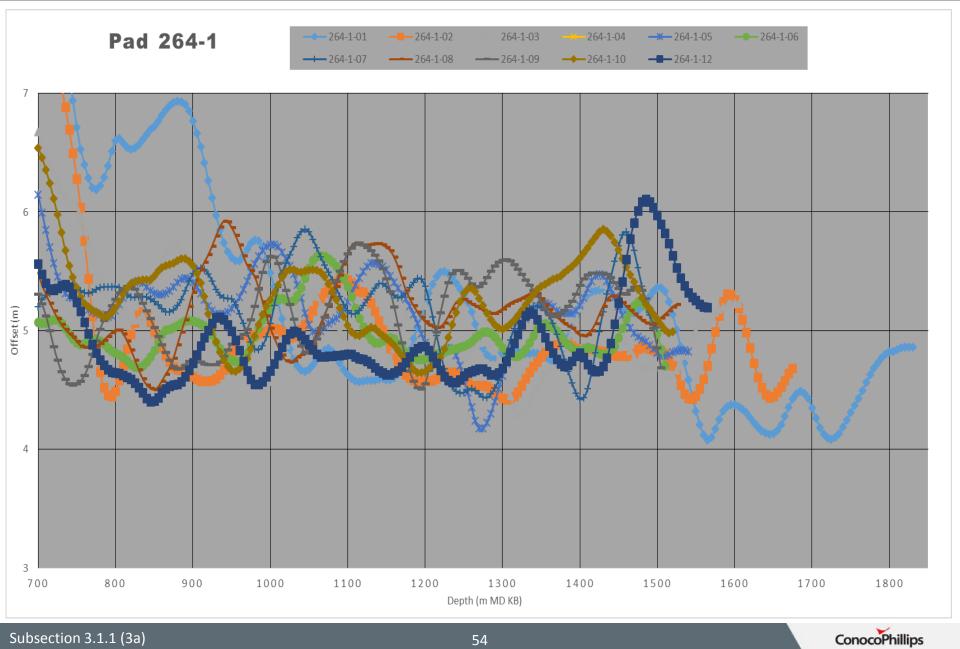


Subsection 3.1.1 (3a)

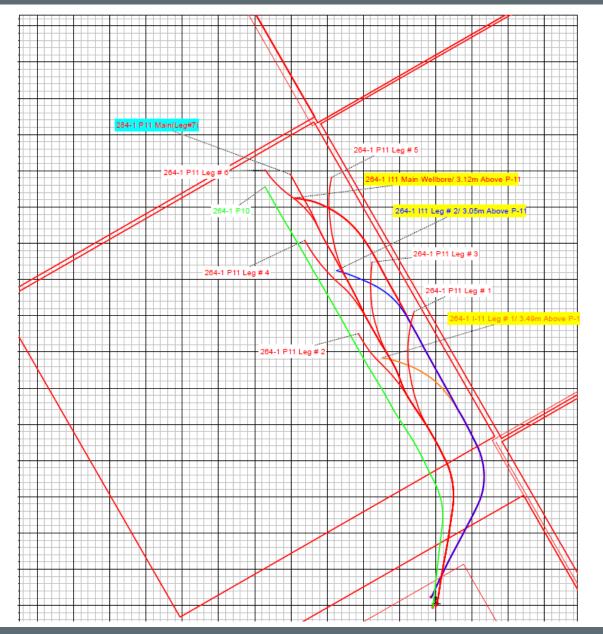
Well Pad 263-2 Producer and Injector Vertical Offset



Well Pad 264-1 Producer and Injector Vertical Offset



Well Pad 264-1-11 Fishbone Producer and Injector Vertical Offset

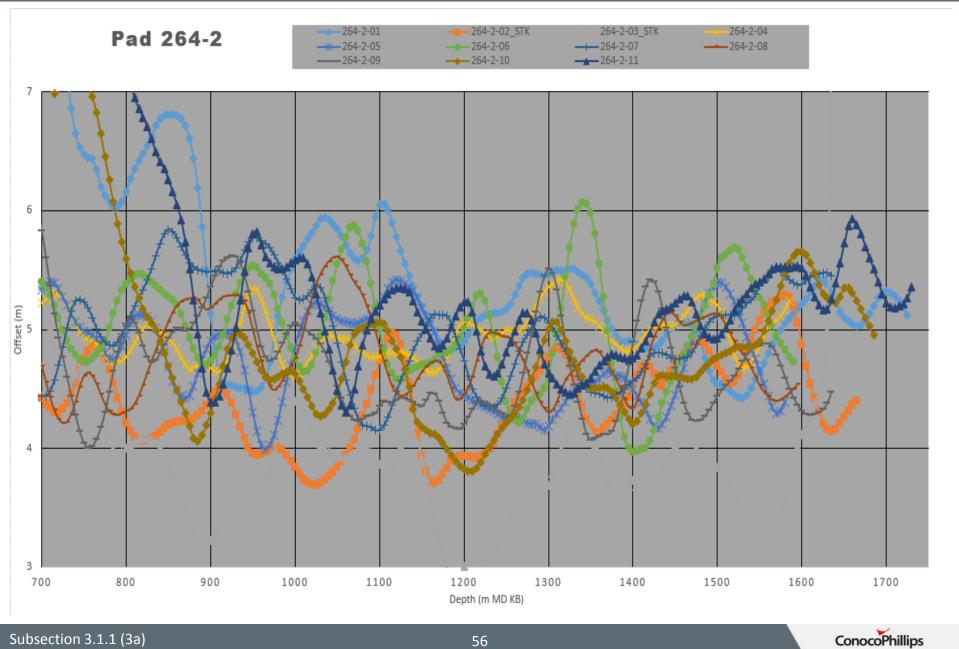


Injector has 3 legs while producer has 7 legs. 3 vertical offsets.

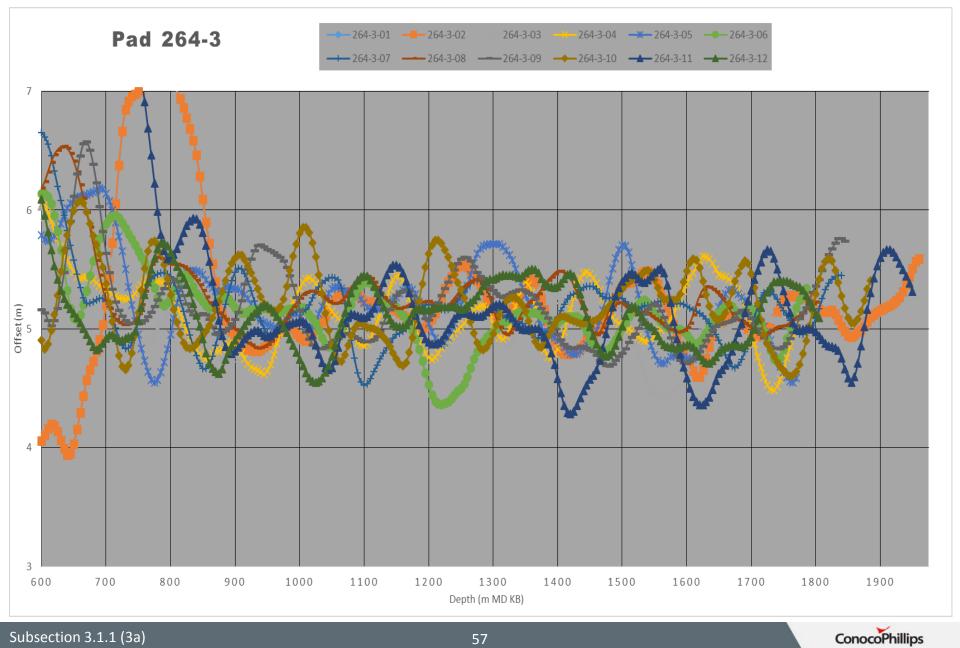




Well Pad 264-2 Producer and Injector Vertical Offset

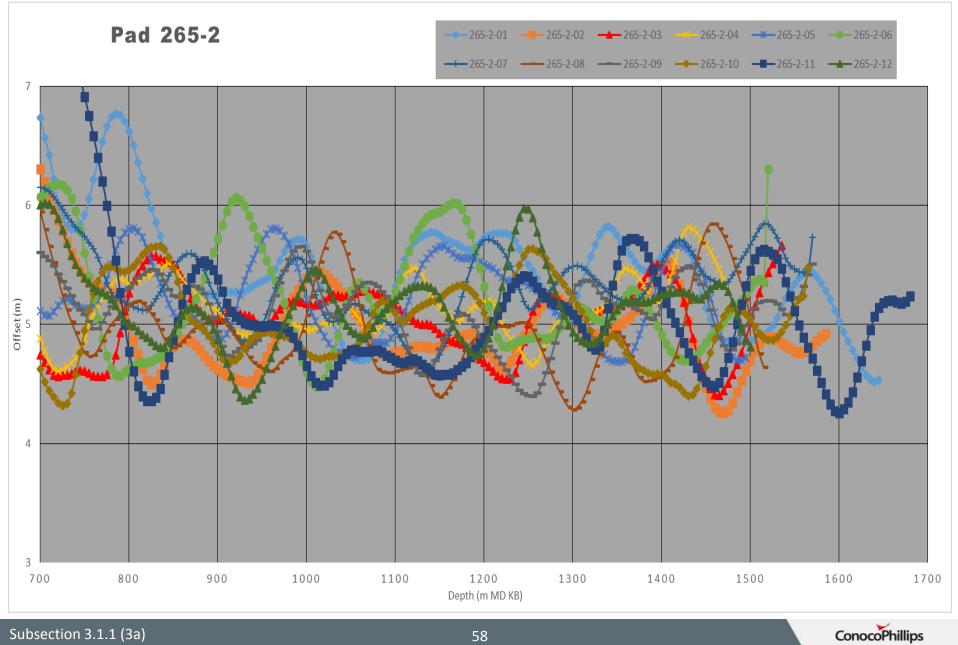


Well Pad 264-3 Producer and Injector Vertical Offset

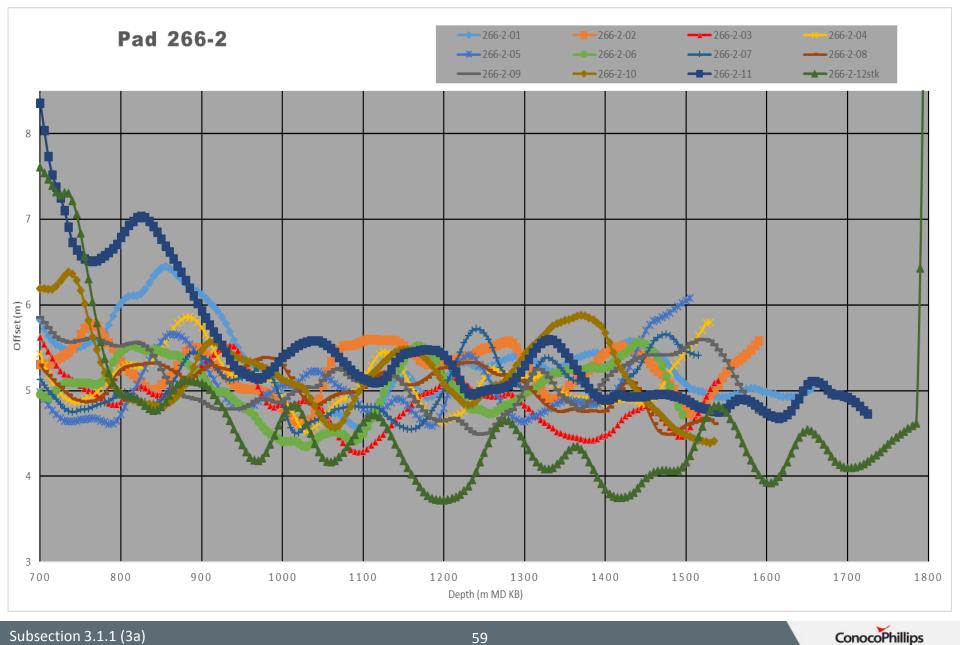


Subsection 3.1.1 (3a)

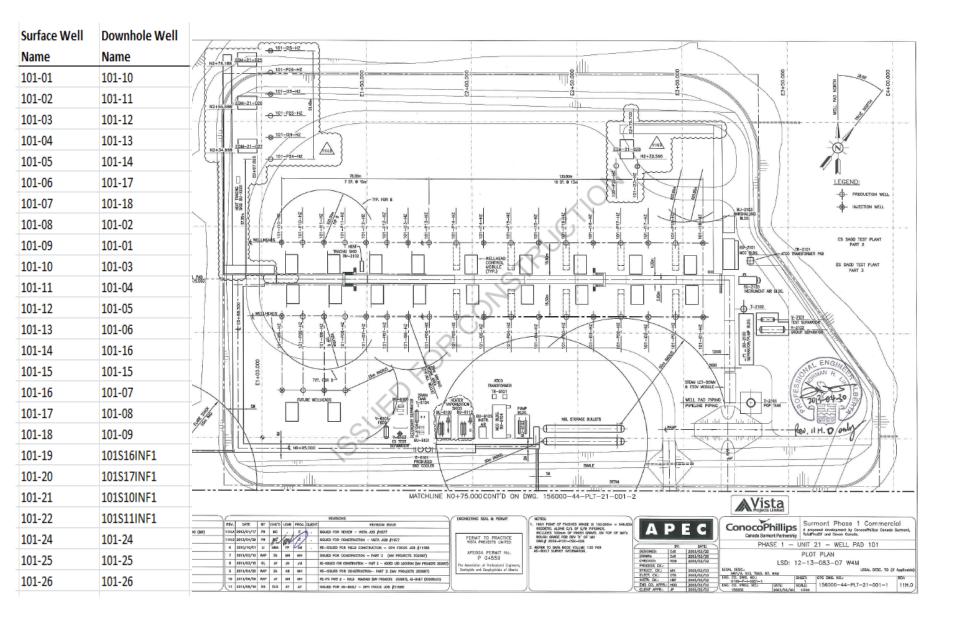
Well Pad 265-2 Producer and Injector Vertical Offset



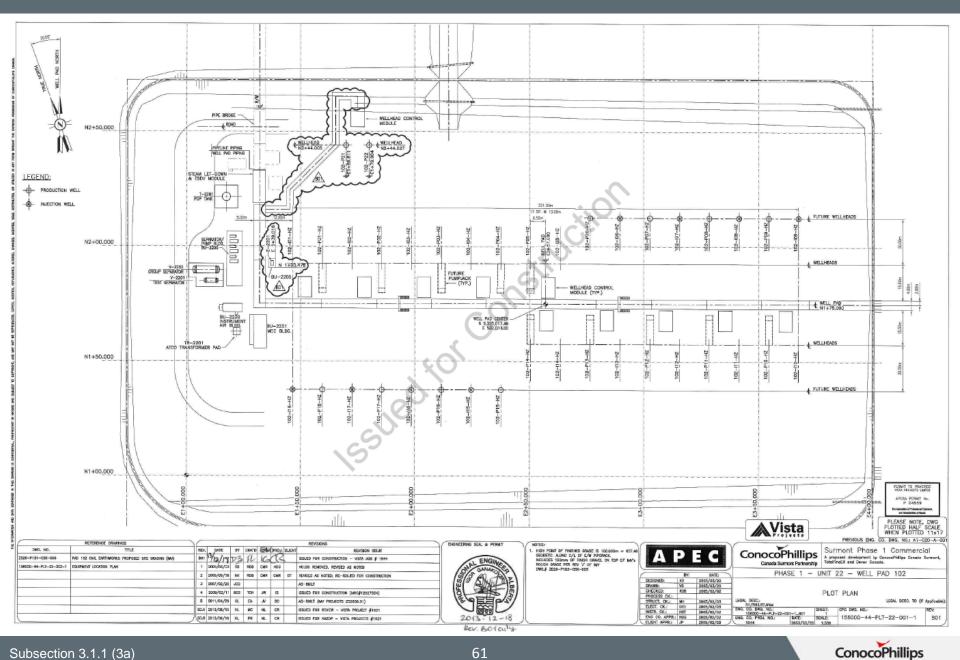
Well Pad 266-2 Producer and Injector Vertical Offset



Pad 101 Plot Plan



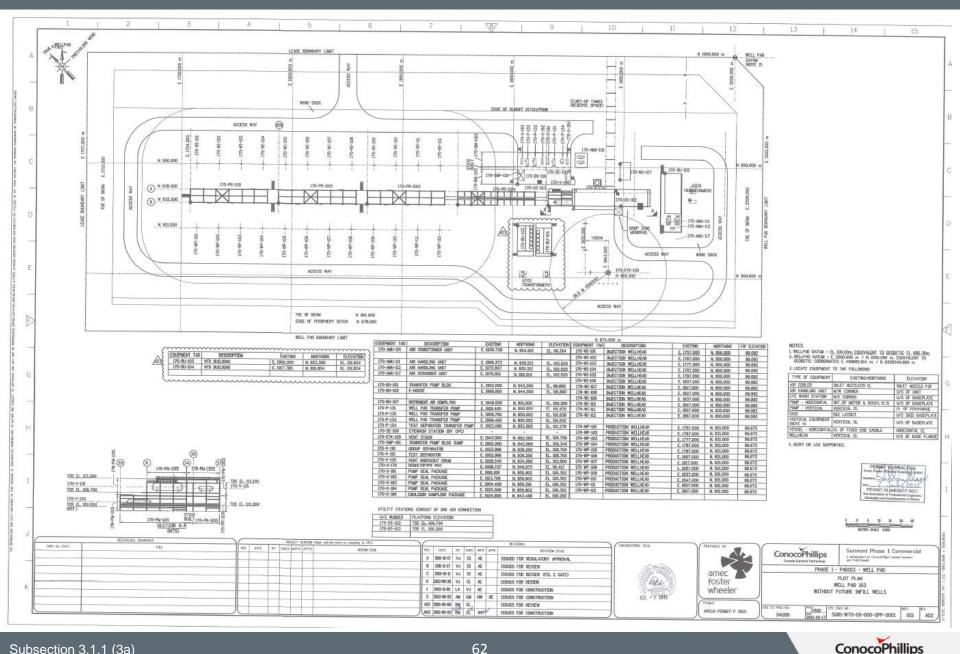
Pad 102 Plot Plan



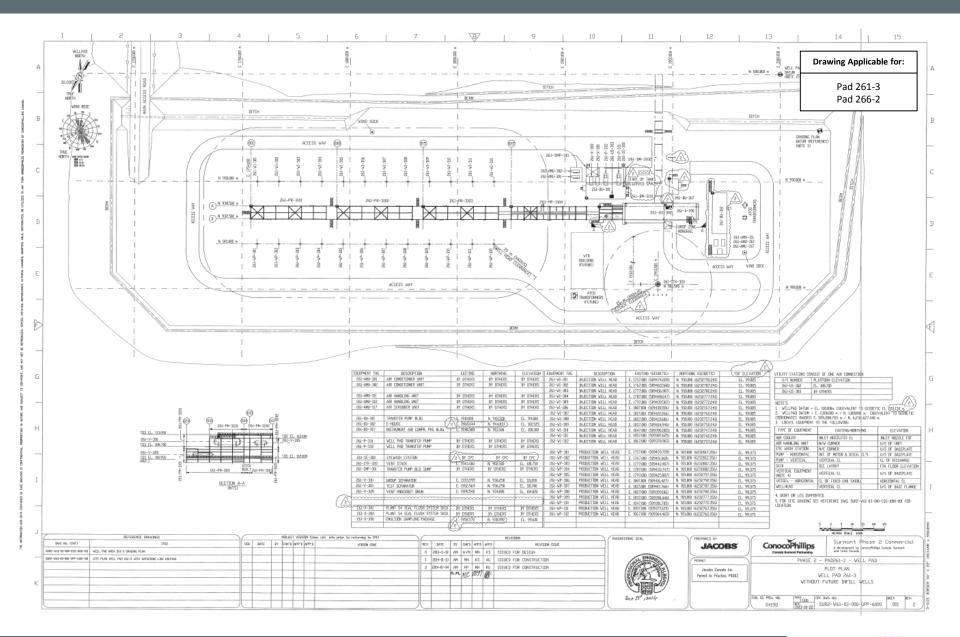
Subsection 3.1.1 (3a)

61

Pad 103 Plot Plan

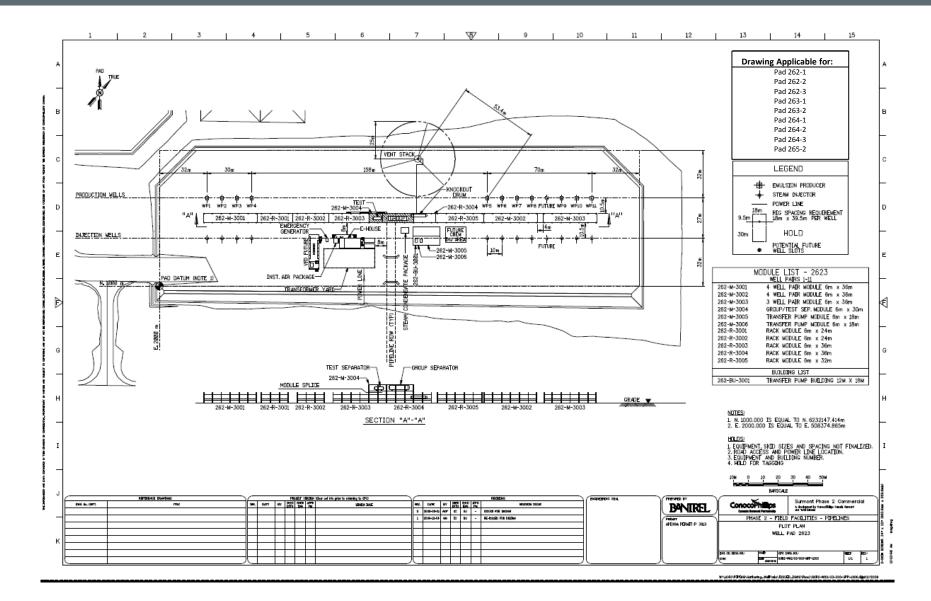


Jacobs S2 Pad Design



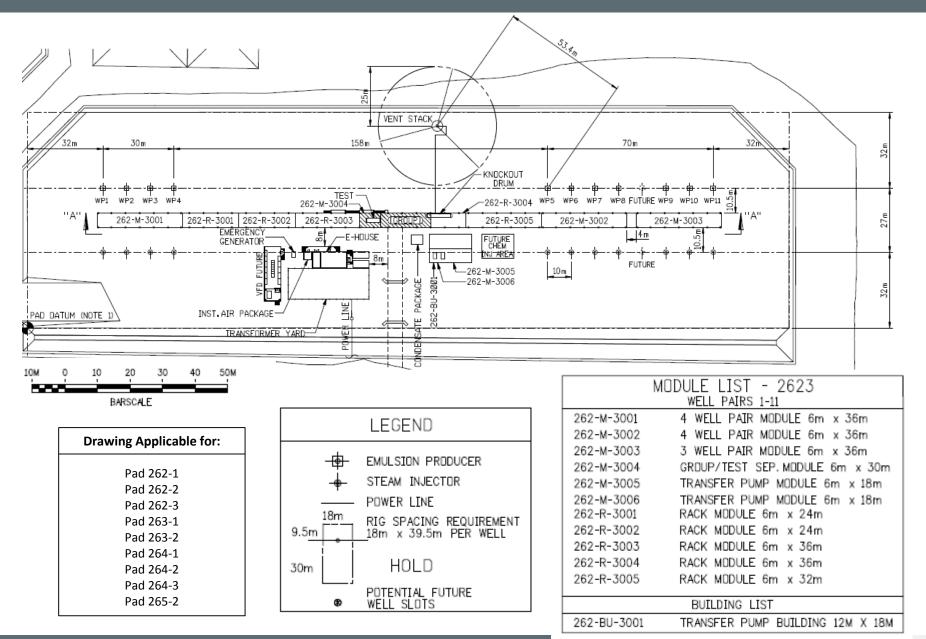


Bantrel S2 Pad Design





Bantrel S2 Pad Design



Pad 101, 102 & 103 Well Completions

Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
101-01 (10DH)	ESP	Parallel	102-1	ESP	Parallel	103-1	Improved Gas Lift Producer A	Concentric
101-02 (11DH)	ESP	Parallel	102-2	ESP (TDFCD)	Parallel		Improved Gas Lift Producer A	Concentrie
101-03 (12DH)	ESP	Concentric	102-3	РСР	Parallel	103-2	(FCD)	Concentric (FCD)
101-04 (13DH)	ESP	Parallel	102-4	ESP	Parallel	103-3	Improved Gas Lift Producer A	Concentric
101-05 (14DH)	ESP	Parallel	102-5	ESP	Parallel		Improved Gas Lift	
101-06 (17DH)	ESP(TDFCD)	Concentric	102-6	ESP (FCD)	Parallel	103-4	Producer A (FCD)	Concentric (FCD)
101-07 (18DH)	Gas Lift	Concentric	102-7	ESP	Concentric	103-5	Improved Gas Lift Producer A	Concentric
101-08 (02DH)	ESP	Concentric	102-8	ESP	Concentric	103-5	Improved Gas Lift	
101-09 (01DH)	ESP	Concentric	102-9	ESP (TDFCD)	Concentric	103-6	Producer A (FCD)	Concentric (FCD)
101-10 03DH)	ESP	Concentric	102-10	ESP	Concentric	102 7	Improved Gas Lift	
101-11 (04DH)	ESP(TDFCD)	Concentric	102-11	ESP	Concentric	103-7	Producer A	Concentric Concentric
101-12 (05DH)	ESP	Concentric	102-12	ESP	Parallel	103-8	ESP (FCD)	(FCD)
101-13 (06DH)	ESP	Concentric	102-13	ESP	Parallel	103-9	ESP	Concentric Concentric
101-14 (16DH)	ESP	Parallel	102-14	ESP	Parallel	103-10	ESP (FCD)	(FCD)
101-15 (15DH)	ESP	Parallel	102-15	ESP	Concentric	103-11	ESP	Concentric
101-16 (07DH)	ESP	Parallel	102-16	ESP	Concentric	103-12	ESP (FCD)	Concentric (FCD)
101-17 (08DH)	ESP	Parallel	102-17	ESP	Concentric		((*)
101-18 (09DH)	ESP	Parallel	102-18	ESP	Concentric			
101-19 (17INF)	ESP	Concentric	102-21 (INF)	PCP (FCD)	N/A			
101-20 (16INF)	ESP(TDFCD)	Concentric	102-22 (INF)	PCP (FCD)	N/A			
101-21 (10INF)	РСР	N/A						
101-22 (11INF)	РСР	N/A						

Pad 261-3 & 262-1 Well Completions

Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
261-3-01	Improved Gas Lift Producer A	Concentric	262-1-01	Improved Gas Lift Producer A	Concentric
261-3-02	Improved Gas Lift Producer A	Concentric	262-1-02	Improved Gas Lift Producer A	Concentric
261-3-03	Improved Gas Lift Producer A	Concentric	262-1-03	Improved Gas Lift Producer A	Concentric
261-3-04	Improved Gas Lift Producer A	Concentric	262-1-04	Improved Gas Lift Producer A	Concentric
261-3-05	Improved Gas Lift Producer A	Concentric	262-1-05	Improved Gas Lift Producer A	Concentric
261-3-06	Improved Gas Lift Producer A	Concentric	262-1-06	Improved Gas Lift Producer A	Concentric
261-3-07	Improved Gas Lift Producer A	Concentric	262-1-07	Improved Gas Lift Producer A	Concentric
261-3-08	Improved Gas Lift Producer A	Concentric	262-1-08	Improved Gas Lift Producer A	Concentric
261-3-09	Improved Gas Lift Producer A	Concentric	262-1-09	Improved Gas Lift Producer A	Concentric
261-3-10	Improved Gas Lift Producer A	Concentric	262-1-10	Improved Gas Lift Producer A	Concentric
261-3-11	Improved Gas Lift Producer A	Concentric	262-1-11	Improved Gas Lift Producer A	Concentric
261-3-12	Improved Gas Lift Producer A	Concentric	262-1-12	Improved Gas Lift Producer A	Concentric

Pad 262-2 & 262-3 Well Completions

Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
262.2.01	Improved Gas Lift			Improved Gas Lift	
262-2-01	Producer A	Concentric	262-3-01	Producer A	Concentric
262-2-02	Improved Gas Lift Producer A	Concentric	262-3-02	Improved Gas Lift Producer A(TDFCD)	Concentric
262-2-03	Improved Gas Lift Producer A	Concentric	262-3-03	Improved Gas Lift Producer A	Concentric
262-2-04	Improved Gas Lift Producer A	Concentric	262-3-04	Improved Gas Lift Producer A	Concentric
262-2-05	Improved Gas Lift Producer A	Concentric	262-3-05	Improved Gas Lift Producer A	Concentric
262-2-06	Improved Gas Lift Producer A	Concentric	262-3-06	Improved Gas Lift Producer A	Concentric
262-2-07	Improved Gas Lift Producer A	Concentric	262-3-07	Improved Gas Lift Producer A	Concentric
262-2-08	Improved Gas Lift Producer A	Concentric	262-3-08	Improved Gas Lift Producer A	Concentric
262-2-09	Improved Gas Lift Producer A	Concentric	262-3-09	Improved Gas Lift Producer A	Concentric
262-2-10	Improved Gas Lift Producer A	Concentric	262-3-10	Improved Gas Lift Producer A	Concentric
262-2-11	Improved Gas Lift Producer A	Concentric	262-3-11	Improved Gas Lift Producer A	Concentric
262-2-12	Improved Gas Lift Producer A	Concentric	262-3-12	Improved Gas Lift Producer A	Concentric

Pad 263-1 & 263-2 Well Completions

Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
262.4.04	Improved Gas Lift	Concentrie	262.2.01	Improved Gas Lift	Concentrie
263-1-01	Producer B(FCD) Improved Gas Lift	Concentric	263-2-01	Producer B(TDFCD) Improved Gas Lift	Concentric
263-1-02	Producer B(FCD)	Concentric	263-2-02	Producer B	Concentric
263-1-03	Improved Gas Lift Producer B	Concentric	263-2-03	Improved Gas Lift Producer B	Concentric
263-1-04	Improved Gas Lift Producer B	Concentric	263-2-04	Improved Gas Lift Producer B	Concentric
263-1-05	Improved Gas Lift Producer B	Concentric (FCD)	263-2-05	Improved Gas Lift Producer B	Concentric
263-1-06	Improved Gas Lift Producer B(FCD)	Concentric	263-2-06	Improved Gas Lift Producer B	Concentric
263-1-07	Improved Gas Lift Producer B(FCD)	Concentric	263-2-07	Improved Gas Lift Producer B	Concentric
263-1-08	Improved Gas Lift Producer B(FCD)	Concentric	263-2-08	Improved Gas Lift Producer B	Concentric
263-1-09	Improved Gas Lift Producer B(FCD)	Concentric	263-2-09	Improved Gas Lift Producer B	Concentric
263-1-10	Improved Gas Lift Producer B	Concentric	263-2-10	Improved Gas Lift Producer B	Concentric
263-1-11	Improved Gas Lift Producer B(FCD)	Concentric	263-2-11	Improved Gas Lift Producer B	Concentric
263-1-01	Improved Gas Lift Producer B	Concentric	263-2-01	Improved Gas Lift Producer B	Concentric

Pad 264-1, 264-2 & 264-3 Well Completions

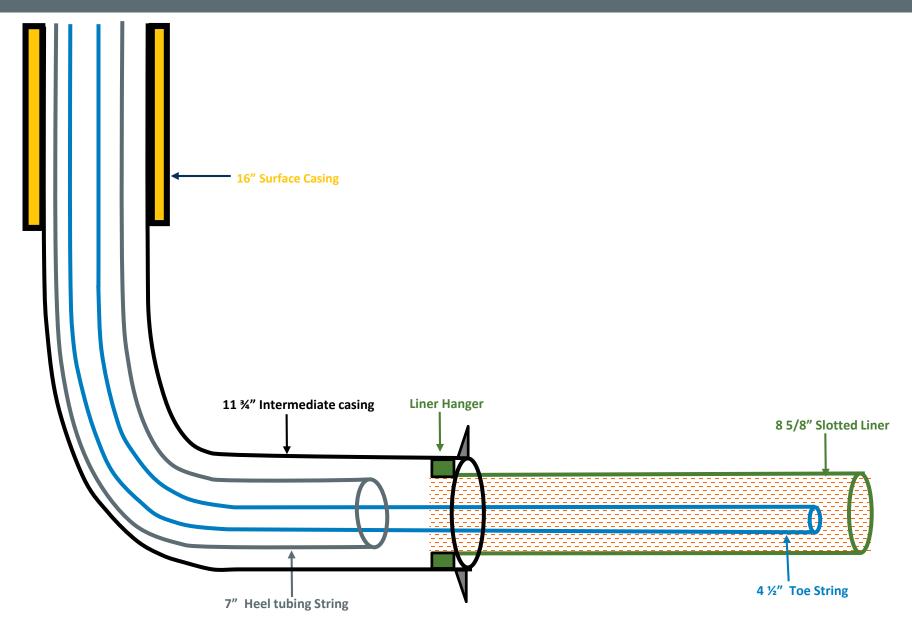
Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
				Increased Coast ift			Improved Gas Lift	
264.4.04	Improved Gas Lift	Companyation	264-2-01	Improved Gas Lift Producer B	Concentric	264-3-01	Producer A	Concentric
264-1-01	Producer A	Concentric	204-2-01	Improved Gas Lift	Concentric	264.2.02	Improved Gas Lift	Companyation
264.4.02	Improved Gas Lift	Companyation	264-2-02	Producer B(FCD)	Concentric	264-3-02	Producer A	Concentric
264-1-02	Producer A	Concentric	204-2-02	FIGURCEI B(FCD)	concentric		Improved Gas Lift	
264 1 02	Improved Gas Lift Producer A	Concentrie	264-2-03	Cold	Concentric	264 2 02	Producer A	Concentrie
264-1-03	Improved Gas Lift	Concentric		Improved Gas Lift		264-3-03	(TDFCD)	Concentric
264-1-04	Producer A	Concentric	264-2-04	Producer B	Concentric	264-3-04	Improved Gas Lift Producer A	Concentric
204-1-04	Improved Gas Lift	Concentric		Improved Gas Lift		204-3-04	Improved Gas Lift	Concentric
264-1-05	Producer A	Concentric	264-2-05	Producer B	Concentric	264-3-05	Producer A	Concentric
204-1-05	Improved Gas Lift	concentric		Improved Gas Lift		204-3-03	Improved Gas Lift	concentric
264-1-06	Producer A	Concentric	264-2-06	Producer B	Concentric		Producer A	
204100	Improved Gas Lift	concentre		Improved Gas Lift		264-3-06	(FCD)	Concentric
264-1-07	Producer A	Concentric	264-2-07	Producer B	Concentric		Improved Gas Lift	Concentre
	Improved Gas Lift	Concentre		Improved Gas Lift			Producer A	
264-1-08	Producer A	Concentric	264-2-08	Producer B	Concentric	264-3-07	(TDFCD)	Concentric
	Improved Gas Lift			Improved Gas Lift			Improved Gas Lift	
264-1-09	Producer A	Concentric	264-2-09	Producer B	Concentric		Producer A	
	Improved Gas Lift			Improved Gas Lift		264-3-08	(FCD)	Concentric
264-1-10	Producer A	Concentric	264-2-10	Producer B	Concentric		Improved Gas Lift	
	Improved Gas Lift			Improved Gas Lift		264-3-09	Producer A	Concentric
	Producer A		264-2-11	Producer B	Concentric		Improved Gas Lift	
264-1-11	(FCD)	Concentric					Producer A	
	Improved Gas Lift					264-3-10	(FCD)	Concentric
	Producer A						Improved Gas Lift	
264-1-12	(TDFCD)	Steam Splitter					Producer A	
						264-3-11	(FCD)	Concentric
							Improved Gas Lift	
							Producer A	
						264-3-12	(FCD)	Concentric



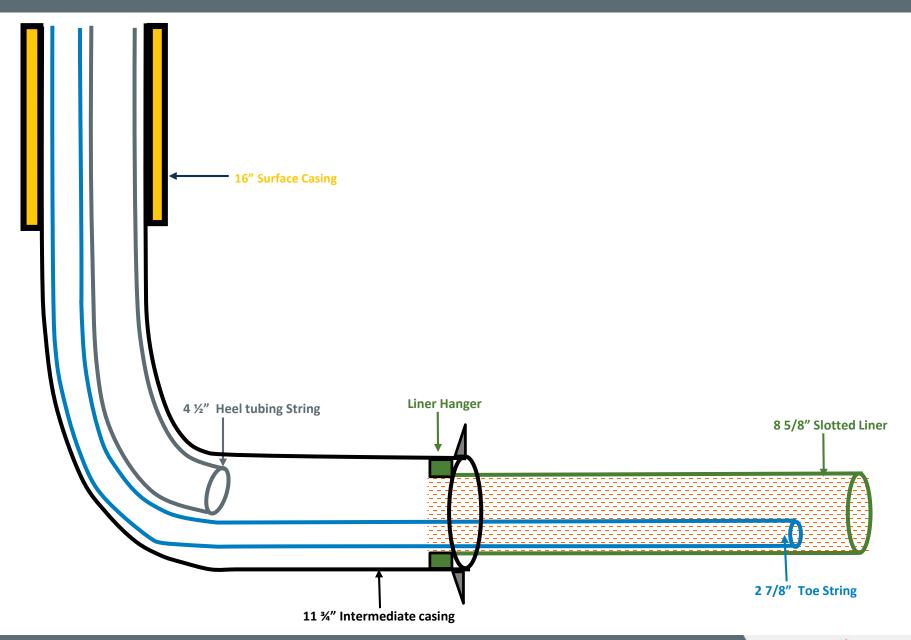
Pad 265-2 & 266-2 Well Completions

Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion	Well Identifier - Surface (Downhole)	Producer Completion	Injector Completion
265-2-01	Improved Gas Lift Producer A	Concentric	266-2-01	ESP (FCD)	Concentric
	Improved Gas Lift		266-2-02	ESP (FCD)	Concentric
265-2-02	Producer A Improved Gas Lift	Concentric	266-2-03	ESP (FCD)	Concentric
265-2-03	Producer A	Concentric	266-2-04	ESP (FCD)	Concentric
265-2-04	Improved Gas Lift Producer A	Concentric	266-2-05	ESP (FCD)	Concentric
265-2-05	Improved Gas Lift Producer A	Steam Splitter	266-2-06	ESP (FCD)	Concentric
265-2-06	ESP (TDFCD)	Concentric	266-2-07	ESP (FCD)	Concentric
265-2-07	ESP	Steam Splitter		Improved Gas Lift Producer A	
265-2-08	ESP	Steam Splitter	266-2-08	(FCD) Improved Gas Lift	Concentric
265-2-09	Improved Gas Lift Producer A	Steam Splitter	266-2-09	Producer A (FCD)	Concentric
265-2-10	Improved Gas Lift Producer A	Concentric	266-2-10	ESP (FCD)	Concentric
265-2-11	Improved Gas Lift Producer A	Steam Splitter	266-2-11	Improved Gas Lift Producer A	Concentric
265-2-12	Improved Gas Lift Producer A	Concentric	266-212	Improved Gas Lift Producer A (FCD)	Concentric

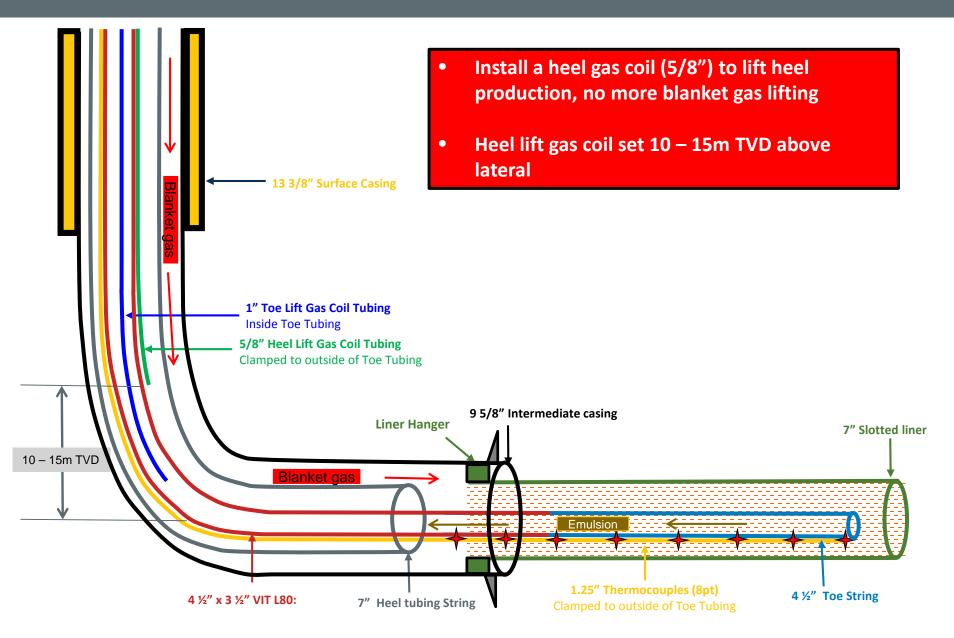
Typical Concentric Injector



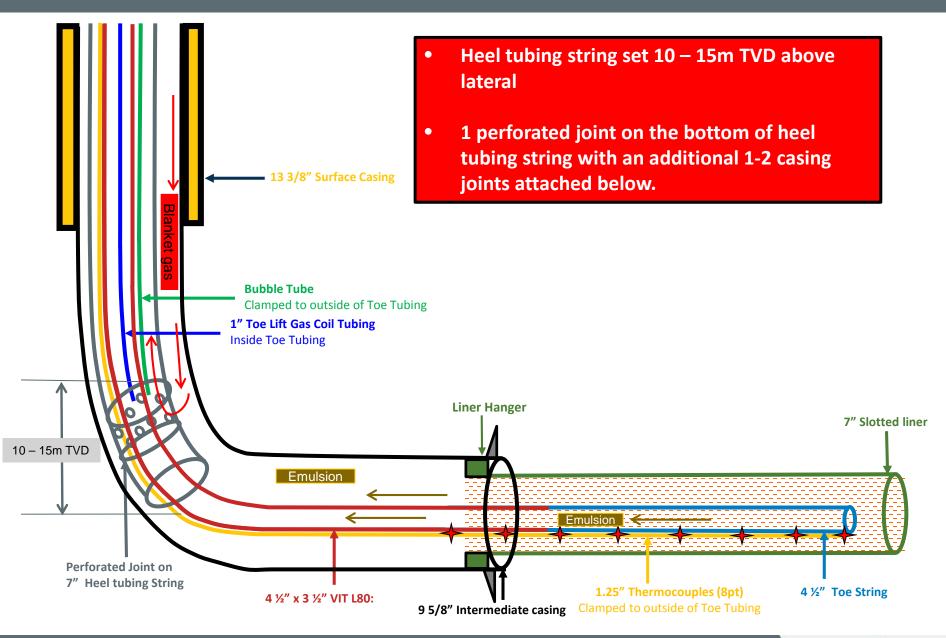
Typical Parallel Injector



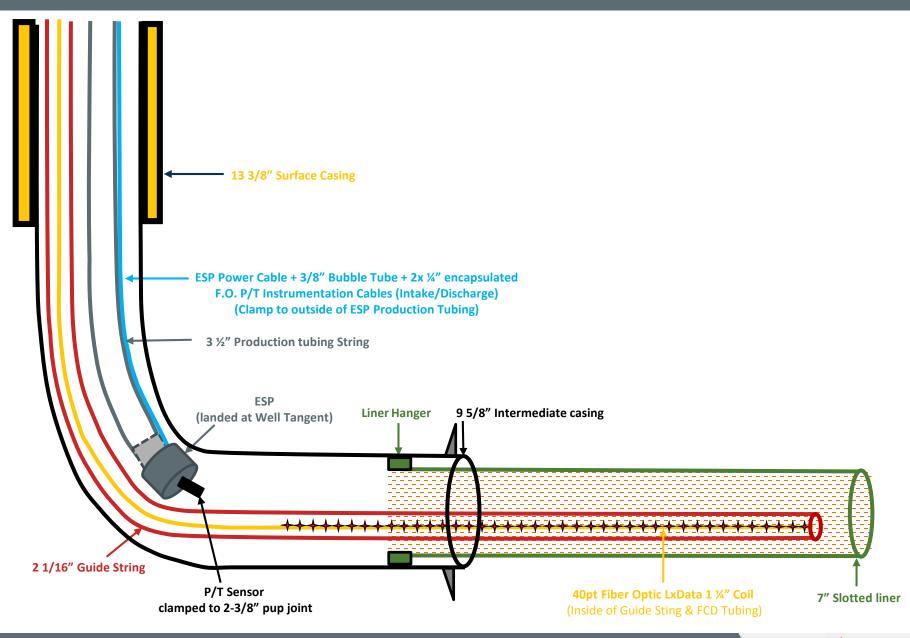
Improved Gas Lift Producer Design, 264-1



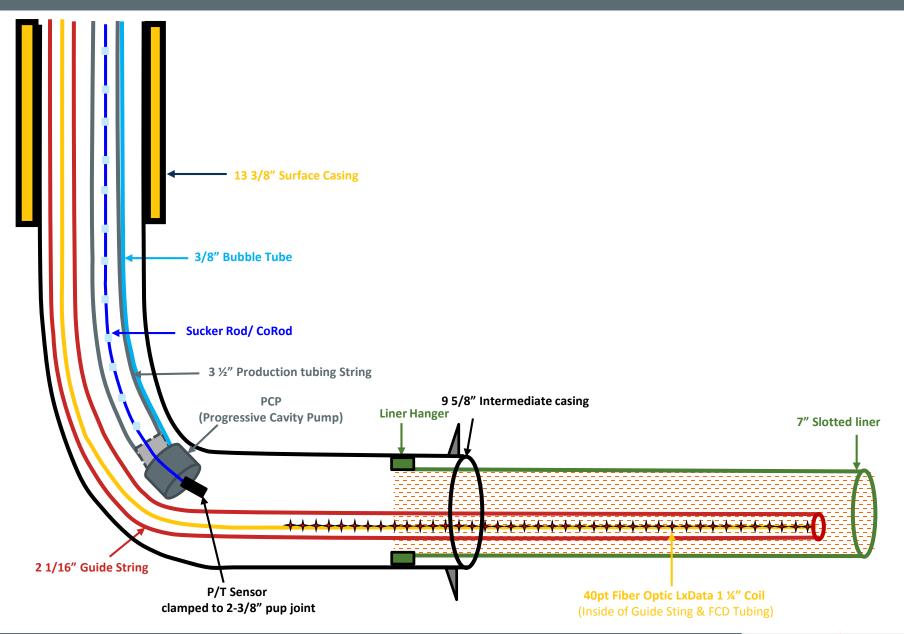
Improved Gas Lift Producer Design, 264-2, 263-2 & 263-1



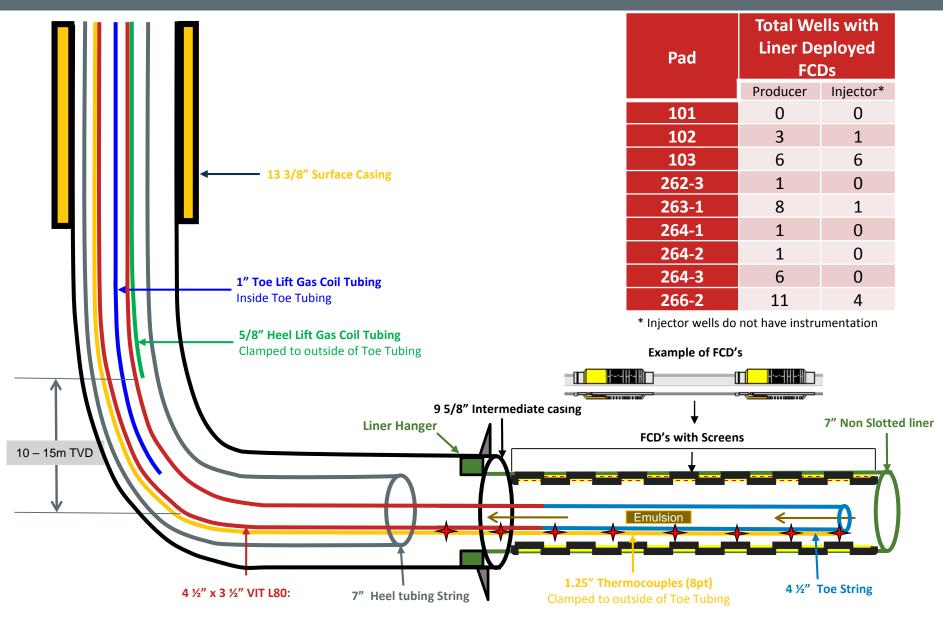
Typical ESP Producer



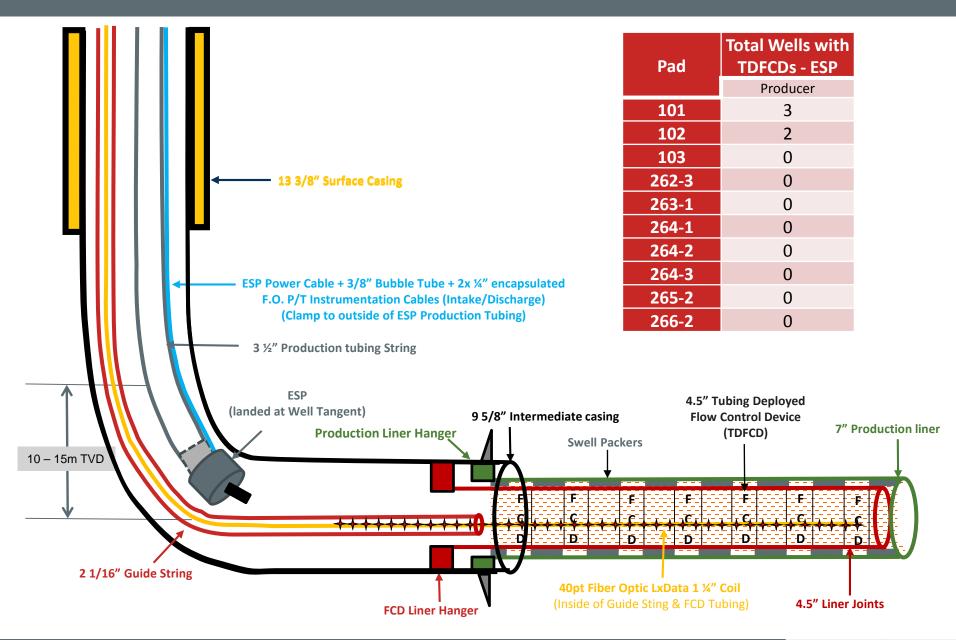
Typical PCP Producer



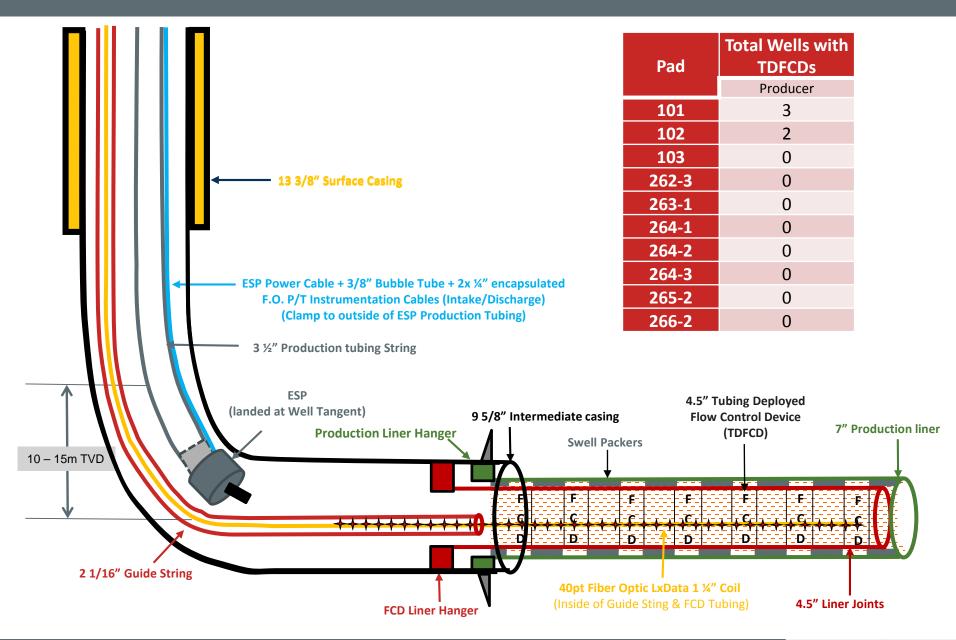
Typical Flow Control Device (FCD) Completion



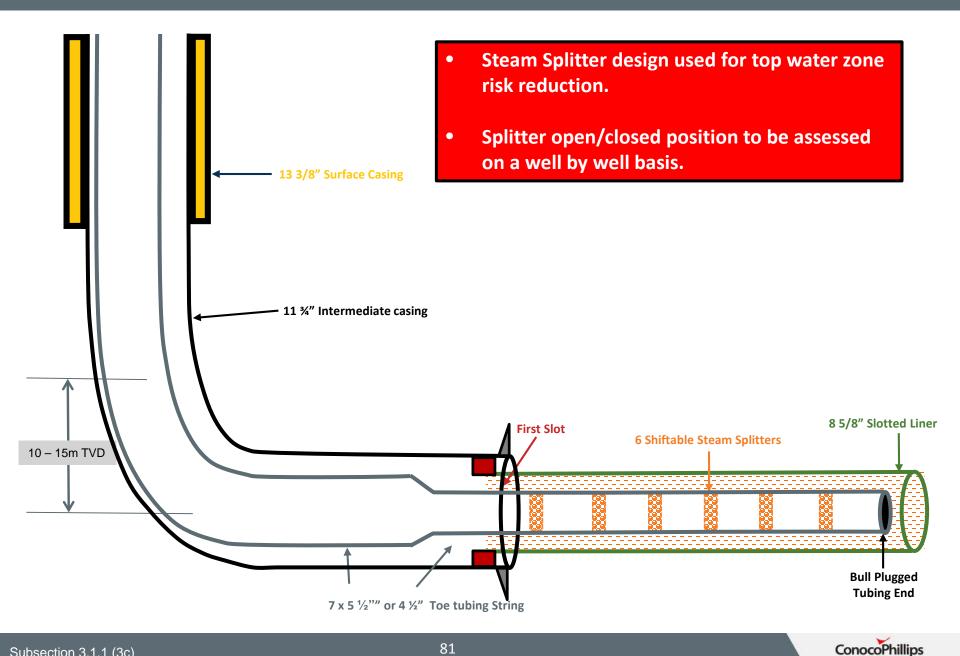
Typical Tubing Deployed FCD (TDFCD) Completion – ESP



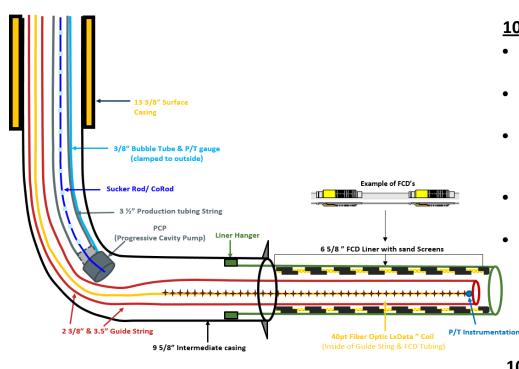
Typical Tubing Deployed FCD (TDFCD) Completion – ESP



Current Surmont 2 Steam Splitter Design

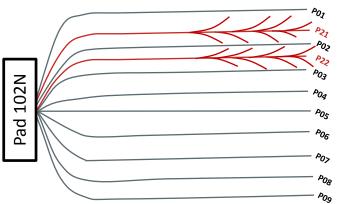


Fishbone Completion Pad 102-P21 & P22 Infills



102-P21 (INF)

- Restarted warmup operations with steam bullheading in Q1 and Q3 2016
- Workover September 2016 to identify previous source of challenges with pump operation
- New PCP pump installed October 2016 and well restarted with steam assist to keep rod torque at manageable levels
- Consistent production from October to present, including improvement in lateral temperatures
- Expecting to remove steam assist as temperatures continue to improve

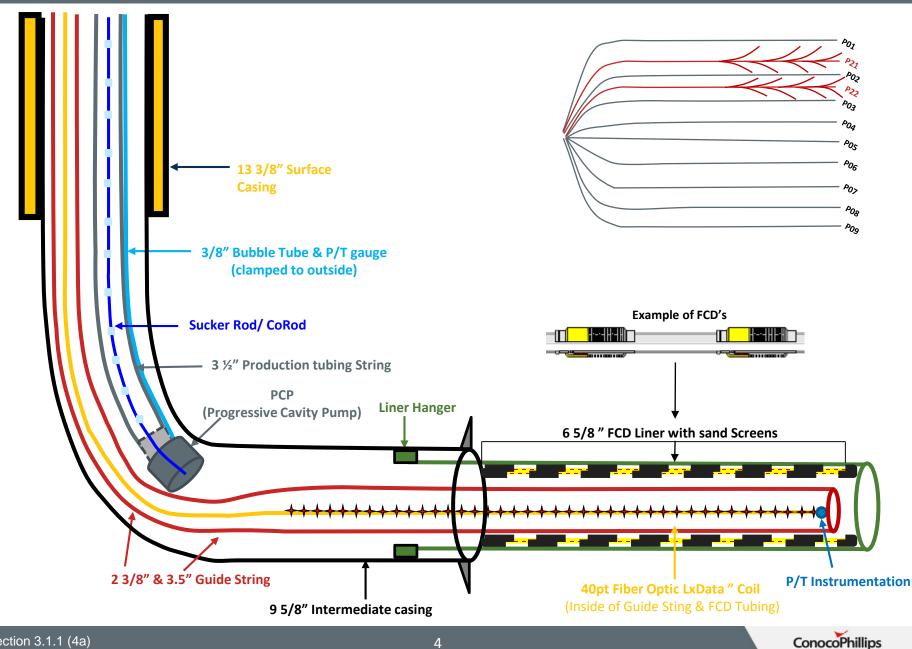


102-P22 (INF)

- Short warmup cycle ran for 2 weeks in Q3 2016. Well has been on standby to use learnings from 102-21
- Downhole temps were showing some improvement along with good injectivity
- Back on warmup Q1 2017 with intention of startup of production with steam assist before Q2 2017



102 P21 Fishbone Completion





Artificial Lift

Subsection 3.1.1 (4)

		Phase 1					Phase 2										
		10	1	10)2	103	261-3	262-1	262-2	262-3	263-1	263-2	264-1	264-2	264-3	265-2	266-2
TOTAL		1	13	1	13	1	1	1	1	1	1	1	1	1	1	1	1
52		2	14	2	14	2	2	2	2	2	2	2	2	2	2	2	2
5		3	15	3	15	3	3	3	3	3	3	3	3	3	3	3	3
		4	16	4	16	4	4	4	4	4	4	4	4	4	4	4	4
107		5	17	5	17	5	5	5	5	5	5	5	5	5	5	5	5
2		6	18	6	18	6	6	6	6	6	6	6	6	6	6	6	6
0		7	19	7		7	7	7	7	7	7	7	7	7	7	7	7
9		8	20	8		8	8	8	8	8	8	8	8	8	8	8	8
7		9	21	9	21	9	9	9	9	9	9	9	9	9	9	9	9
1		10	22	10	22	10	10	10	10	10	10	10	10	10	10	10	10
		11		11		11	11	11	11	11	11	11	11	11	11	11	11
		12		12		12	12	12	12	12			12		12	12	12
ESP		19)	17	7	5	0	0	0	0	0	0	0	0	0	3	8
PCP		2		3	1	0	0	0	0	0	0	0	0	0	0	0	0
GAS LIF	FT	0		0)	7	10	12	7	12	10	10	10	8	12	9	0
SSAGE)	0		0)	0	0	0	2	0	0	0	0	0	0	0	0
RE-CIR	C	0		0)	0	0	0	0	0	0	0	0	0	0	0	0
CIRC		1		0)	0	0	0	0	0	1	0	2	1	0	0	4
OFFLIN	IE	0		0		0	2	0	3	0	0	1	0	1	0	0	0
COLD		0		0		0	0	0	0	0	0	0	0	1	0	0	0



Artificial Lift Types

Gas Lift

- Gas lift is effective with bottom hole flowing pressures >2,700 kPa with pressure of well head (Pwh) approx. 1,000 kPa
- Lifting from heel and toe with gas assist at start of vertical section
- Current production rates range from 100 m3/d to 700 m3/d of emulsion targeting 3,500 kPa

Electric Submersible Pump (ESP)

- ESP for thermal SAGD applications can be sized to meet the specific deliverability of the well.
- Operating temperatures typically below 215°C
- Typically Series 500 installed, and Series 400 pumps installed due to casing restrictions

Progressive Cavity Pumps (PCP)

- Generally PCPs have been used for low deliverability wells and where potential solids may be produced.*
- Installation of metal to metal pumps
- * ConocoPhillips Canada initial strategy for PCPs was to use them on low deliverability wells where the current ESP designs were deemed less appropriate. However, installation of larger PCP are being considered for wells that may produce relatively "cold" viscous fluid for some time.



ESP Run Life Definitions

- **MTTF:** This run-life measure is calculated as the total exposure time of all systems (running, pulled and failed) divided by the number of failed systems.
- Average Runtime: This run-life measure is calculated as the total exposure time of all systems (running, pulled and failed) divided by the number of systems (running, pulled and failed) failed)
- Average run life running ESP: This run-life measure is calculated as the total exposure time of running systems divided by the number of running systems.
- **Window:** window time allows for changes in average run-life to be more apparent, as they are less obscured by previous data.



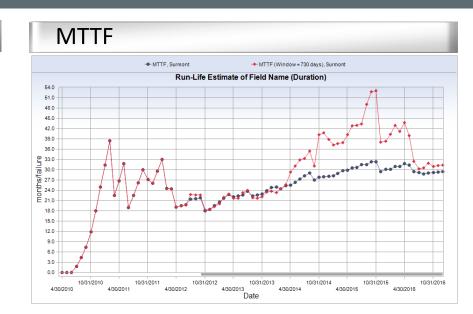
ESP Performance

KPIs

Population:	52 ESP's
Cumulative MTTF:	29.1 months
Windowed* MTTF:	31.4 months
Average Runtime:	15.4 months
Windowed Runtime:	18.8 months
Average run life running ESP:	10.6 months

- **2016:** 16 ESP failures
- **2017:** 5 ESP failures

*(730 day window)



Average Runtime





Artificial Lift Strategy & Performance

- The artificial lift mode selection is reliant on the pressure strategy for any given well, or drainage area (DA).
 - Phase 2 wells currently utilize Gas Lift (GL) and then will be converted to ESP when the flowing bottom hole pressure is below the effective GL operating point.
 - Four wells in Pad 103 will be ESP day 1. Which means following the circulation time the well will be converted directly to ESP. 266-2 is an ESP Day 1 pad as well.

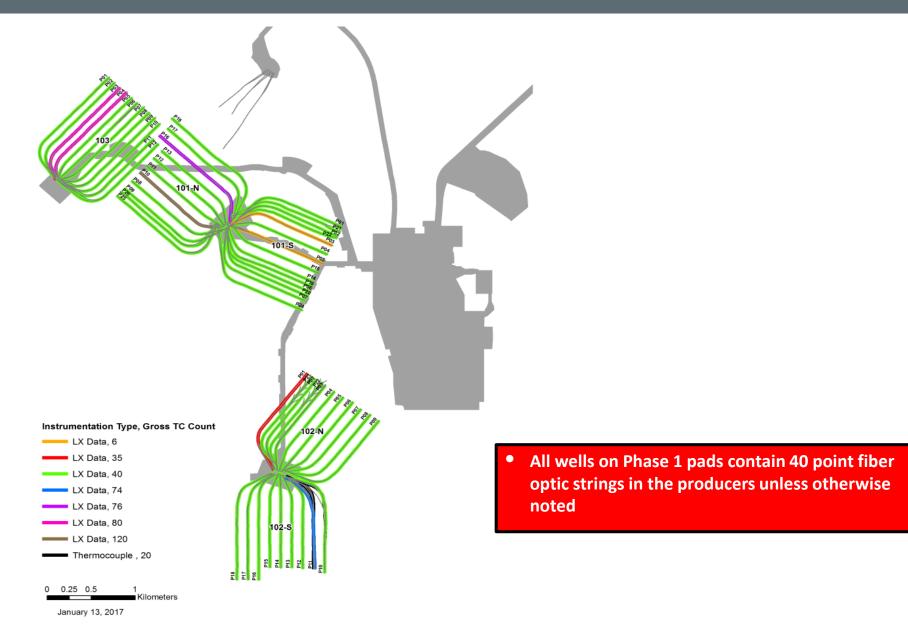




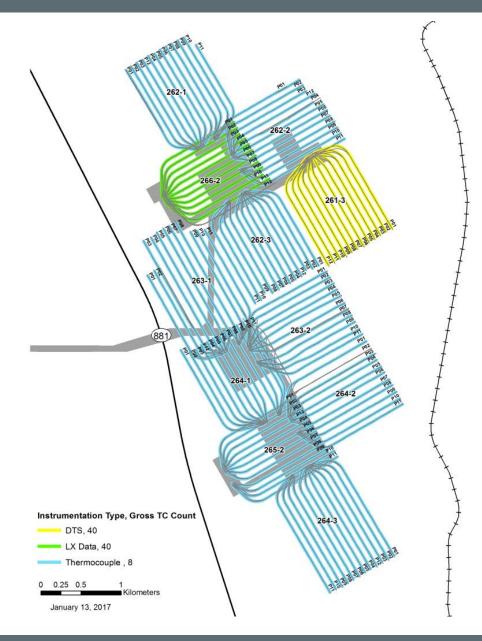
Instrumentation in Wells

Subsection 3.1.1 (5)

SAGD Well Instrumentation



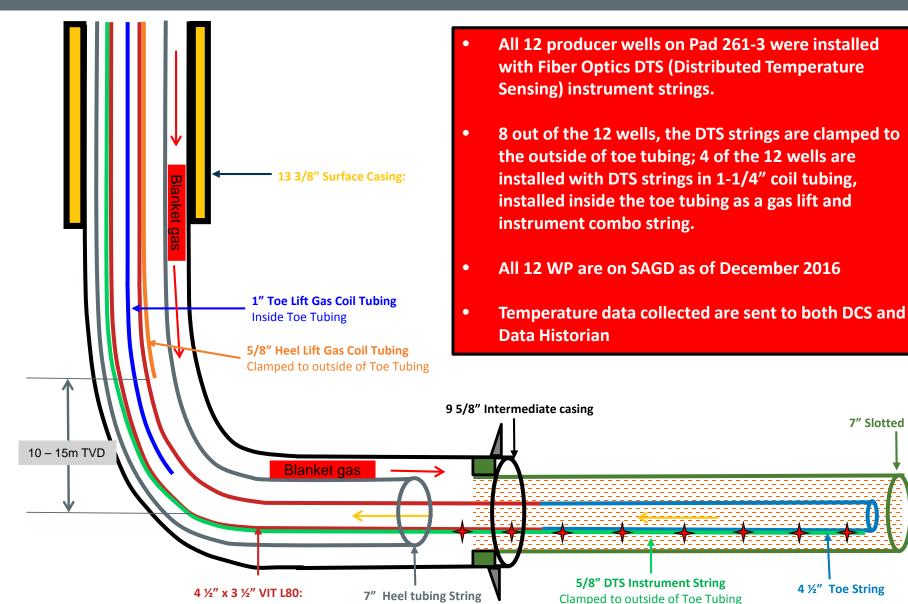
Phase 2 SAGD Well Instrumentation



- 9 of the 11 pads currently online contain 8 thermocouples in the producers.
- The other remaining pads contain 40 instrumentation points as per the image.
- Pads not online as of Feb 2017:
 Pad 267



Distributed Temperature Sensing (DTS) - Pad 261-3



ConocoPhillips

4 ½" Toe String

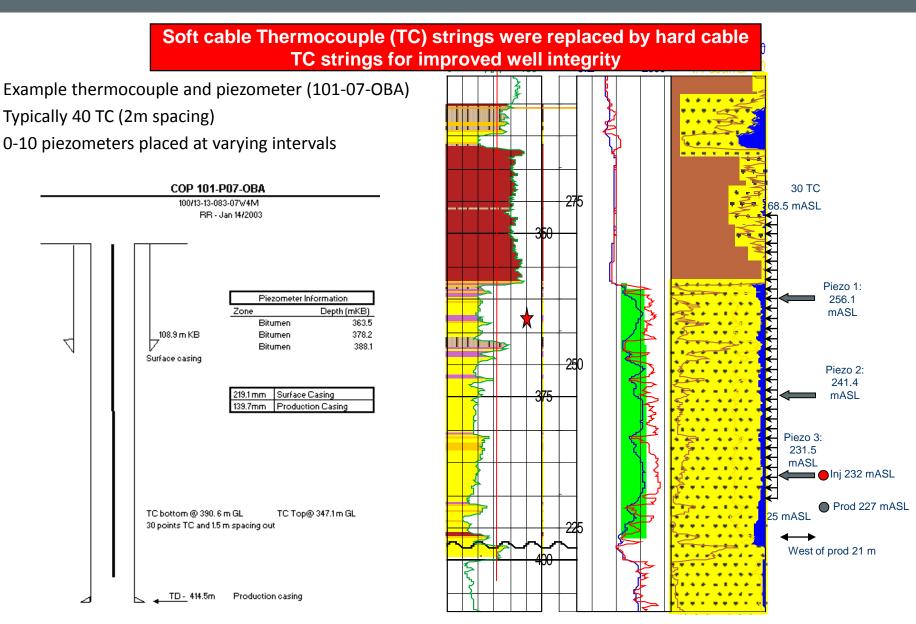
7" Slotted liner

Distributed Acoustic Sensing (DAS) – Pad 103

- DAS was piloted at Surmont to understand if it can be used to reduce the frequency of 4D seismic monitors
 - Similar to a VSP it uses a receiver within the well along with a source at surface
 - Additionally it can passively record within the well to complement seismic
- The DAS trial aimed to utilize the DAS technology on producer wells completed with FCD's
- Initial flow rate from DAS data analysis shows DAS data has potential for production profiling at Surmont
- The same capillary tube as LxData or DTS can be used to perform the DAS survey

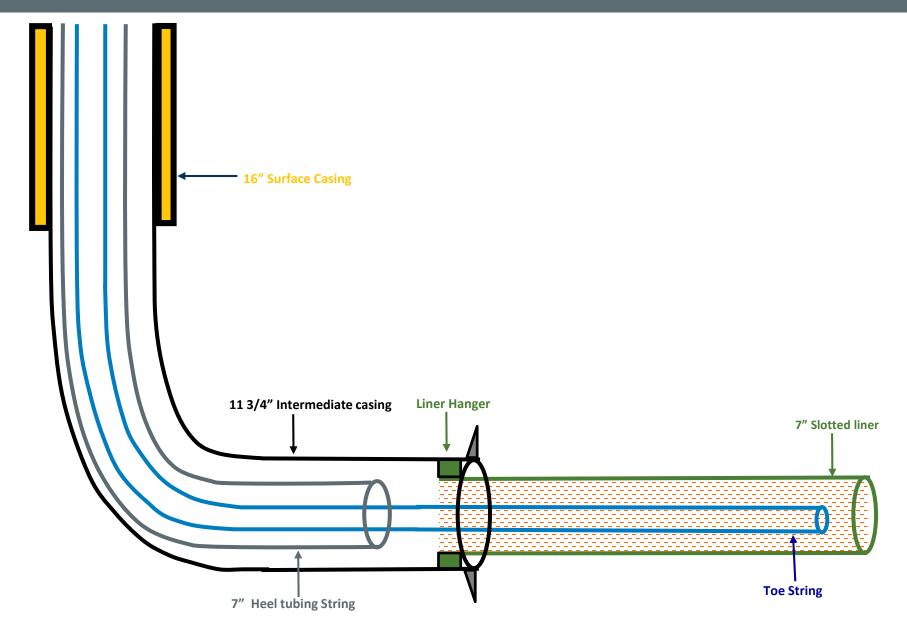


Typical Observation Well Measurement

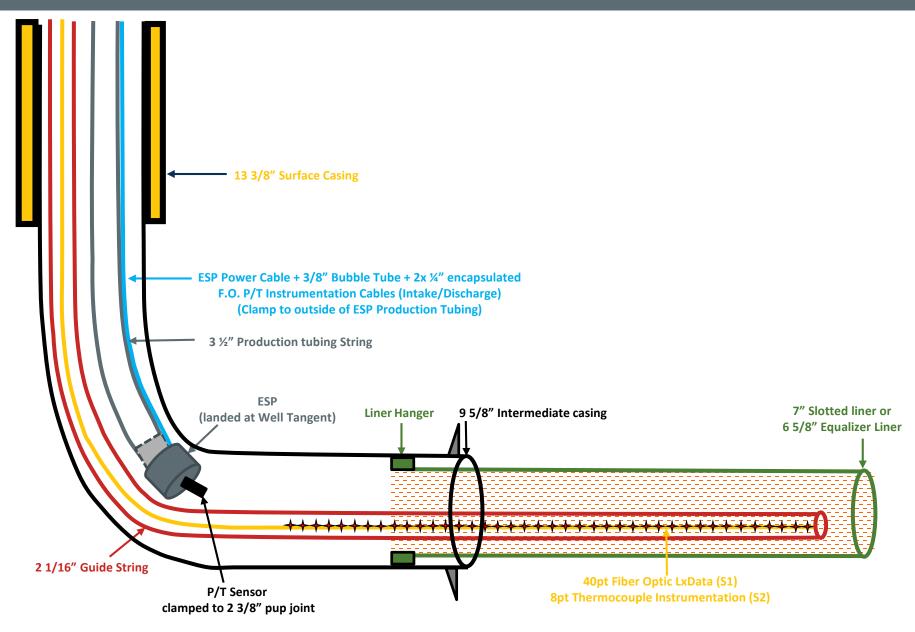


Subsection 3.1.1 (5a, 5b)

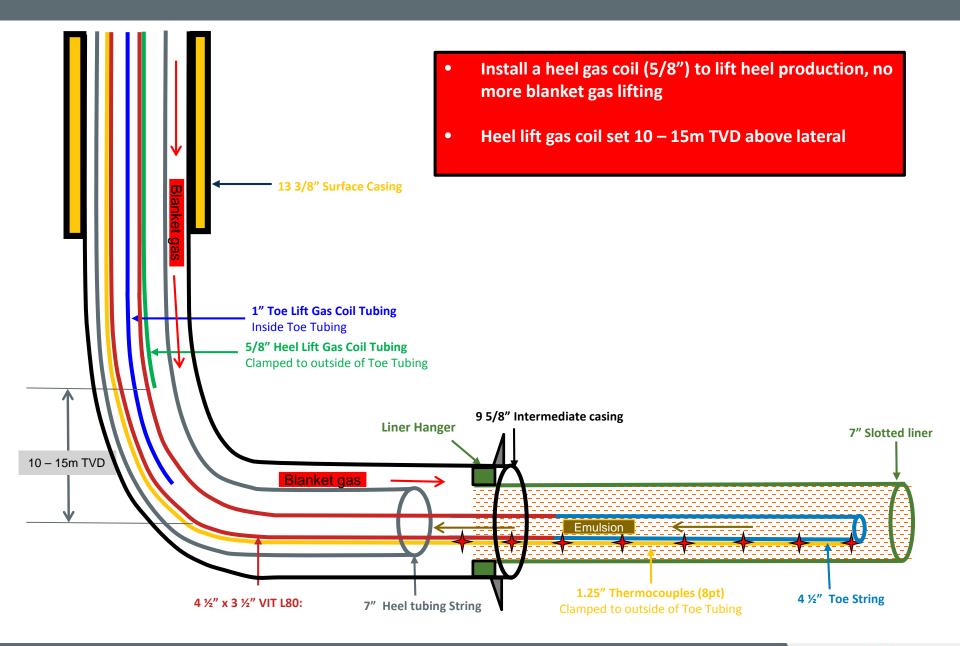
Typical Injector Well Configuration



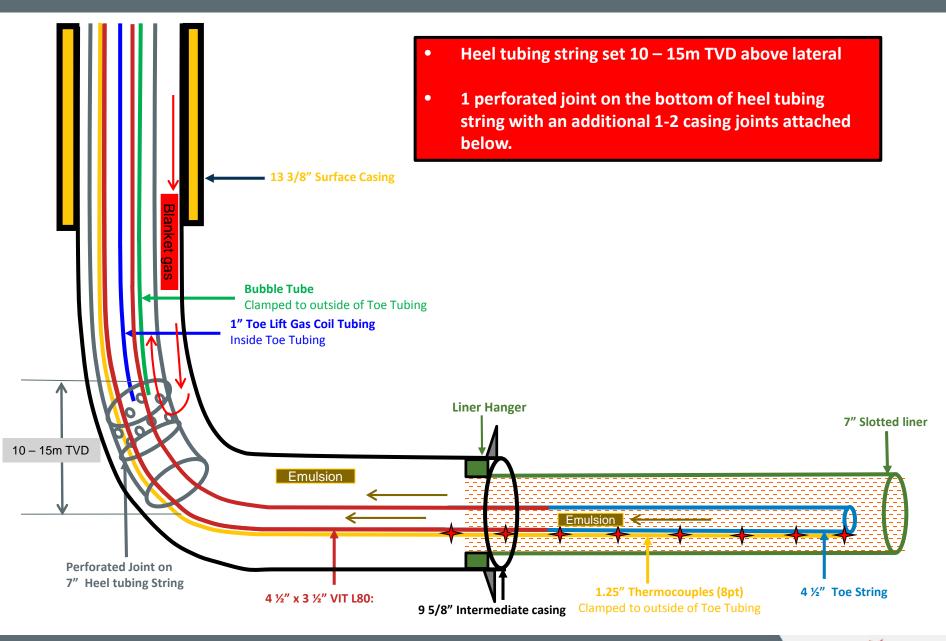
Typical ESP Well Configuration



Improved Gas Lift Producer A: All Pads Excluding 263-1, 263-2 & 264-2



Improved Gas Lift Producer B: 263-1, 263-2 & 264-2

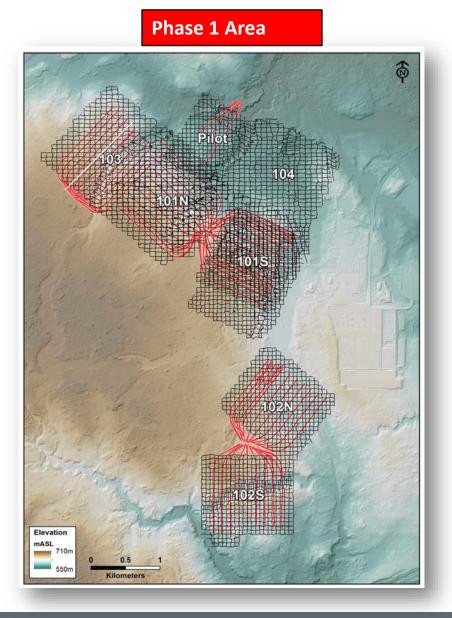




4D Seismic

Subsection 3.1.1 (6)

4D Seismic Location Map – Phase 1



Pilot

- Buried analog single component geophones
- Cased dynamite shots (1/4 Kg) @ 9 m
- 14th monitor acquired in September 2015

Pad 101N

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- 8th monitor acquired in March 2015

Pad 101S

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- 9th monitor acquired in March 2015

Pad 102N

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- 9th monitor acquired in April 2015

Pad 102S

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- 6th monitor acquired in October 2016

Pads 103 and 104

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- 2nd monitor acquired in October 2016



4D Seismic Location – Phase 2



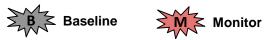
Phase 2

- Buried analog single component geophones
- Cased dynamite shots (1/8 Kg) @ 6 m
- Acquired in three stages:
 - Initial 11 DA's: 2010-11
 - South extension: 2013-14
 - North extension: 2014-2015
- First Monitor acquired in Spring 2016: 263-2



Phase 1 4D Seismic Program

PAD	2013		20	14	20	15	2016		
	Spring	Fall	Spring	Fall	Spring	Fall	Spring	Fall	
101N	MAX A	XMX X	MAX A	M	XMX				
101S	S.M.S		M		MM S				
102N	M.		M.Z		M				
102S			M					M	
Pilot		M.S		MAX A		S.W.S			
103							M	M	
104									







Phase 2 4D Seismic Program

PAD	2016					
	Spring	Fall				
263-1		M				
264-1		2M3				
265-2		2 MZ				
264-3		2M3				
262-1						
266-2						
262-3						
263-2	2 M Z					
264-2						
262-2						
261-3						

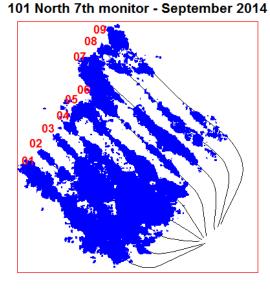




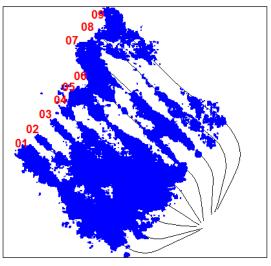


2015 4D Seismic Results Pad 101

- Well Pair 07/08/09, without a true baseline.
- 4D anomaly volume have increased for the remaining well pairs.
- Good conformance, especially at the heel.



101 North 8th monitor - March 2015

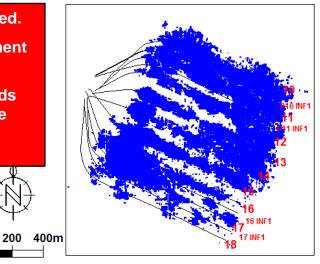


- 4D anomaly volumes have increased.
- Continued conformance improvement along Well Pad 10, 11, 16, 17.
- Infill wells drilled between Well Pads 10, 11, 12, 16, 17 and 18 to optimize production in a geological more complex zone.

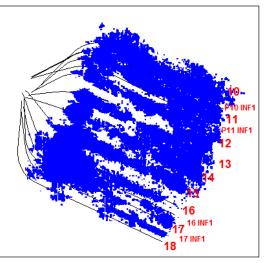
= 4D anomaly

~60 deg C Isotherm

101 South 8th monitor - March 2014



101 South 9th monitor - March 2015

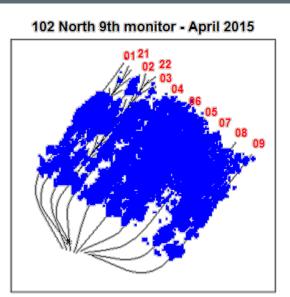




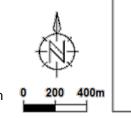
Subsection 3.1.1 (6b)

2016 4D Seismic Results Pad 102 (102S)

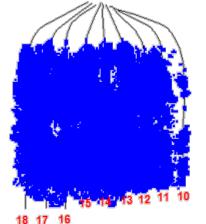
- 4D anomaly volumes have increased. Improved conformance along well pairs 1 to 9.
- 102 North 8th monitor April 2014



 4D anomaly volume have increased. Improved conformance along well pairs 10 to 18.

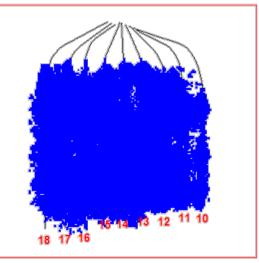


= 4D anomaly ~60 deg C Isotherm



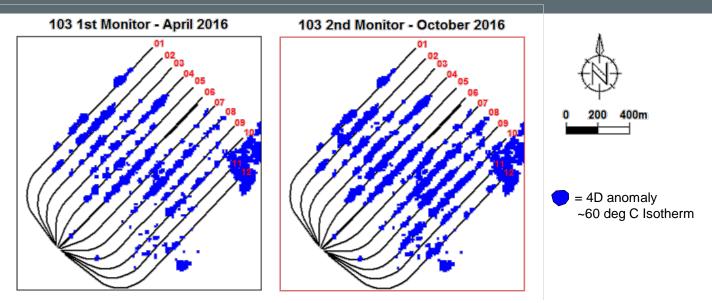
102 South 5th monitor -April 2014

102 South 6th monitor - October 2016





2016 4D Seismic Results Pad 103



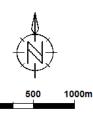
- Relative good conformance in most of well pair.
- 4D indications of coalescence with thermal chamber of Pad 101N (103-11 and 103-12)



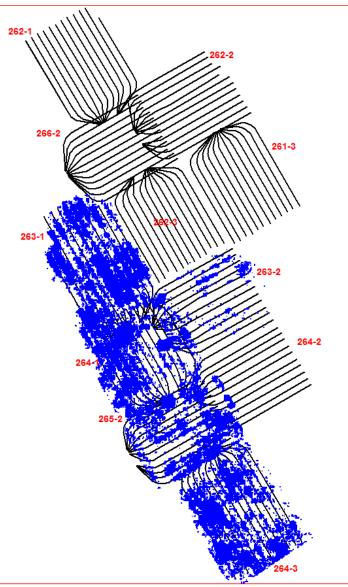
2016 4D Seismic Results Phase 2

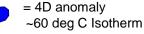
• Spring Monitor:

- 263-2
- Fall Monitors:
 - 263-1
 - 264-1
 - 265-2
 - 264-3
- Relative good conformance in most well pairs (except 263-2 – First Monitor few months after SAGD conversion)
- 4D indications of coalescence between 263-1 and 264-1



S2 1st Monitor - 2016 (Spring - Fall)







Seismic Examples: 101-P16 Conformance (Toe)

Problem:

Well pair 101-P16 • lacking good conformance along well pair.

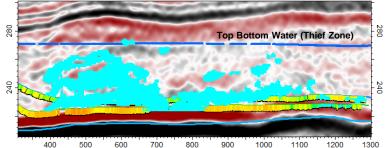
Action:

Increase pressure Ö of steam injection at toe.

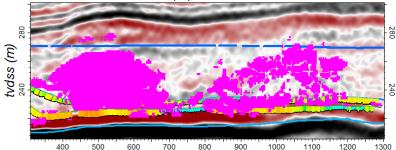
Results:

Conformance ۲ improved at toe.

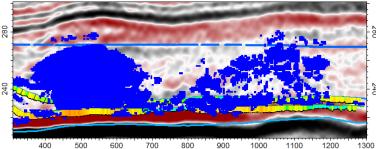
Well Pair 101-16 (14) - Monitor 5th - April 2011

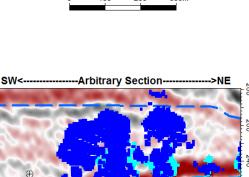






Well Pair 101-16 (14) - 9th Monitor - March 2015





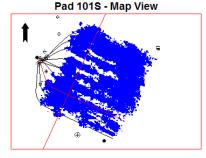
5862200

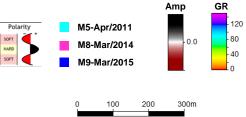
280

240

5861800

5862000

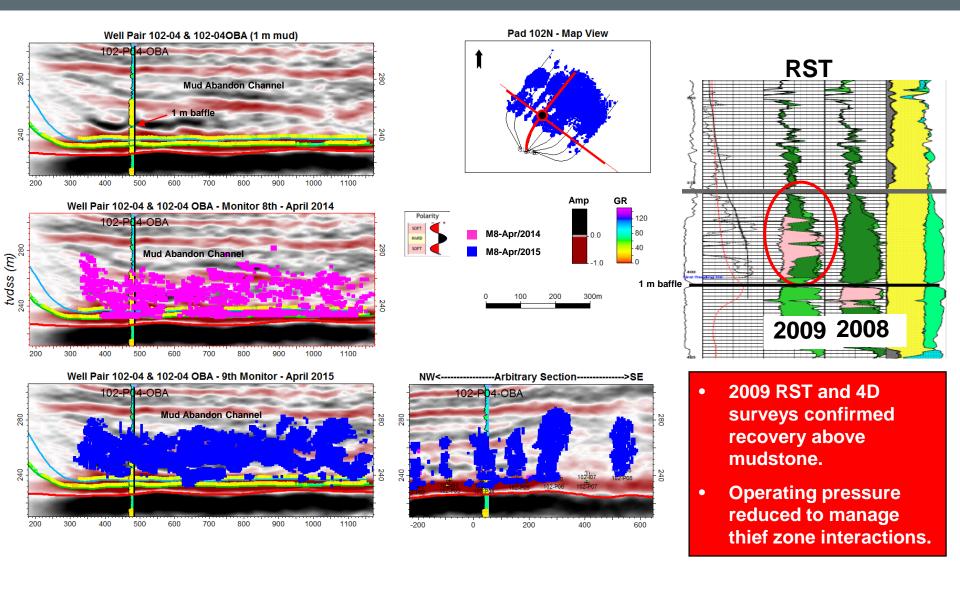






5862400

Seismic Examples: 102-04 OBA Baffle Breakthrough (Heel)



4D Seismic Program 2016

- 4D seismic has proven very useful in monitoring and optimizing conformance and pressure strategy.
- 4D correlates with observation well data.
- Continuing to optimize heel/toe production/injection splits using 4D results.
- Ongoing efforts to history match reservoir models using 4D seismic.

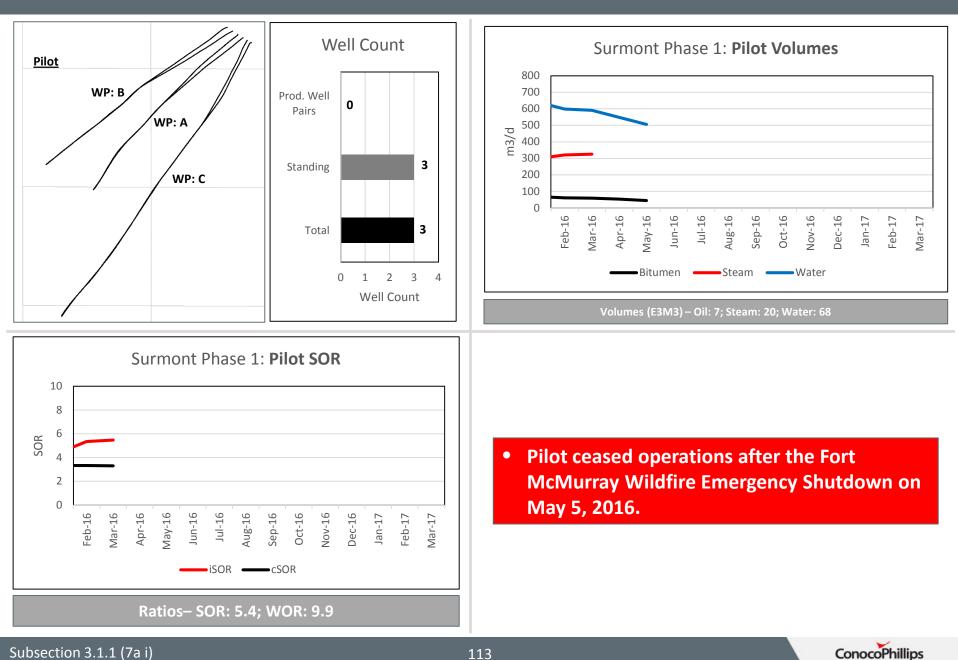




Scheme Performance

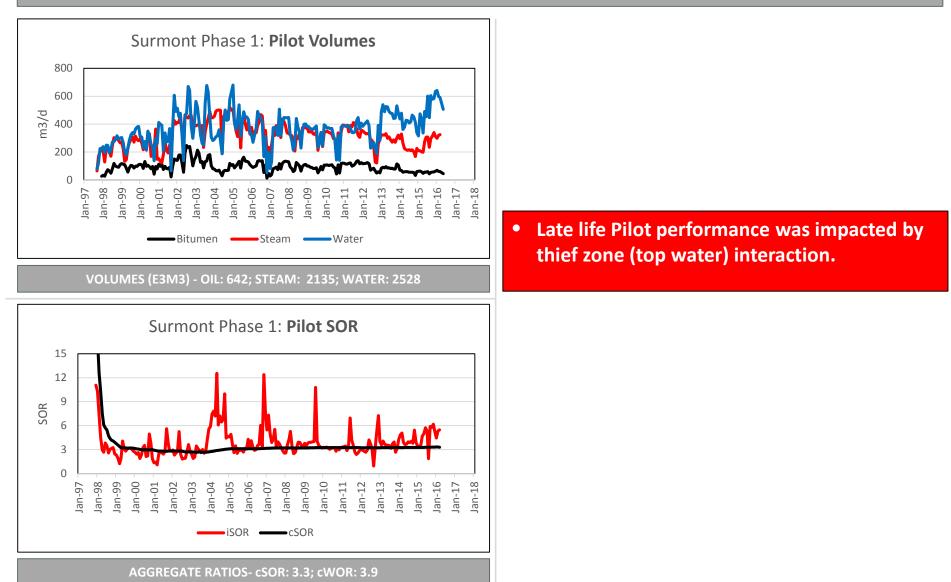
Subsection 3.1.1 (7)

Surmont: Pilot Performance Plot



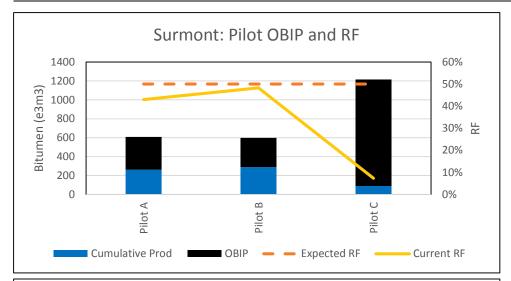
Surmont: Historical Pilot Performance Plot

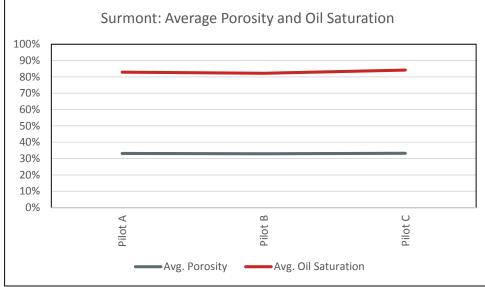
SURMONT PILOT- WELL PAIRS A, B, C



Subsection 3.1.1 (7a ii)

Surmont: Pilot – OBIP and RF





- OBIP: 597 1215 E3M3
- Current RF: 7% 48%

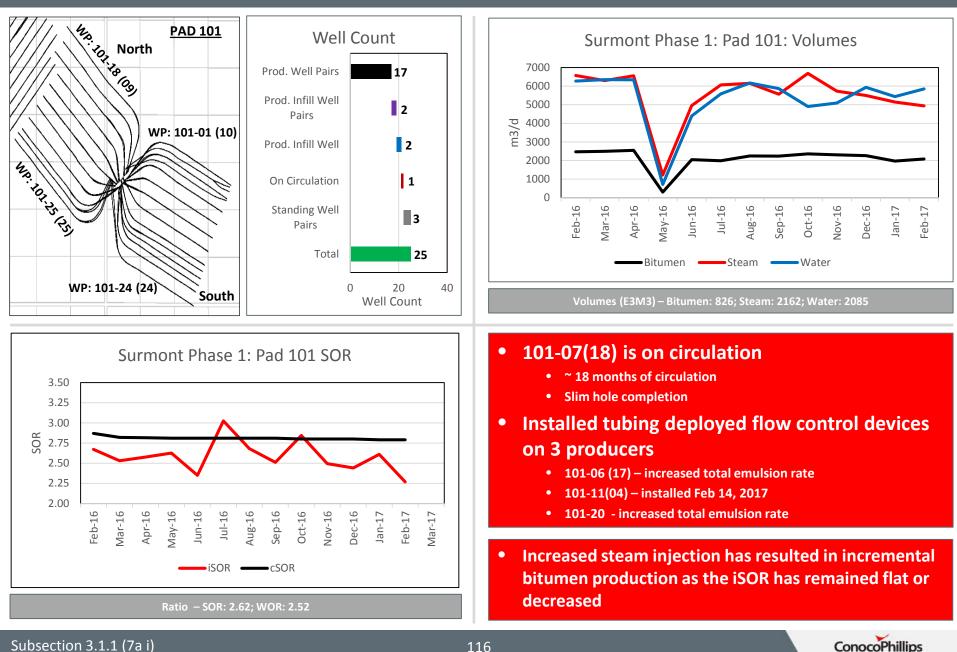
- Porosity: 33%
- Oil saturation: 82% 84%



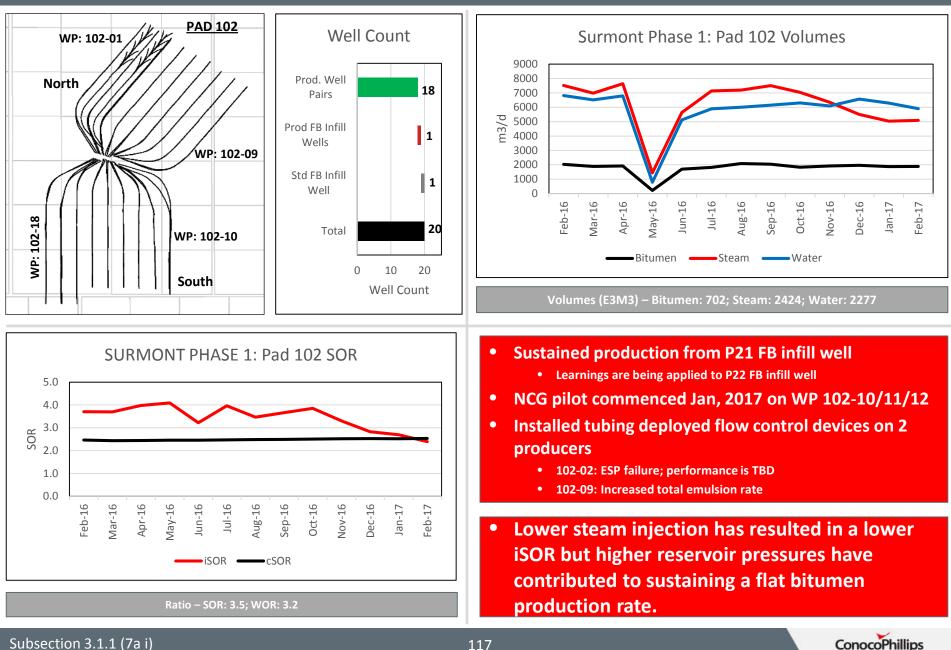
Subsection 3.1.1 (7c i & ii)

 $OBIP = (BV)(\Phi)(So)$

Surmont: Pad 101 Performance Plots

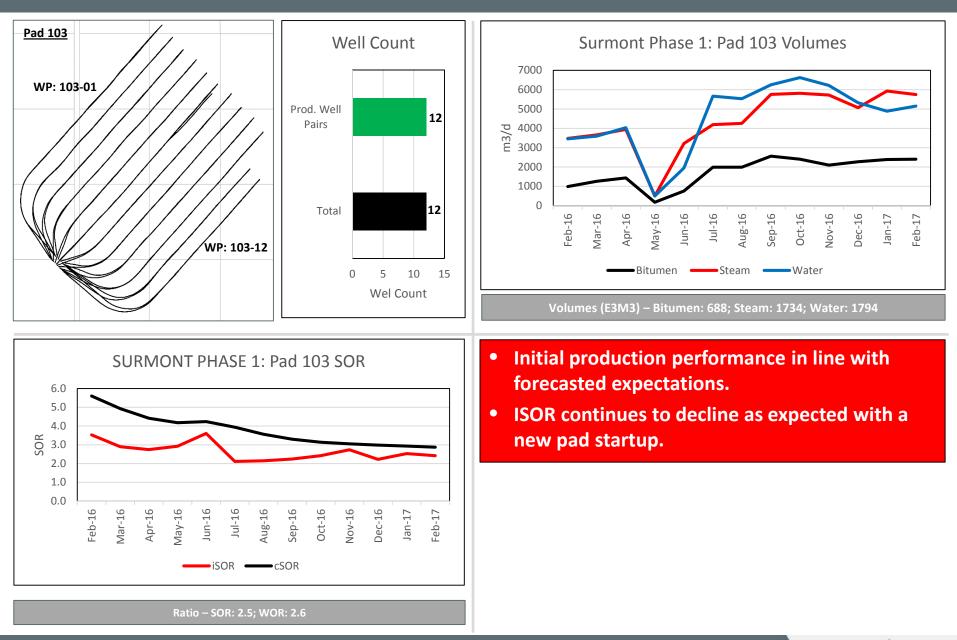


Surmont: Pad 102 Performance Plots

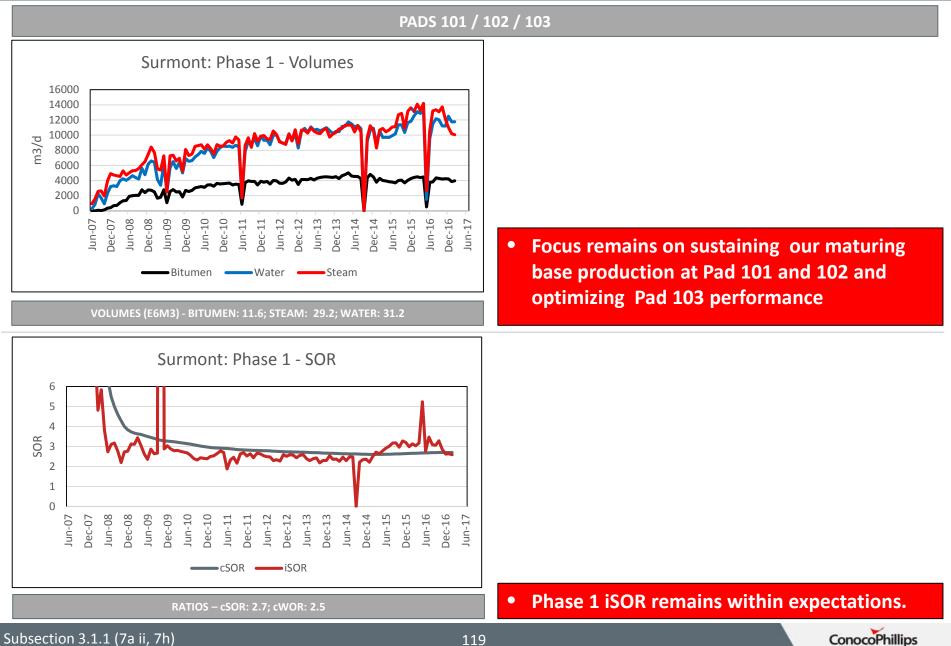


Subsection 3.1.1 (7a i)

Surmont: Pad 103 Performance Plots

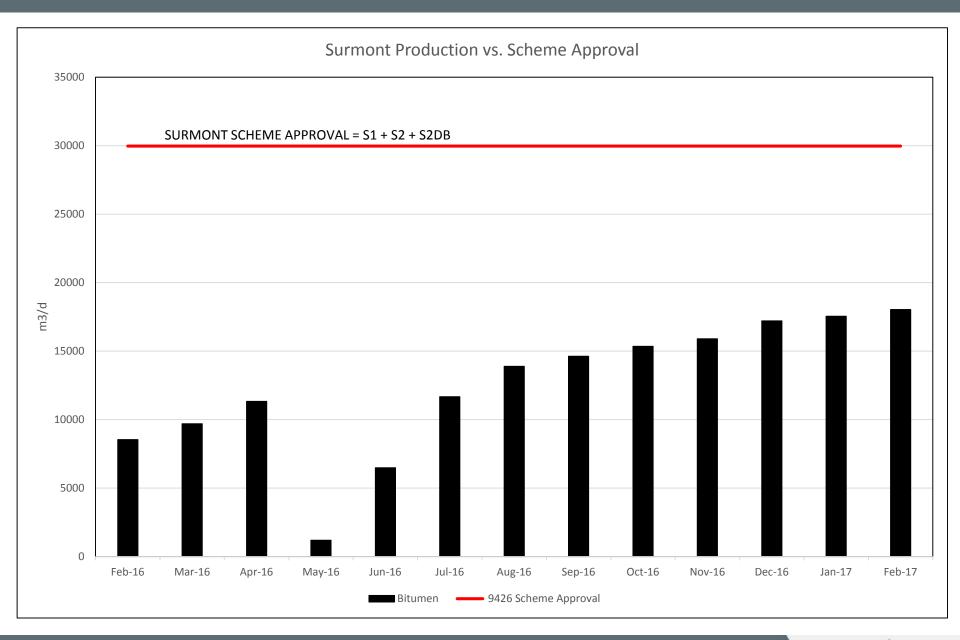


Surmont: Phase 1 Historical Performance Plots

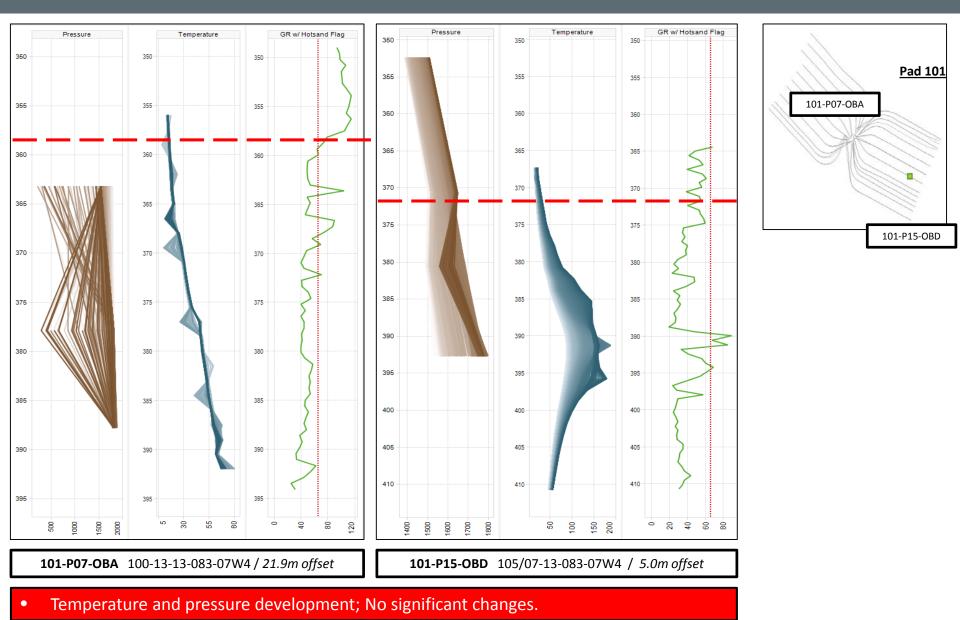


Subsection 3.1.1 (7a ii, 7h)

Surmont: Production vs. Scheme Approval

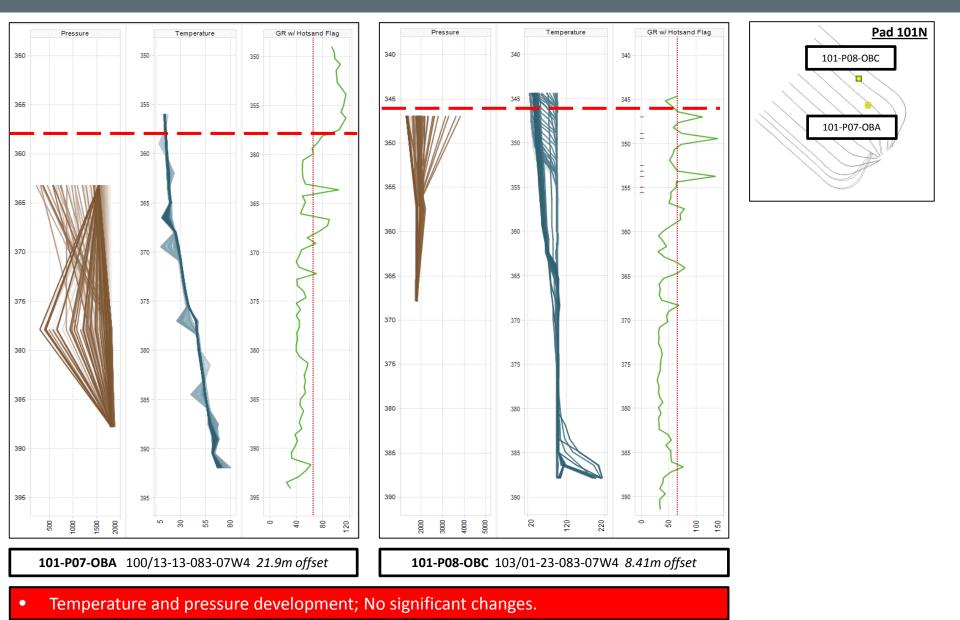


Obs Wells Temp & GR – 101-P07-OBA, 101-P15-OBD



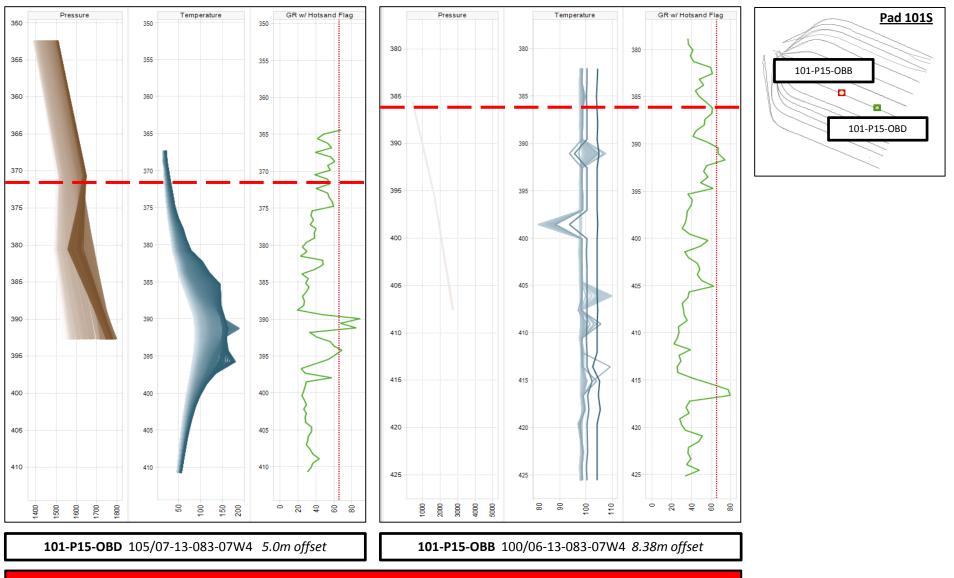
Subsection 3.1.1 (7b)

Surmont: Obs Wells Temp & GR – 101-P07-OBA, 101-P08-OBC



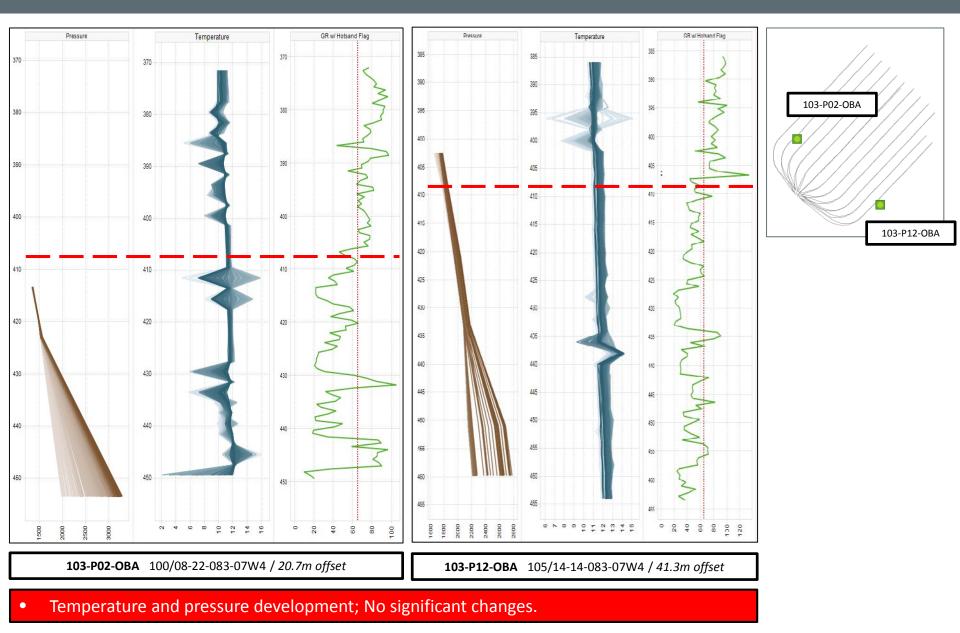
Subsection 3.1.1 (7b)

Surmont: Obs Wells Temp & GR – 101-P15-OBD, 101-P15-OBB

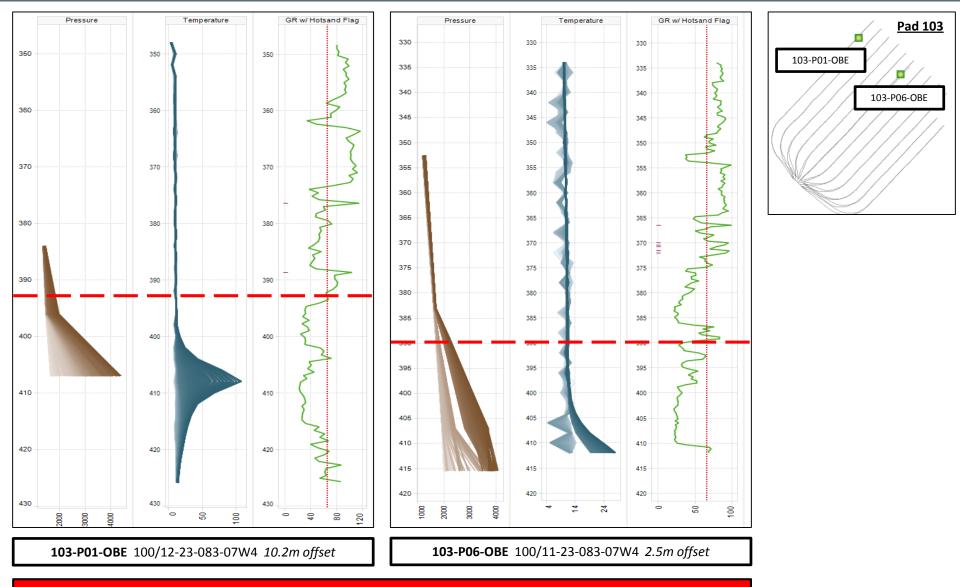


Temperature and pressure development; No significant changes.

Obs Wells Temp & GR – 103-P02-OBA, 103-P12-OBA

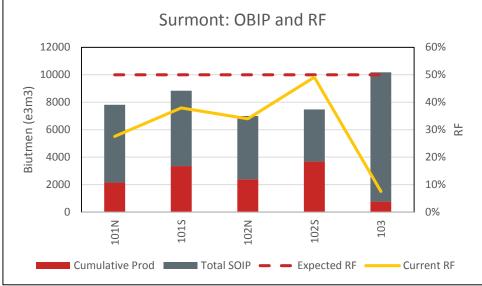


Surmont: Obs Wells Temp & GR – 103-P01-OBE, 103-P06-OBE



• Temperature and pressure development; No significant changes.

Surmont: Phase 1 - OBIP and RF



DA	Cumulative Prod	SOIP	Expected	Current	Avg Phi	Avg So
DA	E3m3	E3m3	RF	RF		
101N	2155	7817	50%	28%	33%	82%
101S	3352	8842	50%	38%	33%	81%
102N	2379	6998	50%	34%	33%	81%
102S	3676	7481	50%	49%	31%	74%
103	768	10176	50%	8%	32%	84%

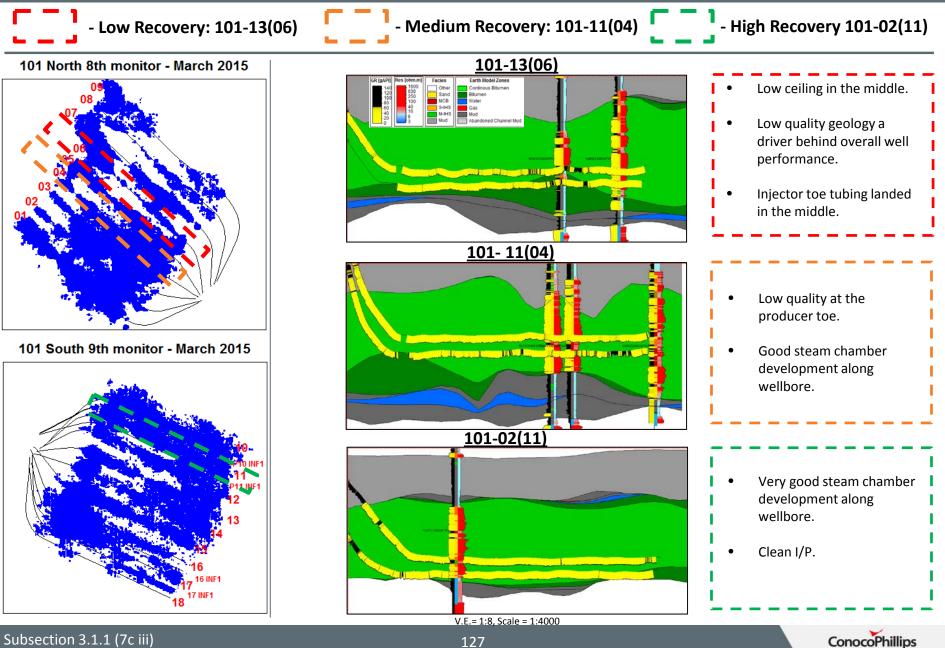
- **OBIP: 6,998 10,176 E3M3** •
- Current RF: 7.5% 49% •
- Porosity: 31% 33% •
- **Oil saturation: 74% 84%** •
- Cumulative volumes and recoveries align • with internal forecasts. Blowdown timing will determine final EUR/RF.



100% 90% 80% 70% 60% 50% 40% 30% 20% 10% 0% Pilot C Pilot A Pilot B 101N 101S 102N 102S 103 ----- Avg. Oil Saturation Avg. Porosity

Surmont: Average Porosity and Oil Saturation by DA

Surmont: Pad 101 Low, Medium, High Recovery Examples



Subsection 3.1.1 (7c iii)

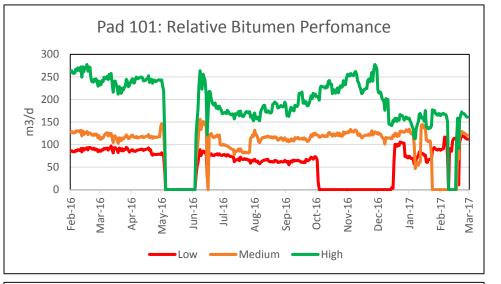
127

Surmont: Pad 101 Low, Medium, High Recovery Examples

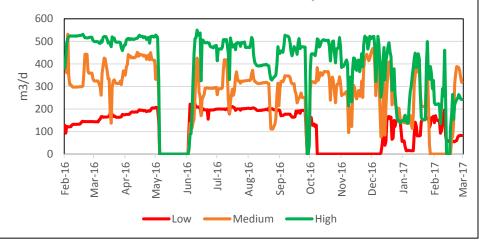
- Low Recovery: 101-13(06)

- Medium Recovery: 101-11(04)

- High Recovery: 101-02(11)



Pad 101: Relative Steam Injection

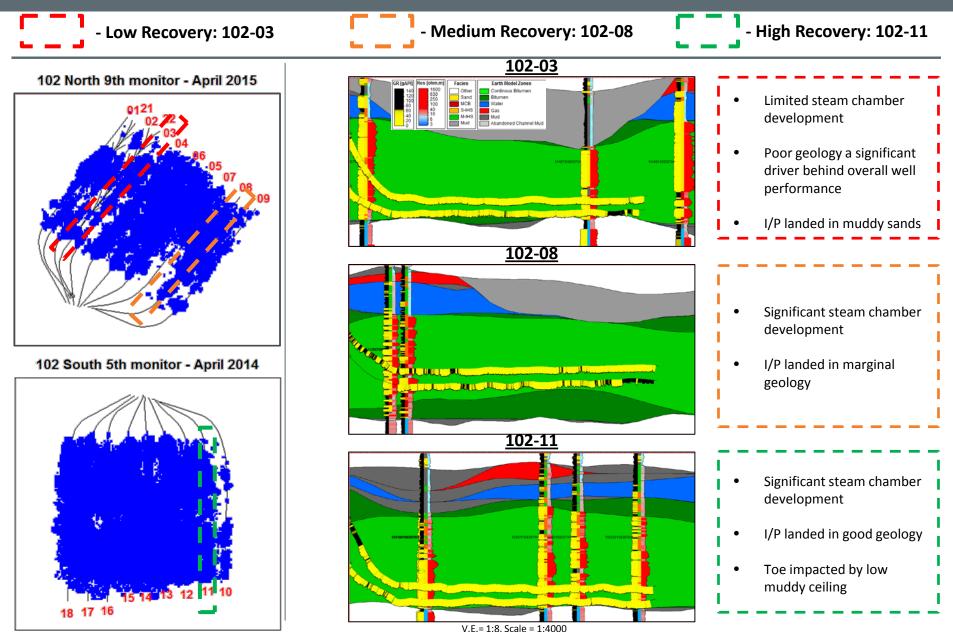


Sustained / increased bitumen production from subject wells.

• Effective steam management improved performance of 101-06.



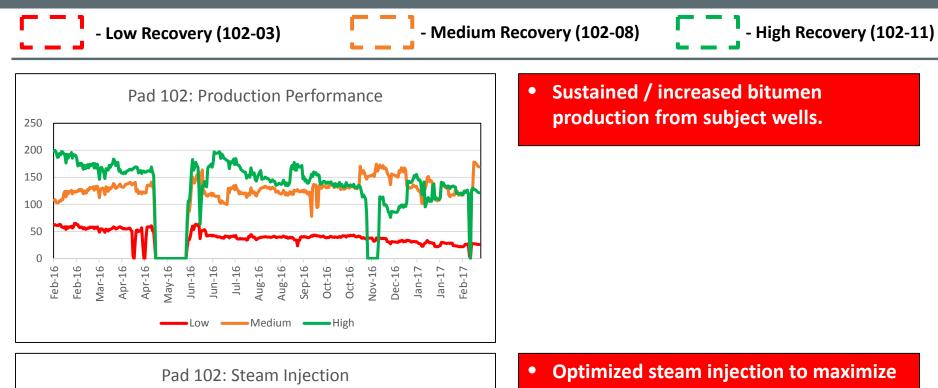
Surmont: Pad 102 Low, Medium, High Recovery Examples

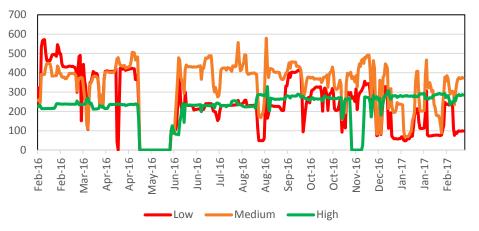


Subsection 3.1.1 (7c iii)

129

Surmont: Pad 102 Low, Medium, High Recovery Examples





bitumen production from 102-11.

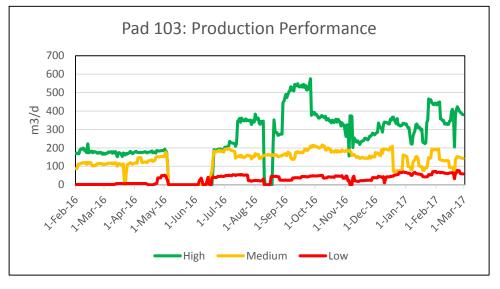


Surmont: Pad 103 Low, Medium, High Recovery Examples

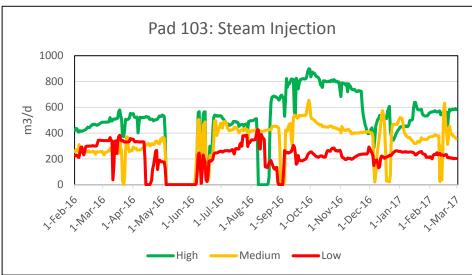
- High Recovery (103-08) - Medium Recovery (103-05) - Low Recovery (103-11) 103-11 Interaction will low Pad 103 2nd Monitor – October, 2016 pressure chamber of 101N Short well (790m) Fish in hole 103-05 SL completion Good geology 103-08 FCD completion Good geology Early ESP conversion ConocoPhillips Subsection 3.1.1 (7c iii) 131

Surmont: Pad 103 Low, Medium, High Recovery Examples





• FCD completion continues to outperform SL



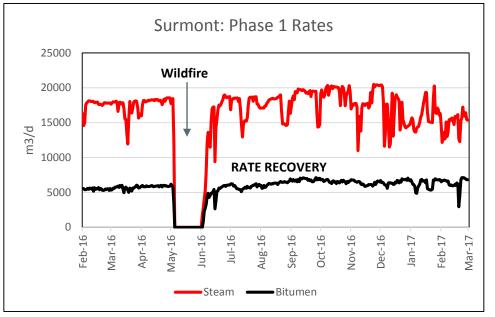
Subsection 3.1.1 (7c iii)

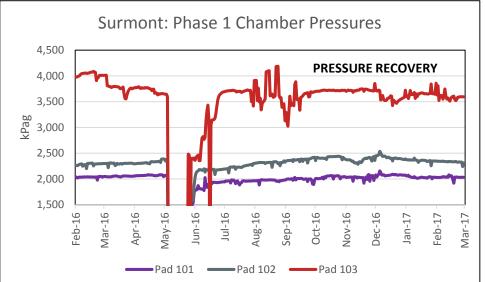


Surmont 1 – Recovery Examples – Normalized Well Life Production Data



Surmont: Post Fort McMurray Wildfire Performance Plots





• Reservoir performance on trend with pre-Fort McMurray Wildfire baseline.

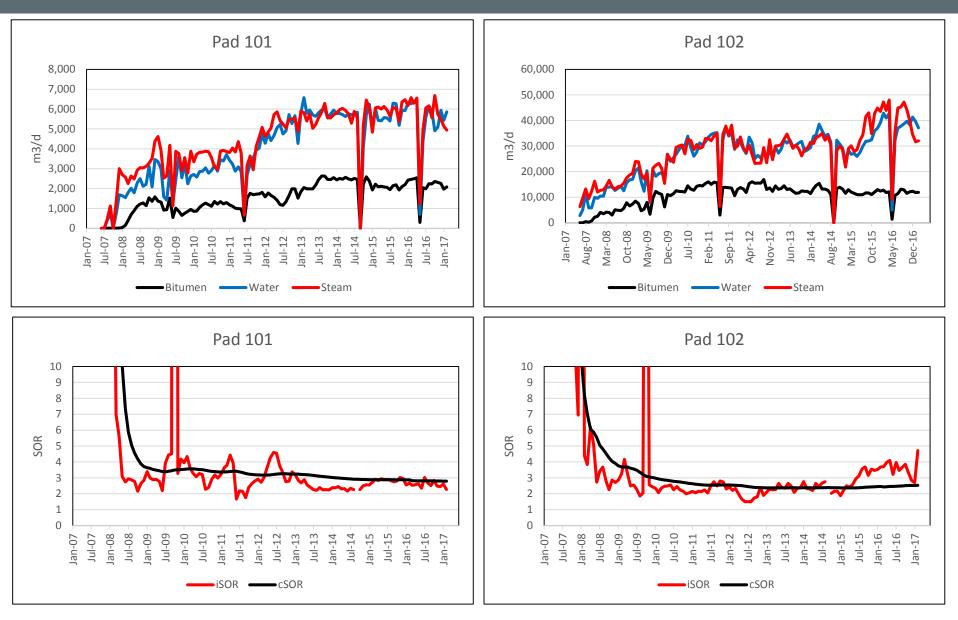


Subsection 3.1.1 (7f)

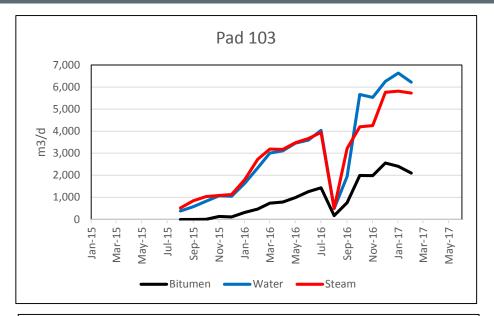
- At pad 101/102, incremental steam injected during 2015/2016 increased the reservoir chamber pressure which attributed to a flat bitumen production profile during the subject timeframe
 - Even during Q4, 2016 when steam injection rates were considerably curtailed, bitumen production rates have held constant.
 - iSOR continues to improve and trend lower
- Liner installed flow control devices at Pad 103 continue to outperform SL wells.
- Initial results from tubing deployed flow control devices at Pad 101/102 continue to be assessed however, early days are illustrating a net increase in total emulsion/bitumen rates.
- Optimization continues to improve performance of mature wells:
 - NCG pilot commenced January, 2017 on 3 wells at Pad 102
 - Fishbone infill well 102-22 expected to be onstream in Q2, 2017
 - Steam injection optimization
 - Subcool management
 - Well stimulations
 - Changes in injector tubing landing depths
 - Additional tubing deployed flow control devices
 - Investigating possible BP drill outs to recover lost sections of laterals

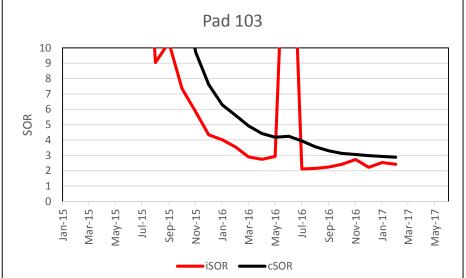


Surmont: Phase 1 Well Pad Rates and SOR



Surmont: Phase 1 Well Pad Rates and SOR

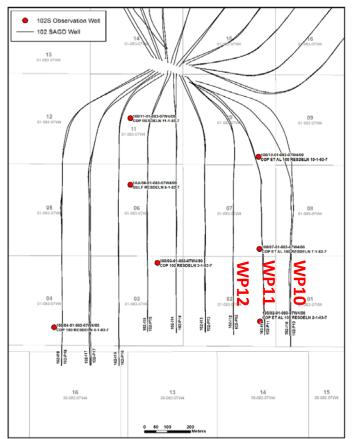






102 NCG Co-Injection Trial

Pad 102S

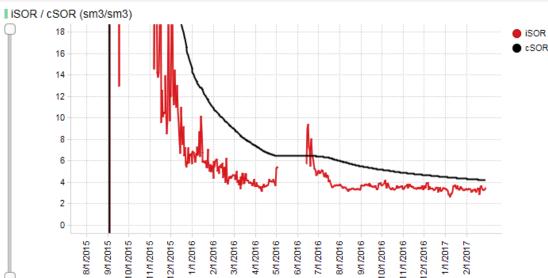


- Pilot focused on co-injection of fuel gas with steam in order to reduce steam requirements ultimately reducing water usage, fuel consumption and lower greenhouse gas emissions.
- Pilot on 102 South is located on the western side of the well pad. Subject pilot wells are:
 - 102-WP10
 - 102-WP11
 - 102-WP12
- Injection concentrations are up to a maximum of 2 mol% methane or 10 E3m³/d per well pair.



Surmont Phase 2 Aggregate Performance Plots





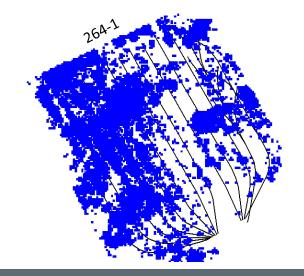
- All eleven pads started as of February 28, 2017.
- Steam/Water trends diverting result of thief zone interactions in Pads 264-1, 263-1, 265-2, 262-2
- Three well pairs re-drilled due to downhole failures

• Surmont 2 ramp-up ongoing.



Performance / Chamber Development Challenges – Pad 264-1

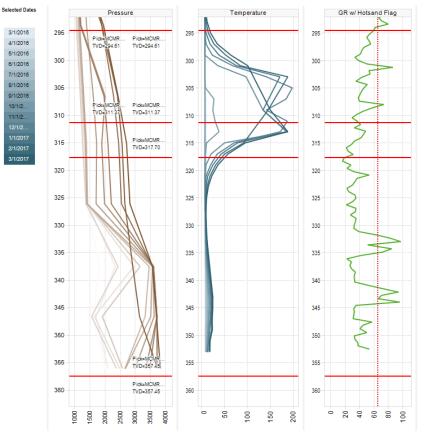




- 264-1 has been operating at a target pressure of
 3,675 kPa
- 11/12 wells converted to SAGD. 1 well circulating
- Good development on West side of DA, however challenging performance on Eastern area
- Top water interaction has been identified in three wells
- Coalescence with Pad to the North on West side

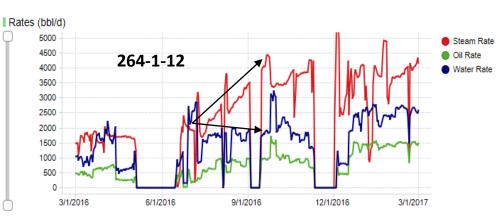


Performance / Chamber Development Challenges – Pad 264-1

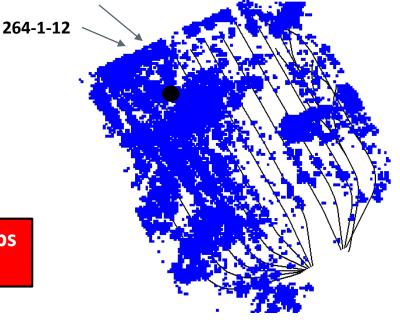


264-1-P04-OBD. 17 meters from well pair

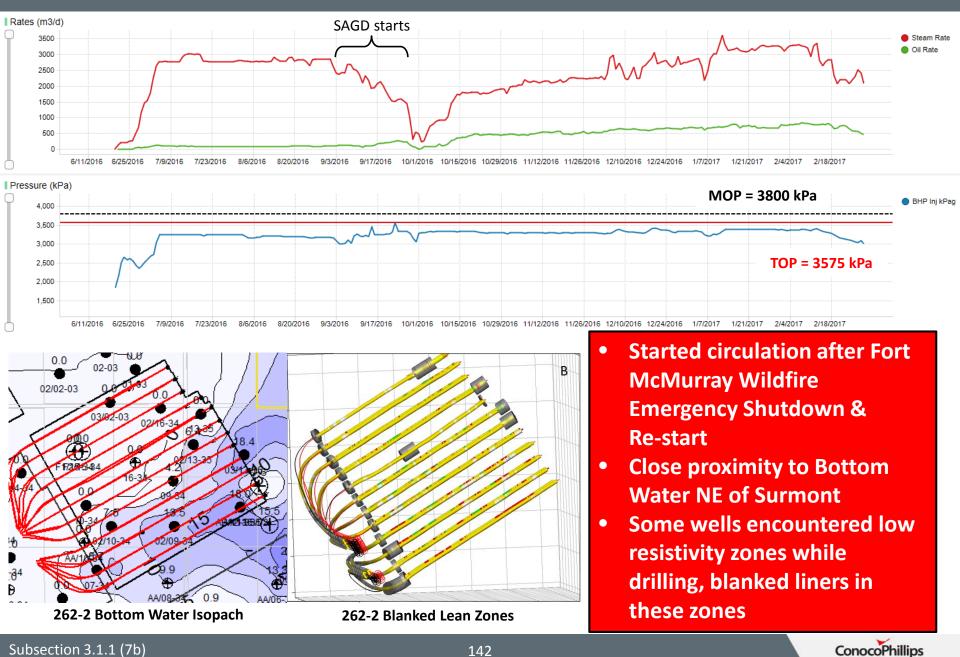
• Top Water interaction observed from Obs Well data and WSR



264-1-04

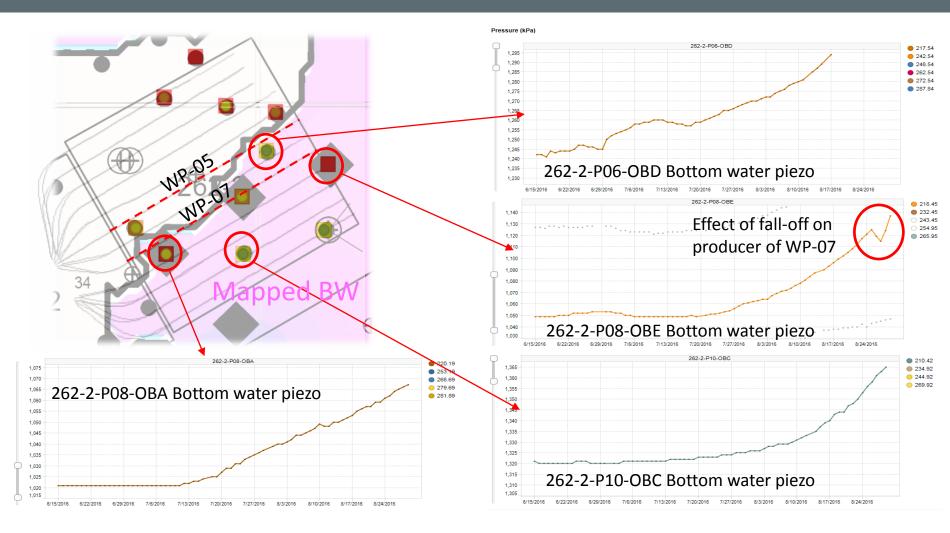


Performance / Chamber Development Challenges – Pad 262-2



Subsection 3.1.1 (7b)

Performance / Chamber Development Challenges – Pad 262-2



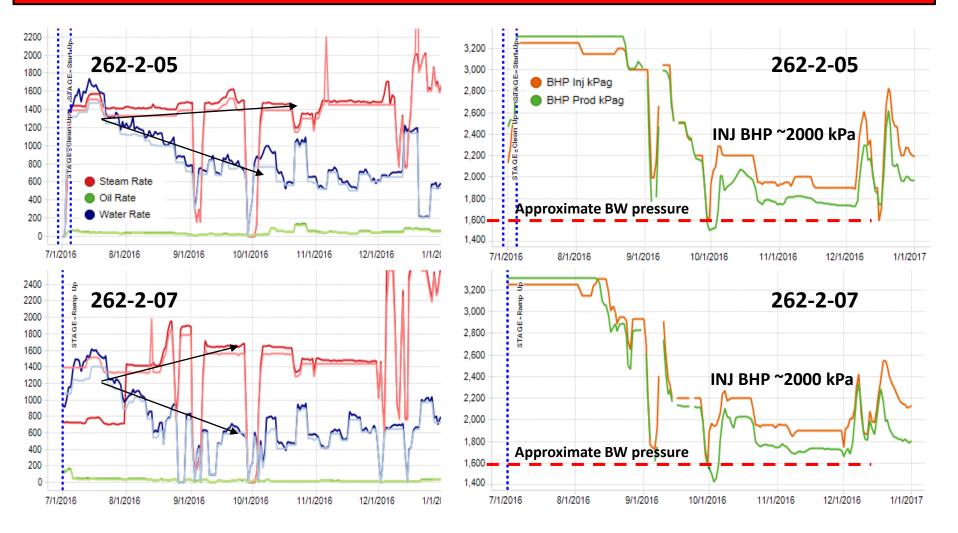
Bottom Water pressurization noticed early after circulation start

Wells 05/07 direct contact with BW reducing circulation effectiveness



Performance / Chamber Development Challenges – Pad 262-2

- Steam leak noticed early after circulation start by reduction of WSR (steam/water trends diverting)
- Pressure reduction mitigation to ~2000 kPa however this is too low for Gas Lift hence needing ESPs

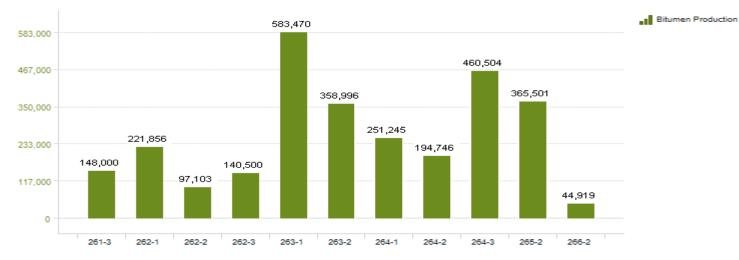


SOIP & Recovery Per Pad

DA	SOIP* (E3M3)	CUM OIL (E3M3)	Recovery Factor
261-3	9,755	148.0	1.5%
262-1	8,755	221.9	2.5%
262-2	8,461	97.1	1.1%
262-3	9,552	140.5	1.5%
263-1	9,146	583.5	6.4%
263-2	8,954	359.0	4.0%
264-1	7,573	251.2	3.3%
264-2	9,845	194.7	2.0%
264-3	10,122	460.5	4.5%
265-2	6,839	365.5	5.3%
266-2	9,383	44.9	0.5%

*SOIP: SAGDable Oil in Place

Cumulative Bitumen Production by Subsurface Pad (m3)



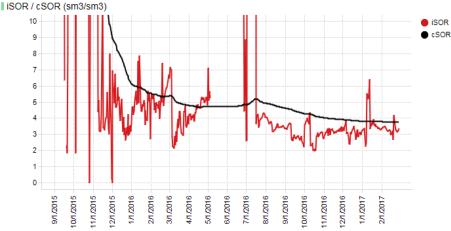
Pads ramping-up. Oil allocated during circulation accounted for RF.

Subsection 3.1.1 (7ci, ii)



Good Performance – WP 263-1-07

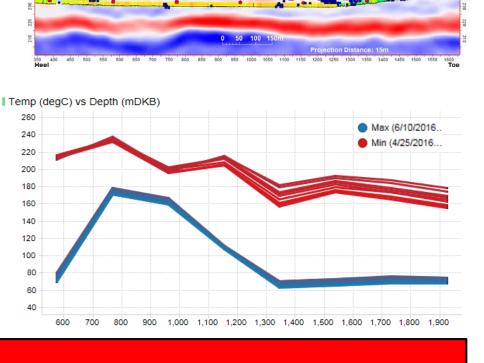






- Very good injectivity translating into fast ramp-up and good production rate.
- Falloff data (confirmed with 4D) shows mainly first half of well contributing to production

Subsection 3.1.1 (7c iii)



263-1-07



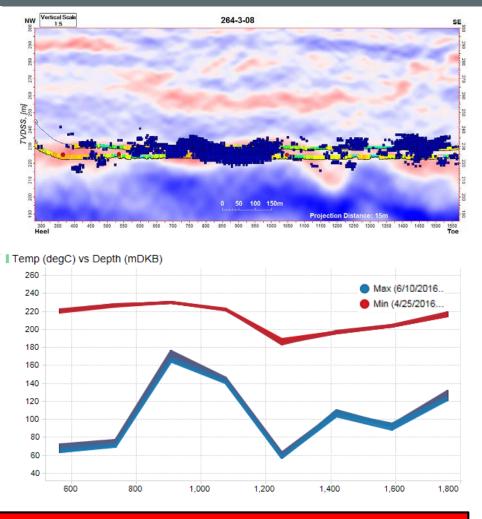
Vertical Scale

SE

IVDSS, [m]

Average Performance – WP 264-3-08





ConocoPhillips

- Well Performance meets expectations.
- Very good injectivity translating into fast ramp-up and good production rate.

1/1/2017 2/1/2017

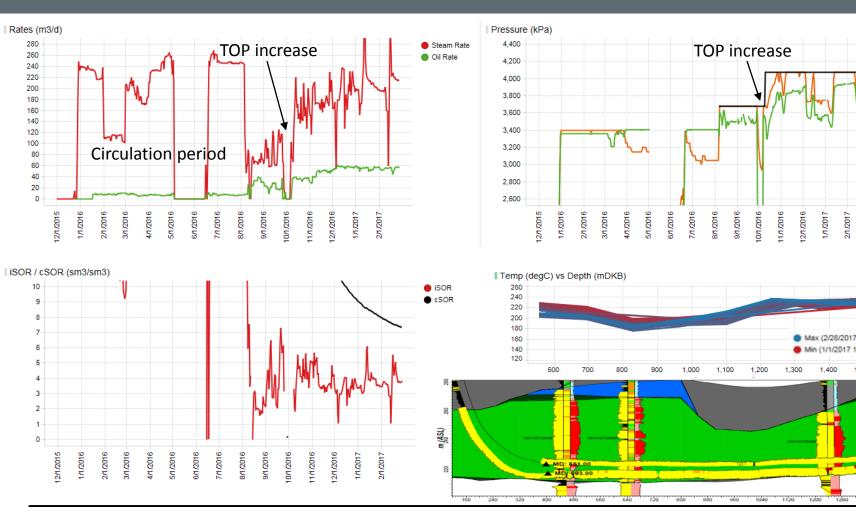
Falloff data (confirmed with 4D) shows two main sections contributing to production

11/1/2015 12/1/2015 11/2016 3/1/2016 5/1/2016 5/1/2016 6/1/2016 7/1/2016 9/1/2016 9/1/2016 11/1/2016

0/1/2015

0

Poor Performance – WP 262-3-08



BHP Inj kPag

Target

1 M /2017 2/1/2017

1,400

1,500

1360 1440 1520

ConocoPhillips

GR [gAP

-120 -120 -100

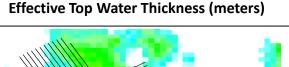
20

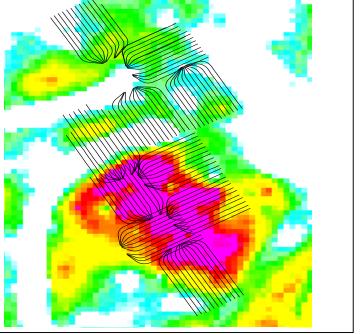
BHP Prod kPag

- Well Performance below expectations despite good geology. Large circulation period (~5 • months) indicated poor communication between injector/producer wells
- Pad MOP increased to 4300kPa in SAGD which helped increase injectivity in the formation
- Flowing temperature data indicates poor development in middle section of the well

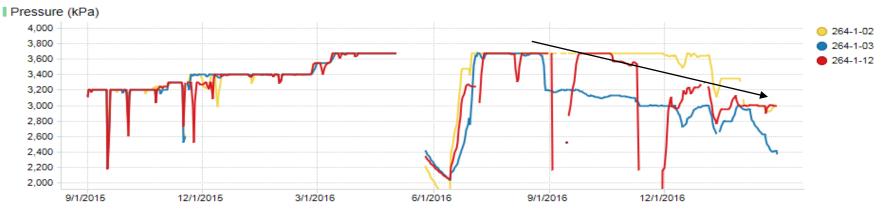
Surmont 2 – Operating Pressure Strategy

- Surmont 2 base case Operating Strategy follows a declining pressure profile, which is influenced by the efficiency of artificial lift, SOR, thief zone (TZ) interaction, etc.
- Certain DAs have been identified at risk for top and bottom water TZ interaction, which has already been observed in some wells.
- Strategy for these DA's account for a more aggressive pressure drop to minimize steam loss into the TZ, but still keeping an overbalanced condition to avoid water influx into the chambers.
- Timing of pressure drop is dependent on each DA's condition. This has already been implemented in some individual wells where interaction has occurred.
- ESP conversions will help implement a lower pressure strategy where required.





ConocoPhillips



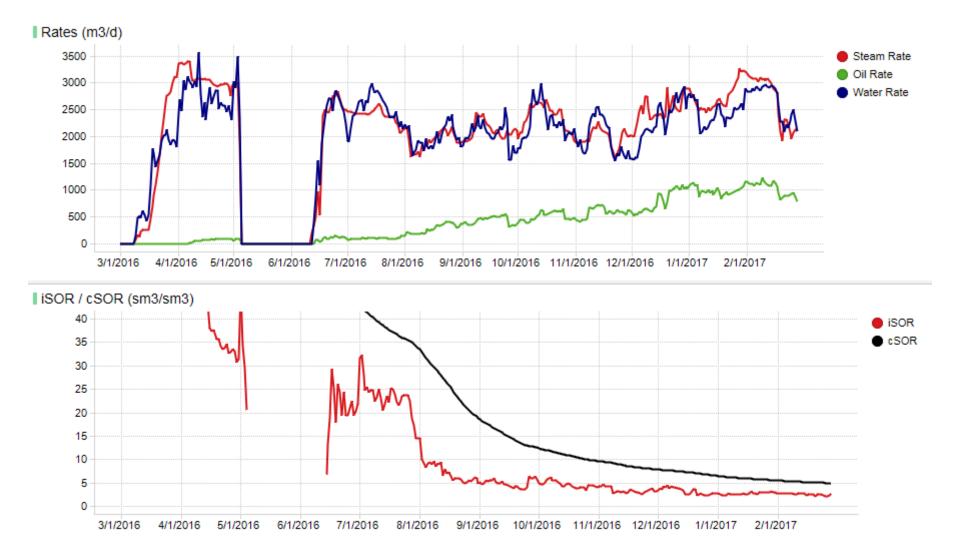
Example of wells in Pad 264-1 where pressure has been decreased to mitigate TZ interaction

Phase 2 - Key Learnings

- Some wells are still challenged with injectivity/productivity issues, which translates into a slower ramp-up or underperformance based on expectations. Evaluation of optimization opportunities is work in progress.
- Liner deployed Flow Control Devices have showed to promote faster development of the wells compared to typical slotted liner wells, mainly due to the operational benefit they provide.
- Proper risk ranking and identification of thief zone areas, combined with close monitoring of chamber development is of great importance for timely execution of operating strategy.
- Optimization projects still under evaluation include:
 - Tubing Deployed FCDs
 - Injector steam splitters
 - Well stimulations



Surmont 2 – 261-3 Pad



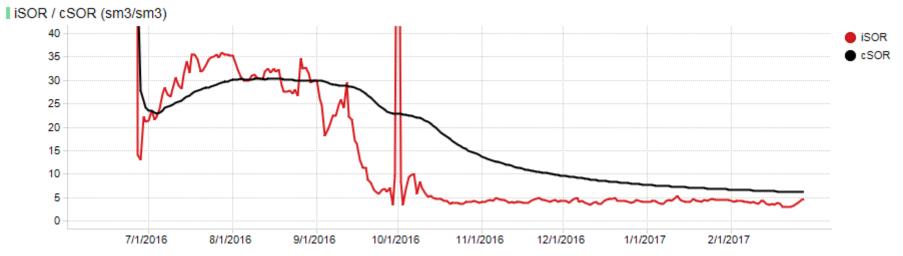
Surmont 2 – 262-1 Pad





Surmont 2 – 262-2 Pad





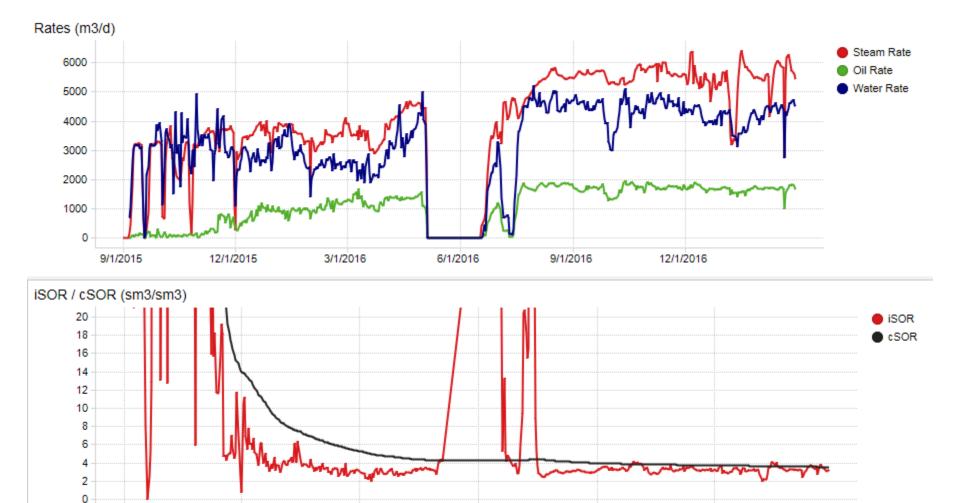
Surmont 2 – 262-3 Pad

Rates (m3/d)





Surmont 2 – 263-1 Pad



ConocoPhillips

9/1/2015

12/1/2015

3/1/2016

6/1/2016

9/1/2016

12/1/2016

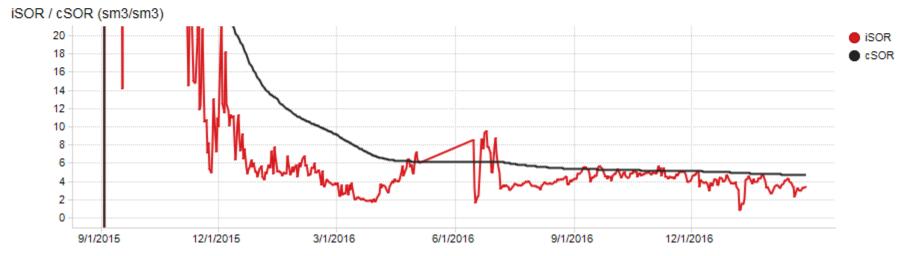
Surmont 2 – 263-2 Pad



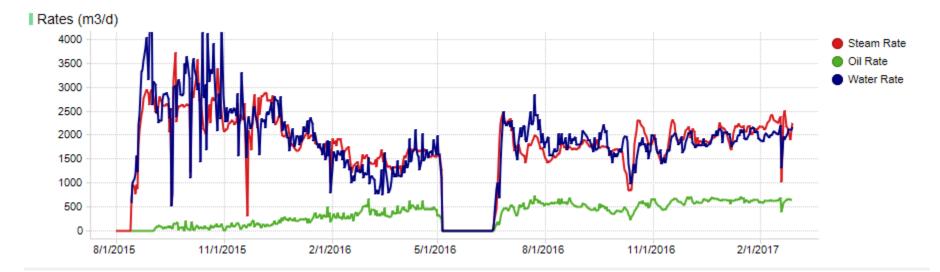


Surmont 2 – 264-1 Pad





Surmont 2 – 264-2 Pad





Surmont 2 – 264-3 Pad

Rates (m3/d) 7000 Steam Rate Oil Rate 6000 Water Rate 5000 Man Bapt Maton 4000 3000 2000 1000 0 10/1/2015 1/1/2016 4/1/2016 7/1/2016 10/1/2016 1/1/2017

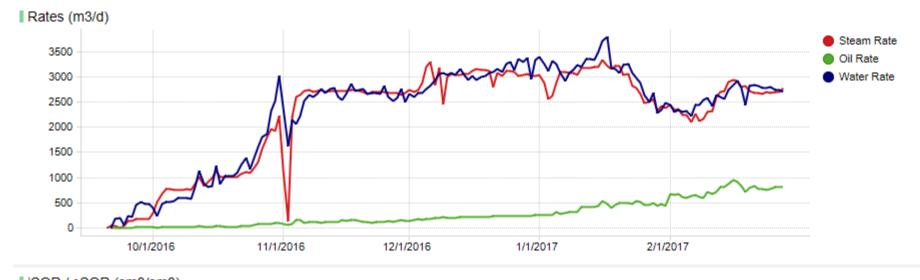


Surmont 2 – 265-2 Pad





Surmont 2 – 266-2 Pad





Subsection 3.1.1 (7h)



Future Plans

Subsection 3.1.1 (8)

Future Plans – Surmont

Surmont 1

- Fishbone infill well 102-22 expected to be onstream in Q2, 2017
- NCG pilot commenced January, 2017 on 3 wells at Pad 102
- Well stimulations are being investigated
- Additional tubing deployed flow control devices will be looked at for install
- Investigating possible BP drill outs to recover lost sections of laterals

Surmont 2

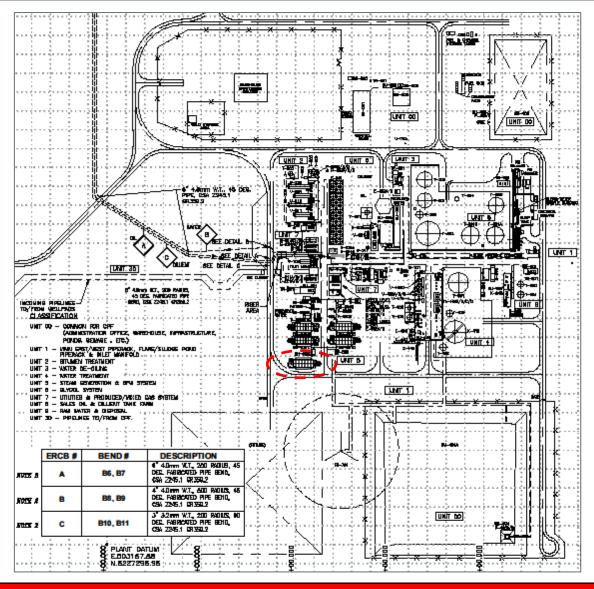
- Start-up remaining 11 wells in Q1 2017
- Start ESP conversions for 5 different pads
- Continue tubing deployed flow control device installations
- Continue more steam splitter installations
- Evaluate well stimulations and redrill opportunities for under performing pads



Surface Operations and Compliance Surmont Project Approval 9426

Facilities Subsection 3.1.2 (1)

Phase 1 Plot Plan: CPF



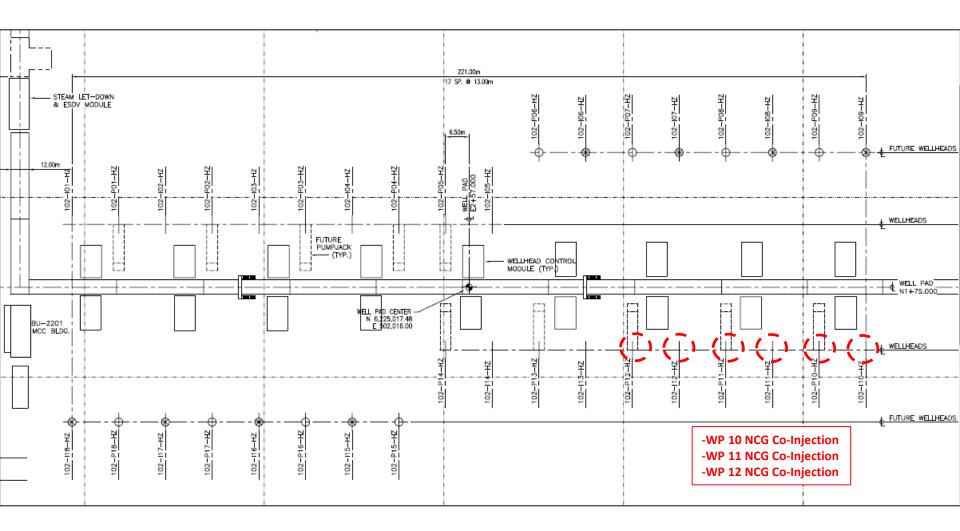
Steam Generator (installed but never tied in) was removed from Phase 1

Subsection

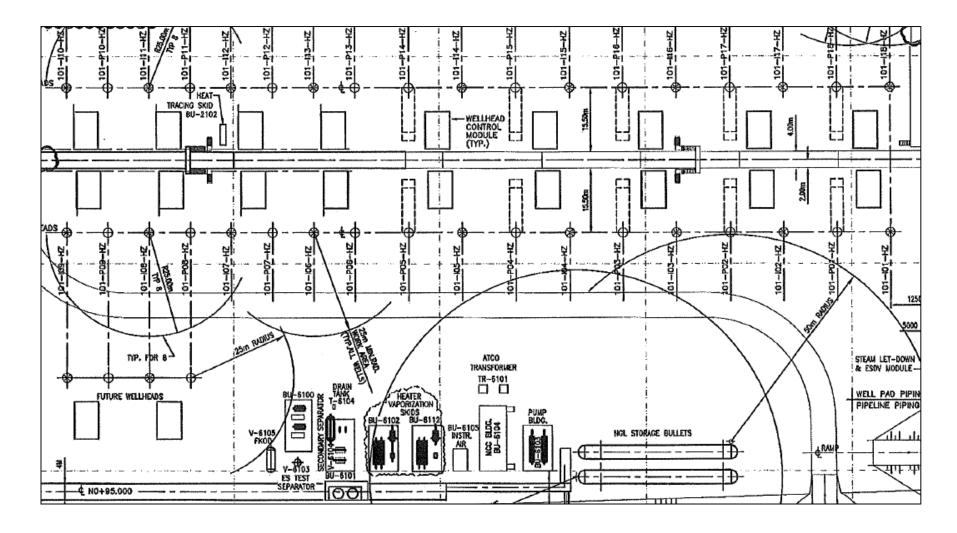
•



Phase 1 Plot Plan: Pad 102

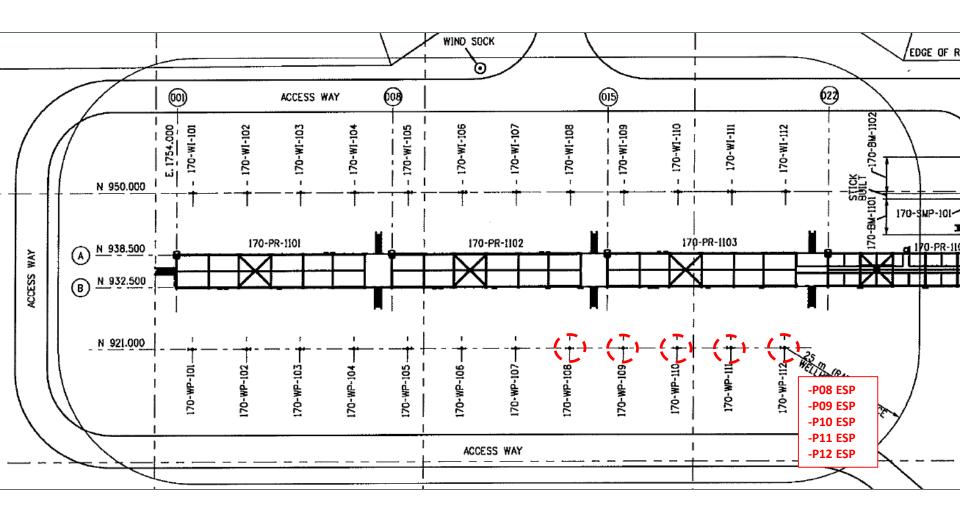


• Non-Condensable Gas (NCG) Co-Injection trial required piping modifications on wellpairs 10, 11, and 12 to tie lift gas lines into heel steam injection lines.



• No ESP Conversions or Major Modifications at Pad 101.

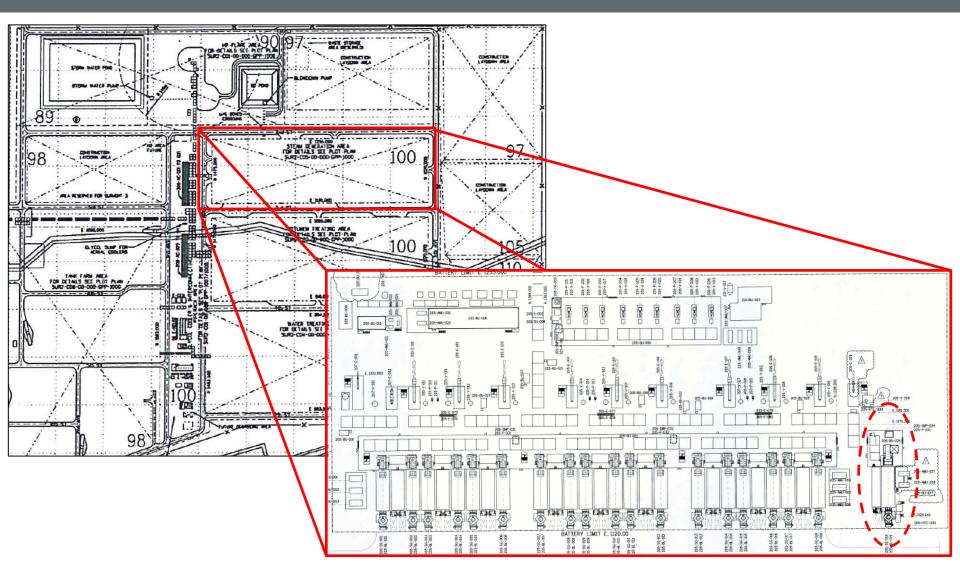




Pad 103 ESP Conversions: Added 3 ESPs in Feb 2016, 1 in Apr 2016, and 1 in Aug 2016

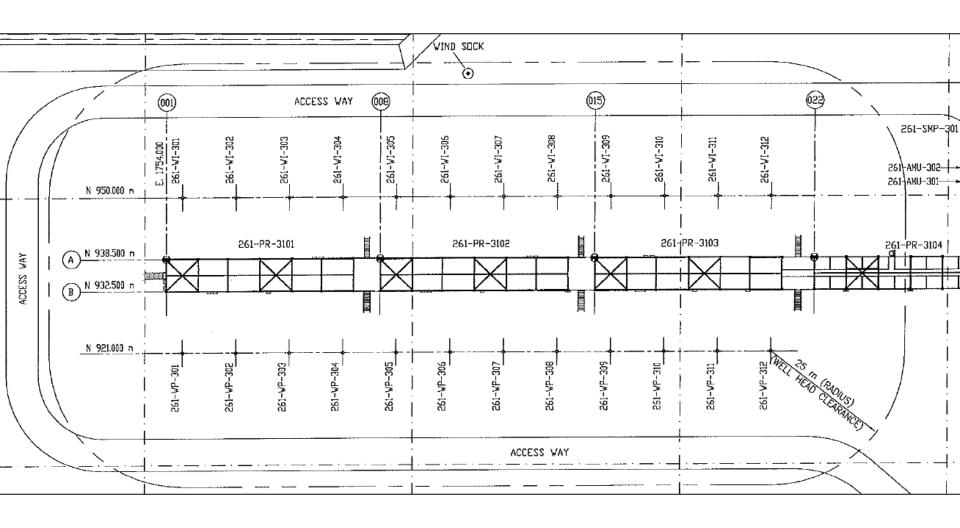


Phase 2 Plot Plan: CPF



Installation of one additional OTSG at Surmont 2, construction work is on-going. No changes in other areas of the plant

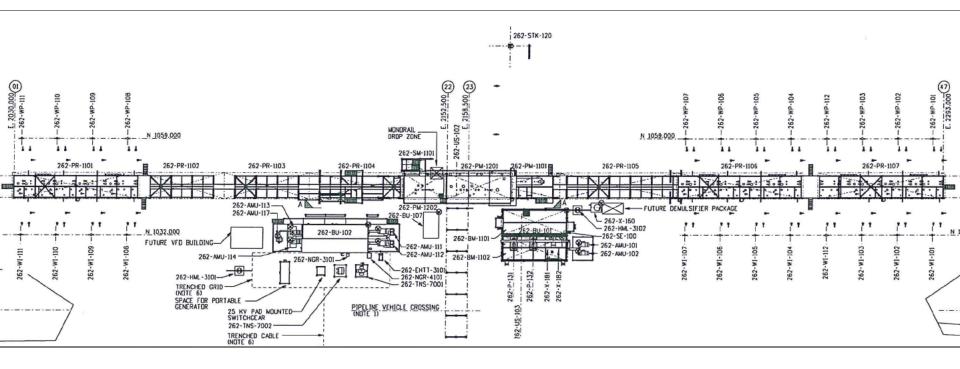
Subsection



No ESP Conversions or Major Modifications at Pad 261-3

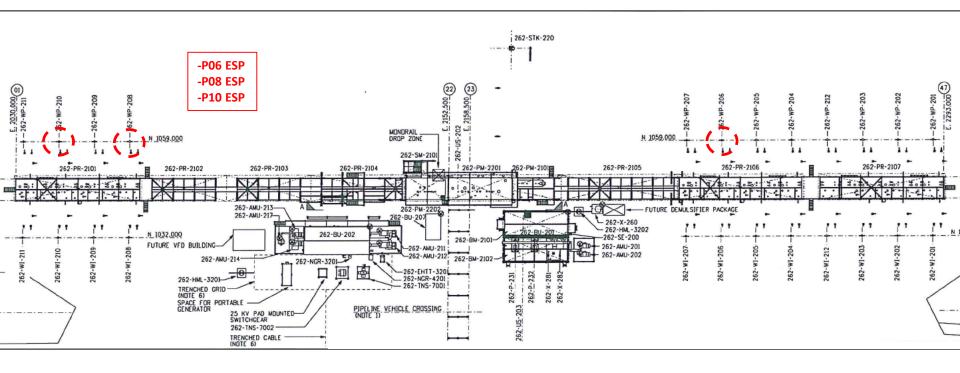


Phase 2 Plot Plan: Pad 262-1



No ESP Conversions or Major Modifications at Pad 262-1

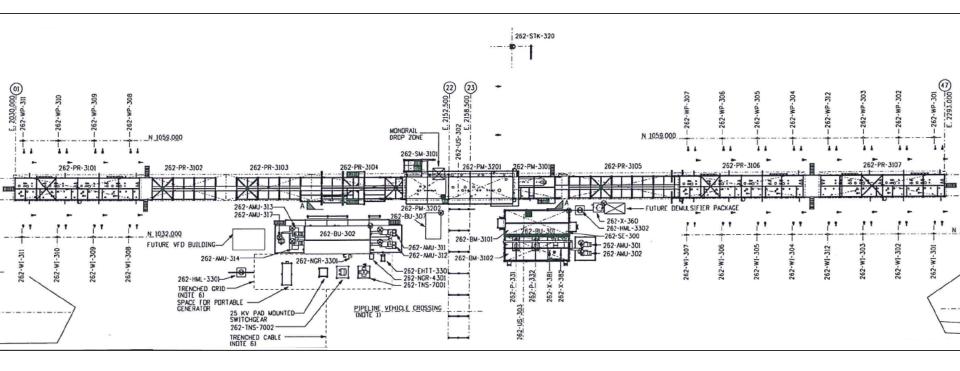




Pad 262-2 ESP Conversions: Added 3 ESPs in Feb 2017



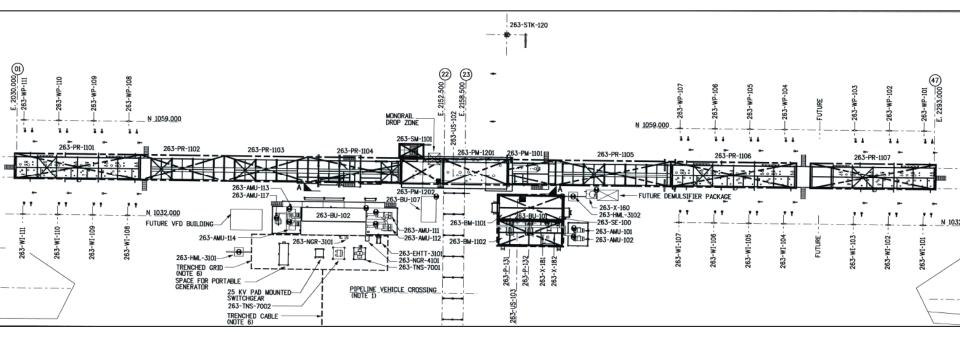
Phase 2 Plot Plan: Pad 262-3



No ESP Conversions or Major Modifications at Pad 262-3



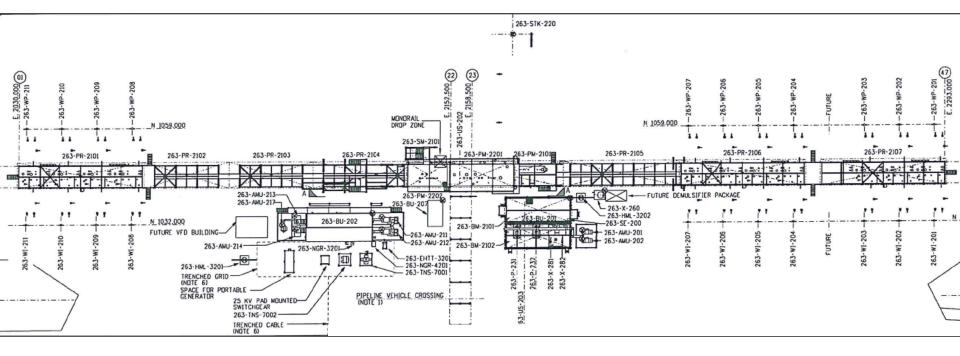
Phase 2 Plot Plan: Pad 263-1



No ESP Conversions or Major Modifications at Pad 263-1



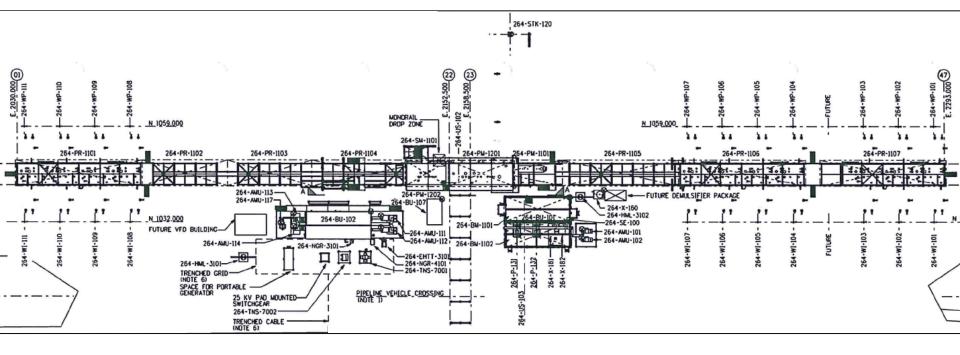
Phase 2 Plot Plan: Pad 263-2



No ESP Conversions or Major Modifications at Pad 263-2



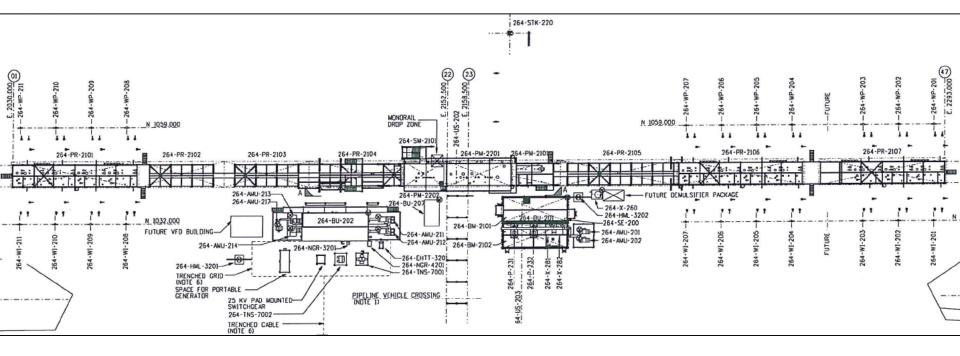
Phase 2 Plot Plan: Pad 264-1



No ESP Conversions or Major Modifications at Pad 264-1



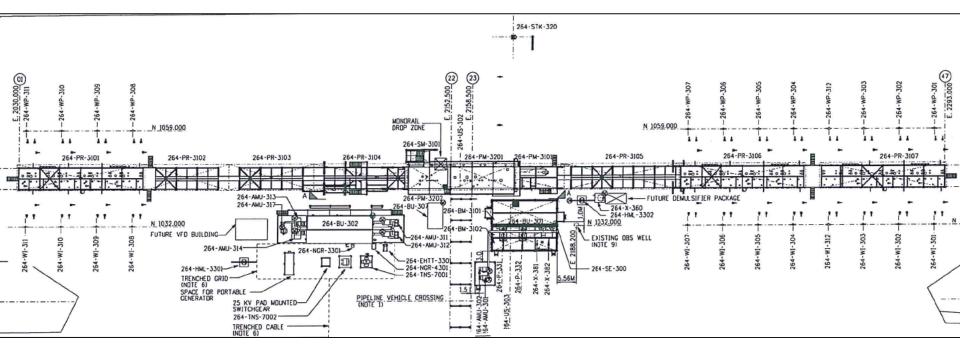
Phase 2 Plot Plan: Pad 264-2



No ESP Conversions or Major Modifications at Pad 264-2



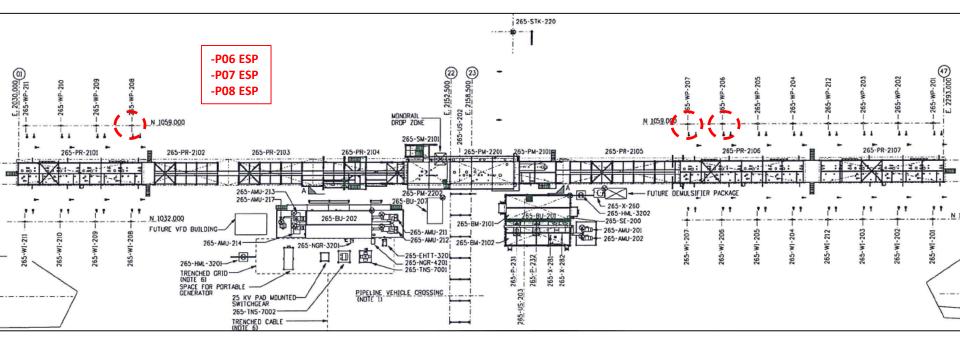
Phase 2 Plot Plan: Pad 264-3



No ESP Conversions or Major Modifications at Pad 264-3



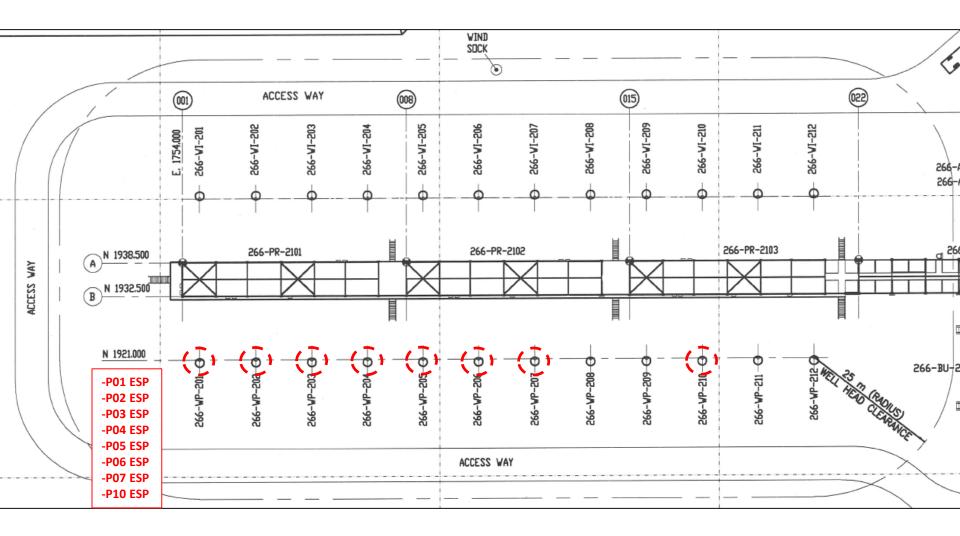
Phase 2 Plot Plan: Pad 265-2



Pad 265-2 ESP Conversions: Added 3 ESPs in Feb 2017



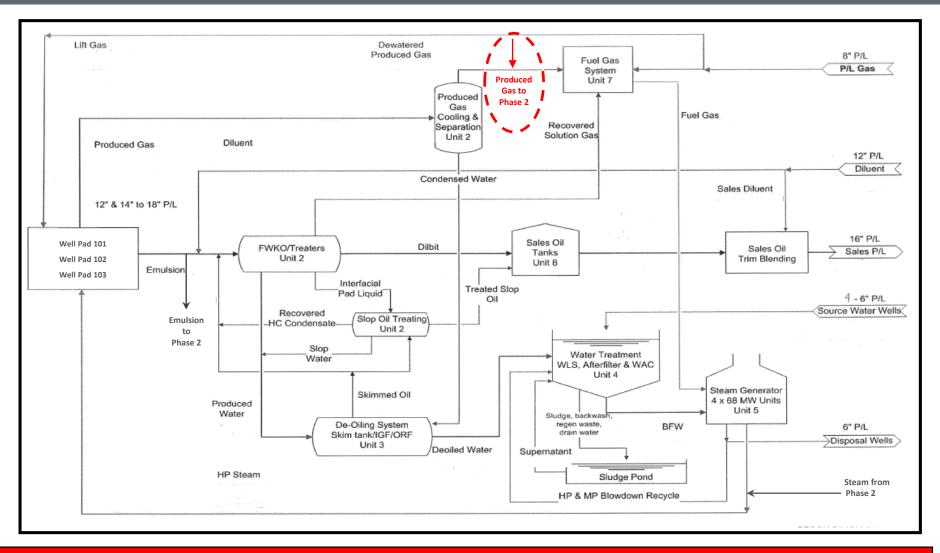
Phase 2 Plot Plan: Pad 266-2



Pad 266-2 ESP Conversions: Added 8 ESPs in Feb 2017

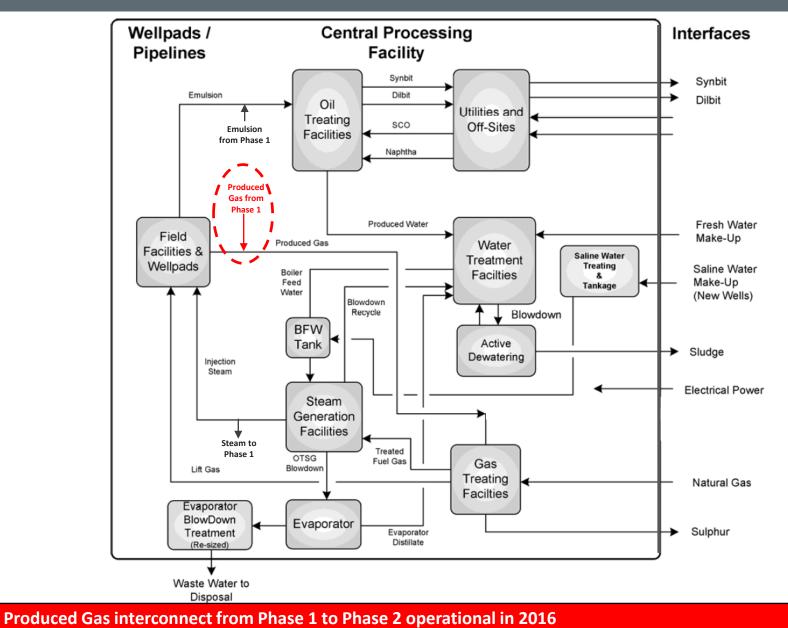


Plant Schematic: Phase 1



Produced Gas interconnect from Phase 1 to Phase 2 operational in 2016

Plant Schematic: Phase 2



Subsection

•

2016 Surmont Operations

• Phase 1:

- Installed new Economizer box on one steam gen with upgraded materials and additional monitoring capabilities.
- Steam control valves upgraded to increase steam production to Pads.
- Installation of forced draft fans on steam generators to maximize air flow, improve combustion and maximize steam production.

• Phase 2

Subsection

- Train 2 and train 3 commissioned and started up.
- Commissioned and started up remaining well pads and prepared for 2017 ESP conversions.
- Low fin thermocouples installation, for monitoring fouling and pigging initiated.



Facility Performance

Subsection 3.1.2 (2)

Facility Performance: Bitumen Treatment by CPF



—— CPF1 —— CPF2

Facility Performance: Bitumen Treatment by Train



Facility Performance: Phase 1 Water Treatment

- Phase 1 water treatment plant continues to operate as per design.
- Chemical trials conducted in 2016 have improved water treatment performance.
- Successful ramp-up from the Fort McMurray Wildfire Emergency Shutdown & Re-start.

Parameter	BFW Specification	Avg. Value	% of time on Spec	
Hardness (Total), mg/L	<0.5	0.31	92.9	
Silica, as SiO2, mg/L	<50	19.6	99.6	
Bitumen in Water, ppm	<0.5	0.24	99.7	
Turbidity, NTU	<3.5	1.05	99.5	

Boiler Feed Water Quality (Feb 1, 2016 to Feb 28, 2017)



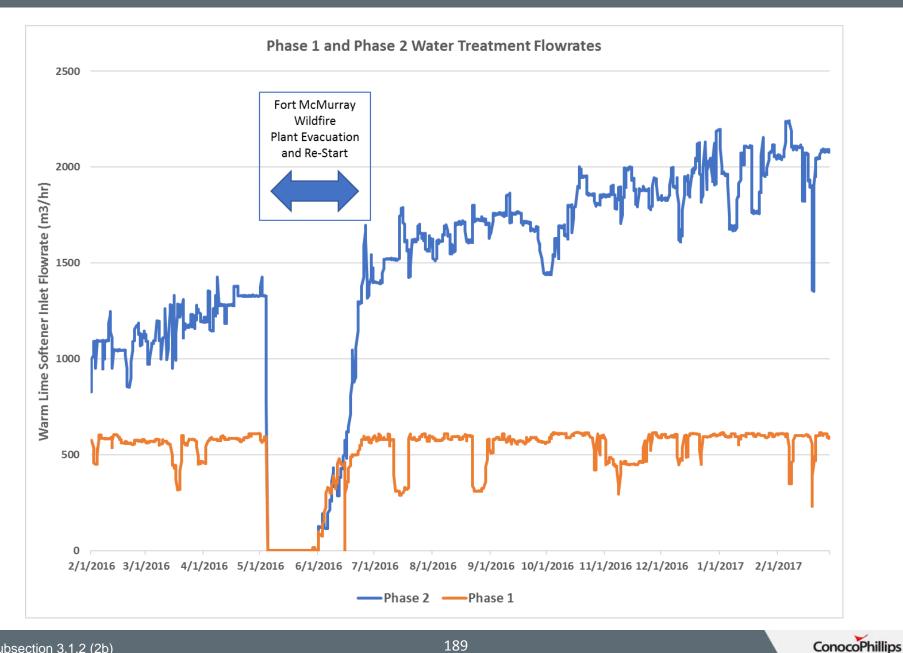
Facility Performance: Phase 2 Water Treatment

- Continued successful ramp up of Phase 2 water treatment plant. Water plant is operating at approximately 80% of nameplate design.
- New well start-ups created deoiling challenges, however the well count has stabilized.
- Successful ramp-up from the Fort McMurray Wildfire Emergency Shutdown & Re-start.

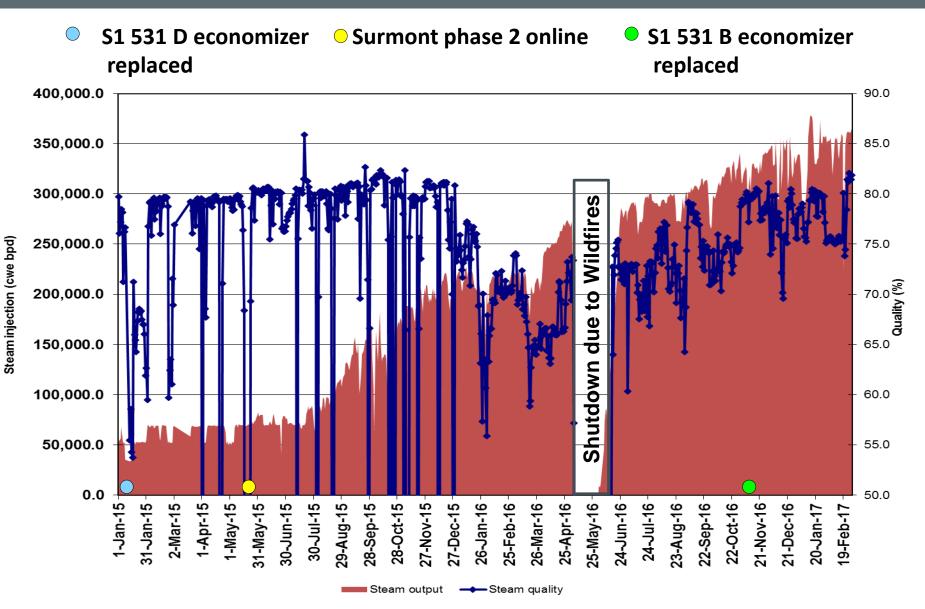
Parameter	BFW Specification	Avg. Value	% of time on Spec	
Hardness (Total), mg/L	<0.5	0.38	83.7	
Silica, as SiO2, mg/L	<50	21.4	100	
Bitumen in Water, ppm	<0.5	0.41	82.4	
Turbidity, NTU	<3.5	1.63	89.9	

Boiler Feed Water Quality (Feb 1, 2016 to Feb 28, 2017)

Facility Performance: Water Treatment



Surmont Project: Steam Generation Performance



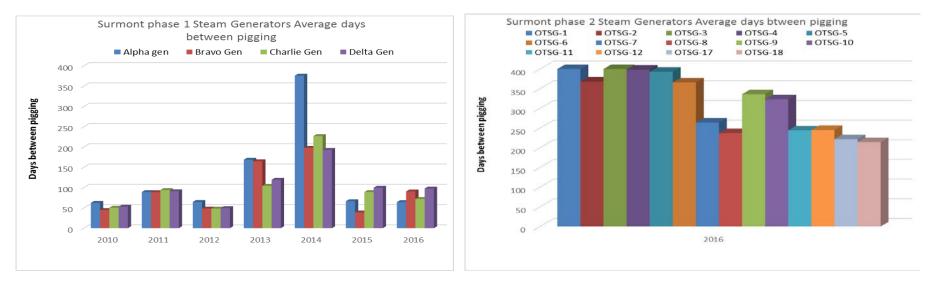
Surmont Phase 2: Steam Generation Performance

- Phase 2 steam generators were commissioned in 2015 and 2016.
- SG-531 B and SG-531 D economizers were replaced (upgraded) on November 2016, allowing for higher steam qualities (83-85%).
- Steam interconnect between Phase 2 and Phase 1 was commissioned in 2015. Excess of steam from Phase 2 is directed to Phase 1 wellpads.
- Average steam rates through interconnect:
 - 2015: ~11,786 bpd.
 - 2016: ~40,021 bpd.
 - 2017: ~29,423 bpd. (January 1 to February 28, 2017)
- Phase 2 continued ramp up in 2016.
- Implementing optimization opportunities like steam enhancement trial



Phase 1 and 2 OTSG Pigging Frequency

Number of pigging events on steam generators and days between pigging.



- The number of pigging events at Phase 1 decreased in 2016 compared with 2015 (15 vs 28 pigging events).
- Well stimulation during October 2015 impacted water quality and pigging frequency during the first quarter of 2016.
- Overall, Phase 2 steam generators have better run time than Phase 1.



Phase 2 Steam Quality Enhancement Trial

			Complete	Complete	In progress			
				294		300		
Q fire, GJ/h	fire, GJ/h		287			Avg. Target 127 m3/h		
-	273			Avg. Target 125 m3/h		Step 3 - 110% Firing		
Target Steam	115 m3/h		Avg. Target 122 m3/h					
Step 0 - 100% Firing			Step 1 - 105% Firing			85%		
Steam Quality	80%		80-83%	83-85%		SP Contraction of the second se		
BFW rate	144 m3/h	ng & SP	153 m3/h	153 m3/h	Pigging & SP	153 m3/h		
Steam Output	115 m3/h	Pigging	121-127 m3/h	127-130 m3/h	Pig	130 m3/h		
Time Line	June-2016 July-2016		Aug-2016 Oct-2016	Oct -2016 Dec -2016		Jan-2017 June-2017		
						1		

Step 3 started on Jan 12

2017 Goal: Step 3 started on January 12, 2017 and data is currently being collected and analyzed.



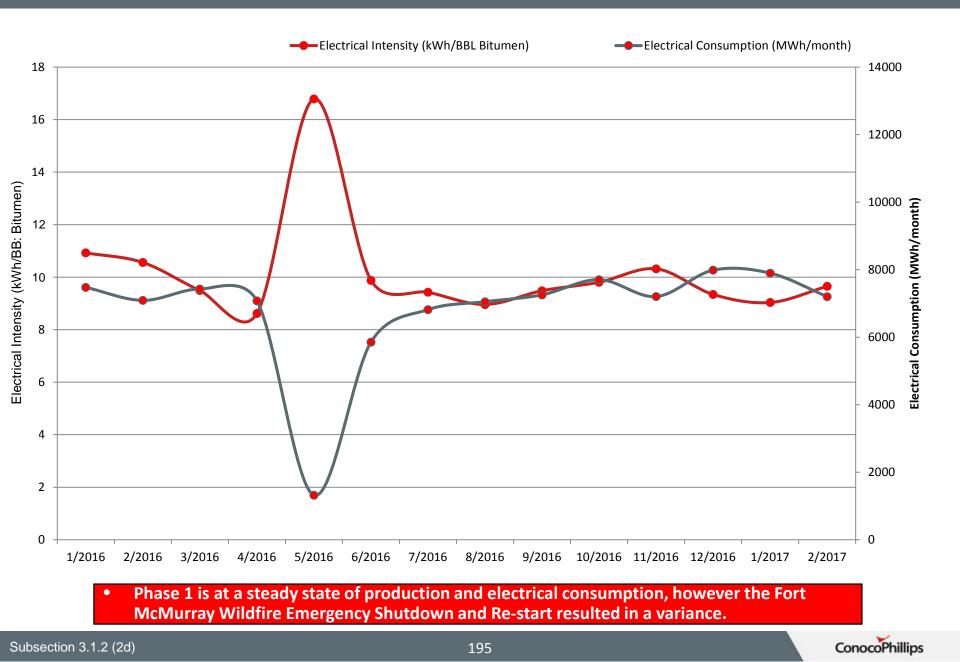
Phase 2 Steam Quality Enhancement Trial

2017 Path forward:

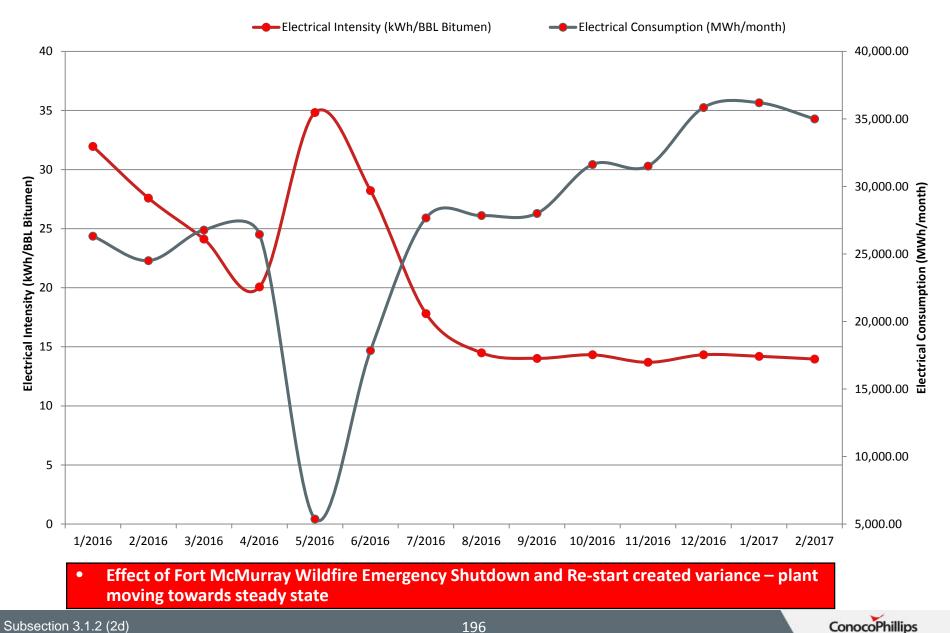
- Steam trials expected to be complete by end of June, 2017.
- Steam gens equipped with additional thermocouples will be fired at 80 – 83% steam quality.
- Install additional thermocouples on remaining Phase 2 gens in 2017.
- Maximize Phase 2 steam production based on learnings from Trial.



Facility Performance: Electricity Consumption Phase 1



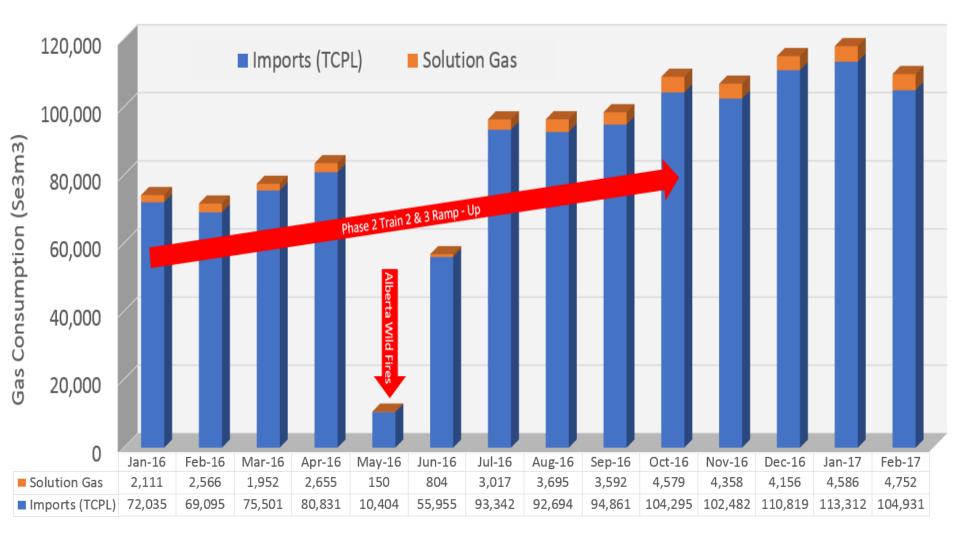
Facility Performance: Electricity Consumption Phase 2



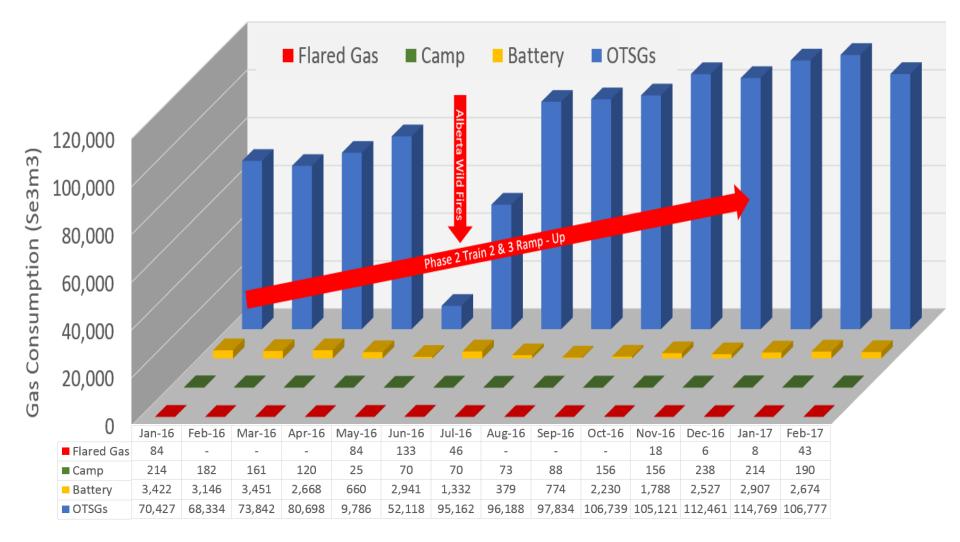
Subsection 3.1.2 (2d)

YEAR	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017
TCPL Gas Imports (10 ³ m ³)	42,999	160,095	183,933	223,447	228,344	250,412	230,339	240,496	433,138	962,313	218,242
Solution Gas (10 ³ m ³)	2,755	4,155	10,073	12,703	13,869	15,193	17,005	14,246	19,301	33,636	9,337
Flared Gas (10 ³ m ³)	4,641	6,439	3,962	705	625	218	117	271	475	371	50
% of Solution Gas Recovery			60.67%	94.45%	95.49%	98.57%	99.31%	98.10%	97.54%	98.90%	99.46%

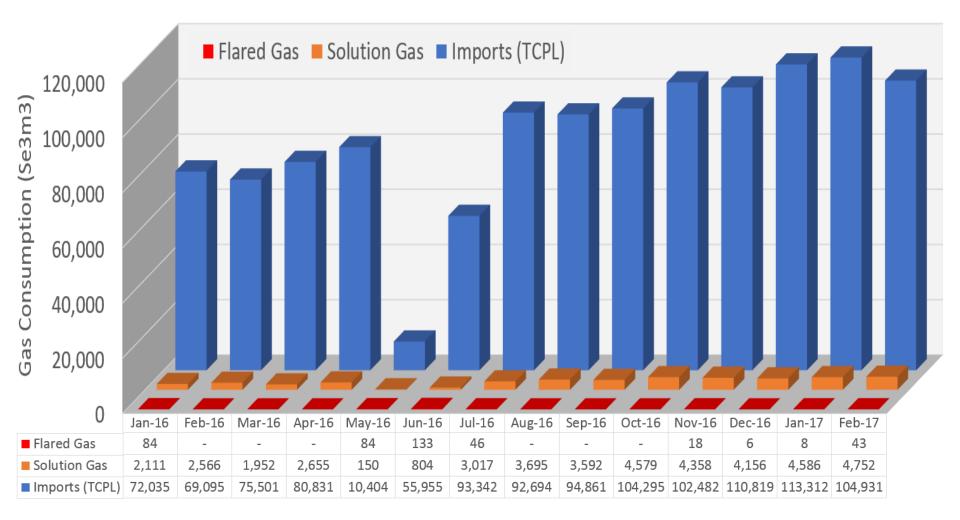
Facility Performance: Gas Consumption



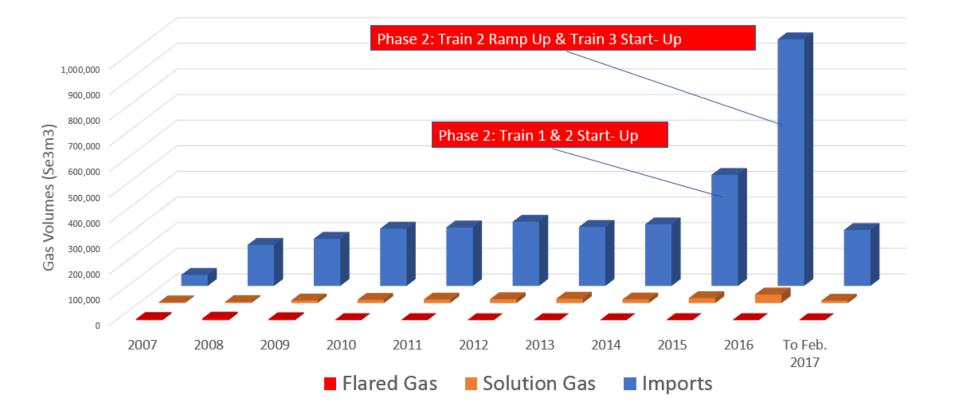
Facility Performance: Gas Consumption by Location



Surmont Facility Performance: 2016 Gas Usage



Surmont Facility Performance: Gas Usage

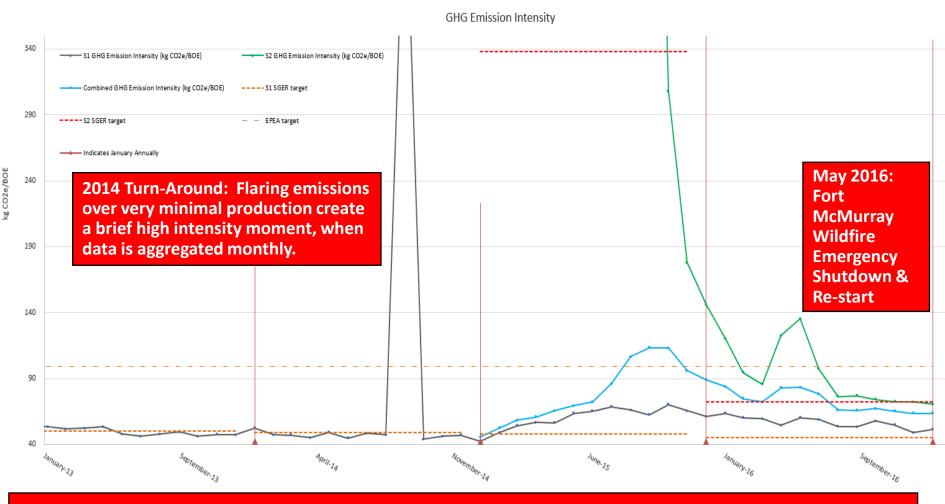


Surmont Facility Performance: Gas Usage - Highlights

- Amount of flared gas was influenced by the following events in 2016:
 - Start-up of Surmont 2 Trains 2 and 3
 - Start-up of six Surmont 2 Well Pads
 - Well Operation shifting from Circulation to Gas Lift and/or ESP
 - May Fort McMurray Wildfire Emergency Shutdown and June re-start



Facility Performance: Greenhouse Gas



• Agreement with AER to continue reporting Phase 2 CO2e emission, through its rampup, separately from Phase 1.

• 2016 Phase 1 SGER intensity reduction target of 15% was not achieved.

• 2016 GHG Emission intensity has ben completed, verified and payment submitted.



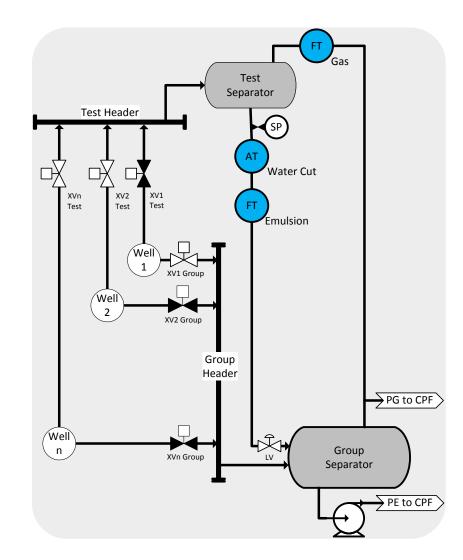


Measurement and Reporting

Subsection 3.1.2 (3)

Well Testing

- Surmont Well Pads are configured to, automatically and sequentially, align each production well into the Test Separator.
- Well Test Duration, Total Produced Emulsion, Average Water Cut and Total Produced Water Vapors are recorded for each Well Test.
- Well Test Results are reviewed to "Approve", if representative of the wells production, or "Reject."
- Well Test Durations range from 5 to 10 hours, with up to 4 hours purge, based on the wells previous liquid production rates.





Each well's estimated monthly production is calculated using only "approved" Well Test Results. Daily estimated volumes are used to calculate the wells monthly estimated volume from the time of an approved well test, until its next approved well test.

Well Monthly Estimated Oil Production =

Well Estimated Daily Oil Production \times Hours per Days in Operation

Well Estimated Daily Oil Production =

Test Produced Emulsion Volume $\times (1 - WC\%) \times 24$ hours Test Duration (hours)

Well Monthly Estimated Water Production =

Well Estimated Daily Water Production \times Hours per Days in Operation

Well Estimated Daily Water Production =

Test Produced Emulsion Volume \times WC% + Water Vapor \times 24 hours

Test Duration (hours)



Well Allocated Oil Production

Well Estimated Monthly Oil Production imes Oil Proration Factor

Oil Proration Factor =

Battery Produced Oil

Total Estimated Monthly Oil Production

• Battery Produced Oil =

Oil Dispositions + Battery Tank Inventory + Shrinkage – Receipts + Well Load Oil

Total Estimated Monthly Oil Production =

 $\sum_{n=1}^{x} Well_n Estimated Montly Oil Production$

where x is the total number of production wells for the reporting period.

• Oil Dispositions =

Sales CTM¹ + Enbridge Tank Inventory + TruckOut

• Oil in Battery's Tank Inventory =

Sales Oil Tanks + OffSpec Tanks + Slop Oil Tanks + Skim Oil Tanks

• Receipt =

Diluent CTM¹+ Diluent Tank Inventory + Diluent TruckIn



Well Estimated Monthly Water Production imes Water Proration Factor

• Water Proration Factor =

Battery Produced Water

Total Estimated Monthly Water Production

• Battery Produced Water =

Water Dispositions + Battery Tank Inventory - Receipts + Well Load Water

Total Estimated Monthly Water Production =

 \sum Well_n Estimated Montly Water Production

where x is the total number of production wells for the reporting period.

Water Dispositions =

Dispositions to Injection Facility + Truck-Out

Water in Battery's Tank Inventory =

Skim Oil Tanks + Slop OilTanks + DeSand/BackWash/ORF Tanks + Sales/OffSpec/Diluent Tanks

• Receipt =

IF Condensate Returns + Water in Diluent + Truck-In



2016 Well Oil and Water Production Highlights and Changes

- After May 2016 Pilot Plant ceased operations, Diluent, Produced Oil and Water receipt/dispositions between Surmont and the Pilot Plant no longer exist.
- At the Test Separator, include the accounting of Water Produced as Vapour, to better estimate water returns during Steam Circulation.
- Large number of wells shifting operating mode, from start-up Circulation to SAGD Production, Gas Lift and/or ESP.
- Considerable effort implemented to achieve water cut meter's performance under shifting well operating conditions.



Well Allocated Oil Production imes GOR

• Gas to Oil Ration (GOR) =

Battery Produced Gas Battery Produced Oil

Battery Produced Gas =

Gas Dispositions – Receipts

Gas Dispositions =

Battery Utility FG + Steam Generators FG + Flare Purge + NCG Colnjection + Flared Gas

• Receipt =

TCPL Fuel Gas CTM¹

¹ CTM: Custody Transfer Meter



2016 Well Gas Production Highlights and Changes

- Non Condensable Gas (NCG) Co-Injection Trial initiated November 2016. Co-Injected volumes are measured and added to the Battery's gas dispositions.
- Plant Control System (DCS) shutdown during Fort McMurray Wildfire Emergency Shutdown & Re-start. Flare volumes were accounted for until DCS shutdown.
- After wildfires, fuel gas was injected into the injection wall (semi-SAGD operation) to restart some S2 wells. The fuel gas injected did not immediately return to the Battery; therefore, the calculated Battery's Produced Gas resulted into "negative volumes" for June 2016 reporting period.



Well Allocated Steam

Well Measured Steam imes Steam Proration Factor

• Well Measured Steam =

Steam Injected @Heel + Steam Injected @Toe

• Steam Proration Factor =

Steam Produced Total Measured Steam

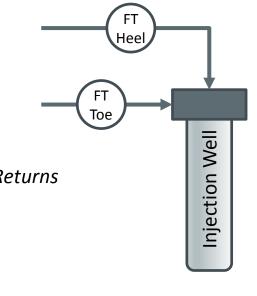
Steam Produced =

Steam Generated (CPF) – Steam Condensate Returns

Total Measured Steam =

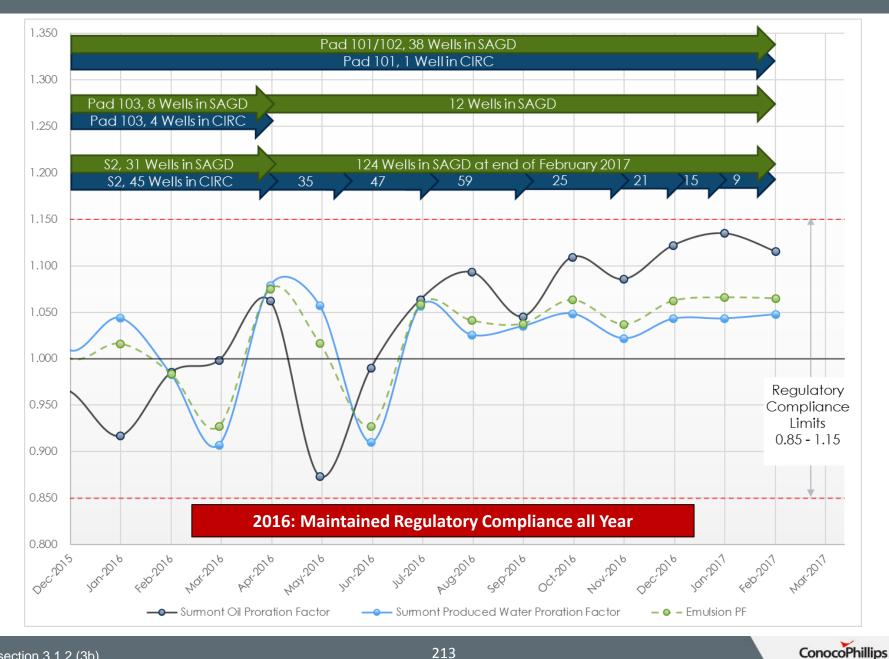
 $\sum_{n=1}^{x} \operatorname{Well}_{n} \operatorname{Measured} \operatorname{Steam}$

where x is the total number of injection wells during the reporting period.

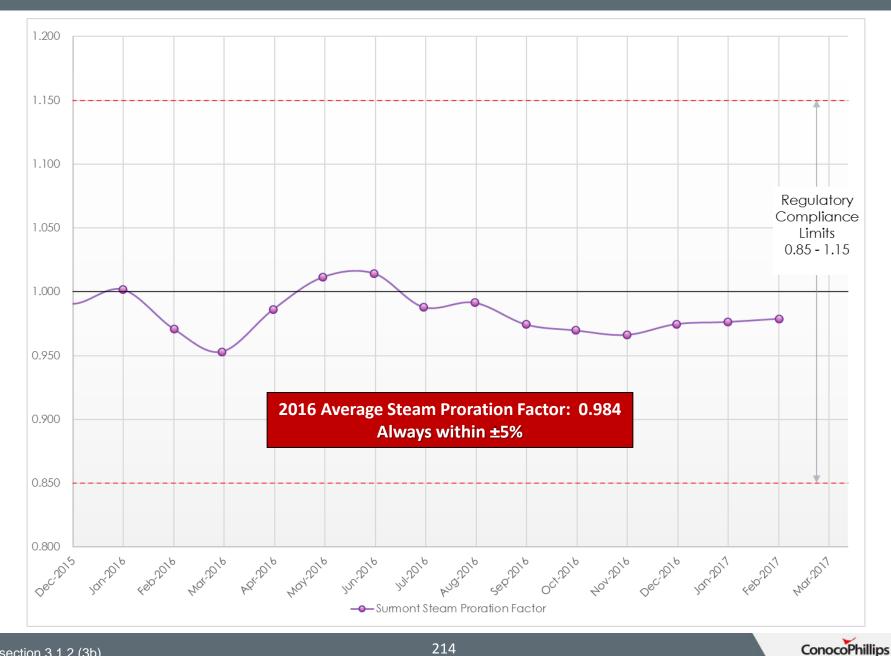




Oil and Water Production Proration Factors



Steam Injection Proration Factor

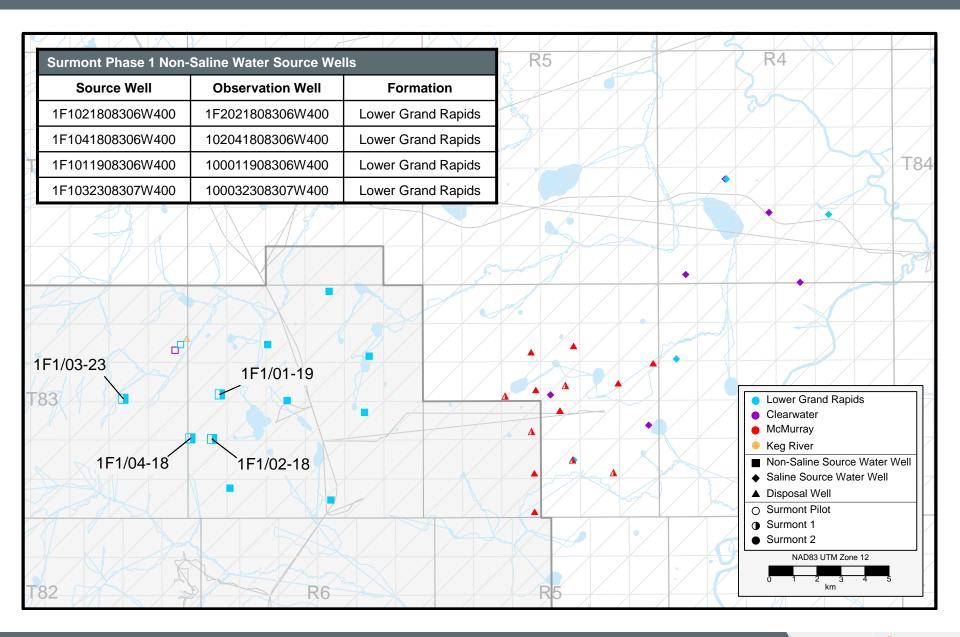




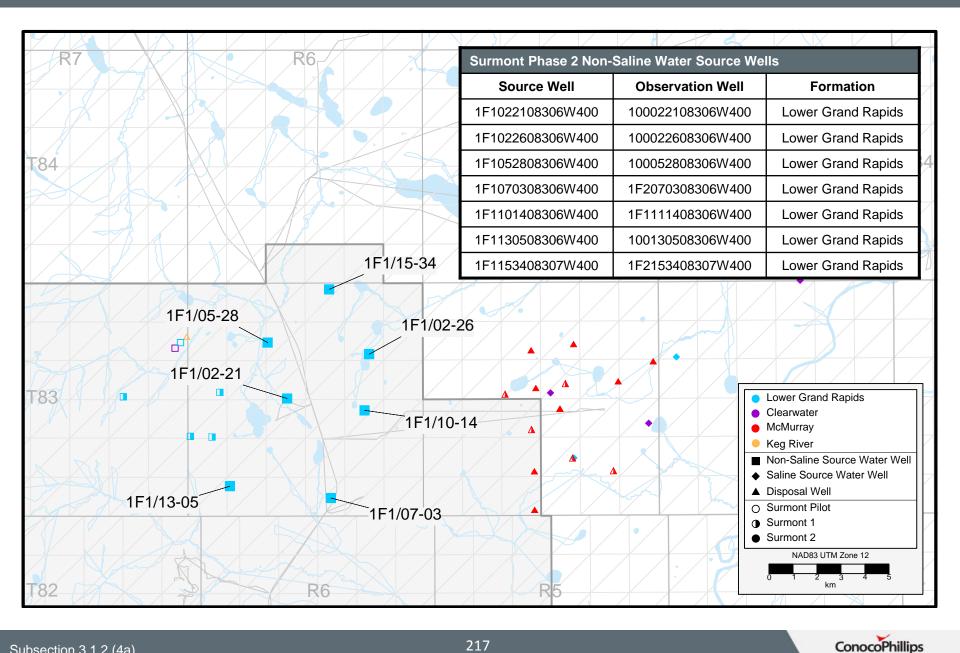
Water Production, Injection, and Uses

Subsection 3.1.2 (4)

Surmont Phase 1 Non-Saline Water Source Wells



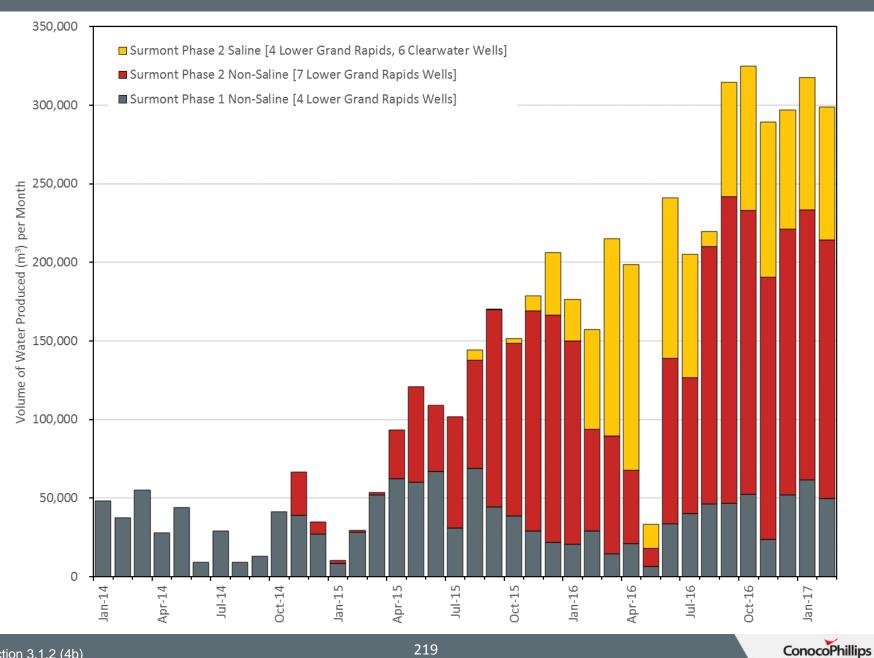
Surmont Phase 2 Non-Saline Water Source Wells



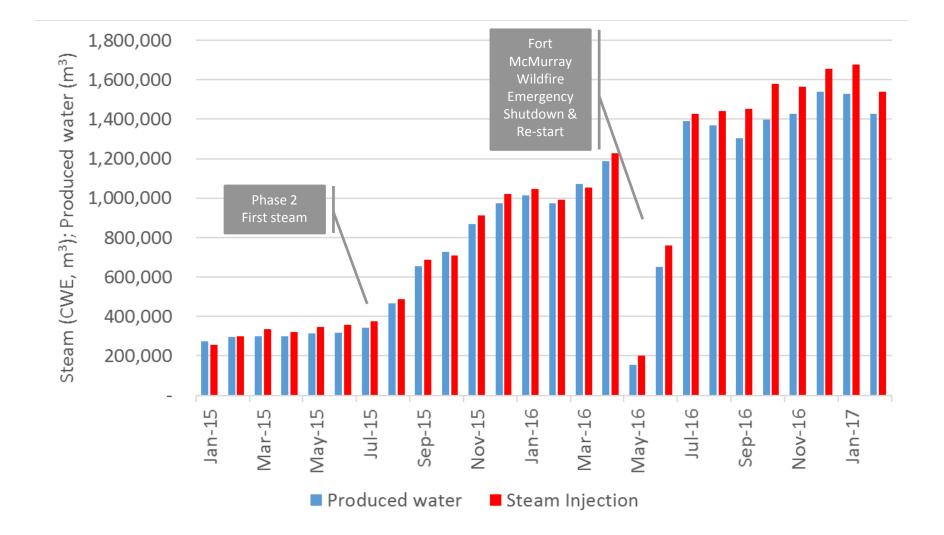
Surmont Phase 2 Saline Water Source Wells

Surmont Phase 2 Salin	a Water Source Wells	R5 R4
Source Well	Formation	
1F1020308404W400	Clearwater	
1F1020608404W400	Clearwater	
1F1033008304W400	Lower Grand Rapids	1F2/09-17 T8
1F1042208305W400	Clearwater	. 1F1/10-17
1F1071308305W400	Clearwater	1F1/16-09
1F1081008305W400	Lower Grand Rapids	1F2/14-11
1F1101708404W400	Clearwater	1F1/02-06
1F1160908404W400	Clearwater	1F1/02-03
1F2091708404W400	Lower Grand Rapids	
1F2141108404W400	Lower Grand Rapids	1F1/04-22
3		 Lower Grand Rapids Clearwater McMurray
		1F1/08-10 ● Keg River ■ Non-Saline Source Water Well ◆ Saline Source Water Well ▲ Disposal Well
32	R6	A Disposal vveli O Surmont Pilot O Surmont 1 Surmont 2 NADB3 UTM Zone 12 O 1 2 3 4 5 km

Surmont Non-Saline and Saline Water Source Wells Production Volumes

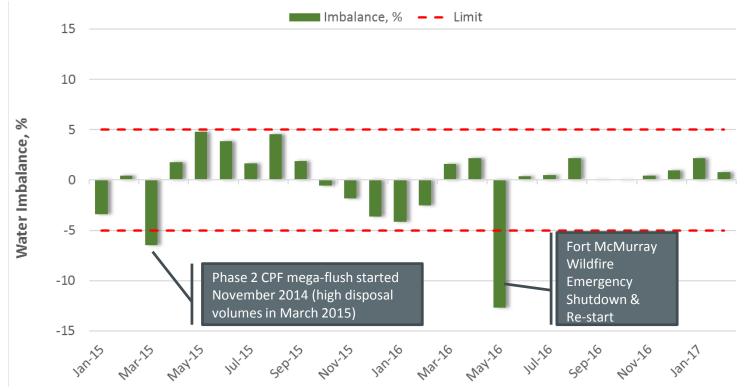


Water Production and Steam Injection Volumes



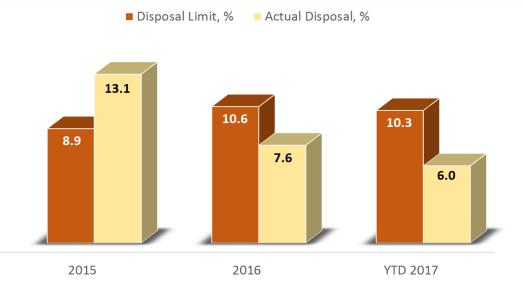
Directive 81: Injection Facility Water Imbalance

- Surmont in compliance with *Directive 81* Injection Facility Water Imbalance since June 2014
- Challenging to keep metering imbalance within 5% when performing large projects (Phase 2 CPF mega-flush Nov 2014 - Mar 2015) or unplanned events (Fort McMurray Wildfire Emergency Shutdown and Re-start May 2016)
- Maintained compliance during Phase 2 ramp up





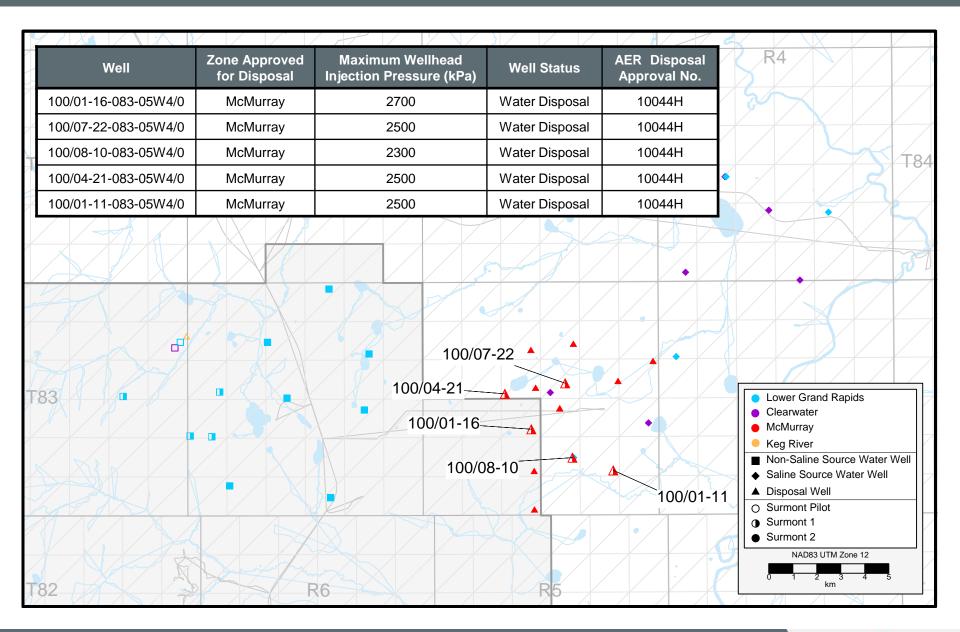
Directive 81: Annual Disposal performance



- Surmont anticipates *Directive 81* disposal limit compliance in 2017 as per current trend (6.0% actual vs. 10.3% disposal limit)
- Surmont accomplished *D-81* compliance in 2016 (7.6% actual vs. 10.6% disposal limit) after commissioning brackish water system and blowdown evaporators at Phase 2 CPF
- Excess disposal in 2015 due to:
 - Phase 2 ramp-up (Testing 12 out of 18 OTSGs)
 - Performed Phase 2 CPF mega-flush (started in Nov 2014 and disposed in Mar 2015)
 - Significant repair work on Phase 1 OTSG-D
 - Well caustic work causing significant water plant upset



Surmont Phase 1 Water Disposal Wells



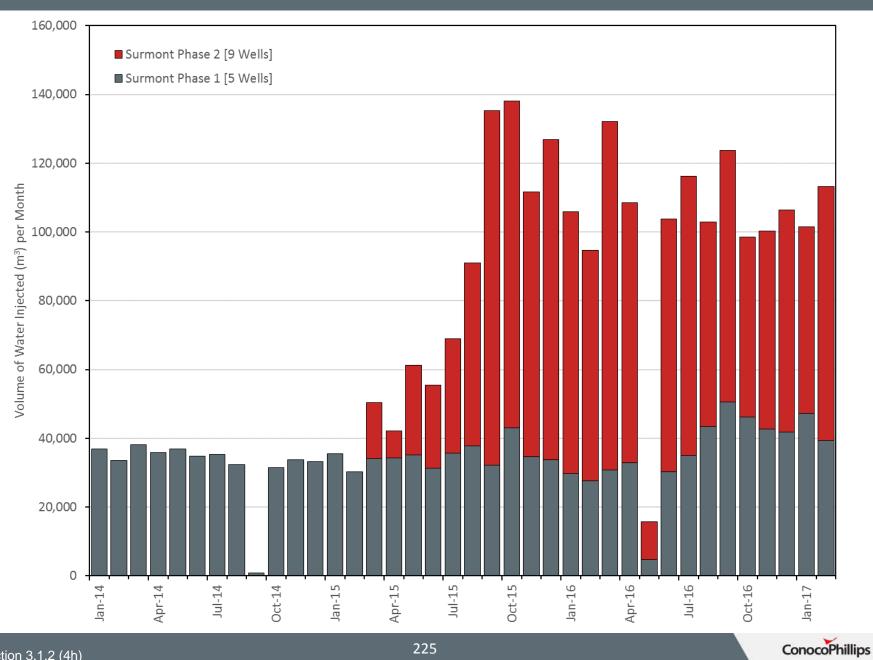


Surmont Phase 2 Water Disposal Wells

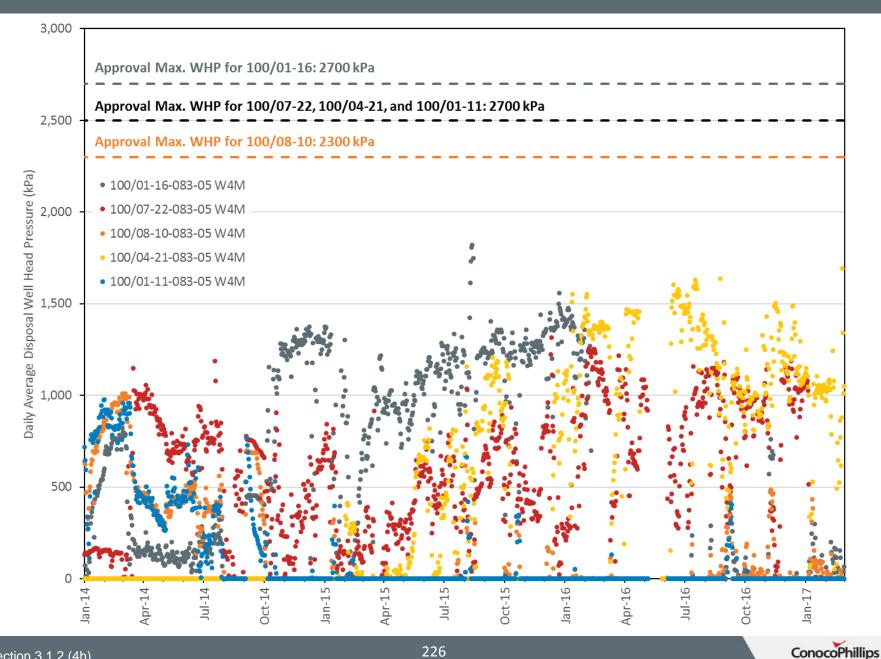
Well	Zone Approved for Disposal	Maximum Wellhead Injection Pressure (kPa)	Well Status	AER Disposal Approval No.	R4
100/01-09-083-05W4/0	McMurray	3400	Water Disposal	10044H	
100/01-04-083-05W4/0	McMurray	2500	Water Disposal	10044H	
102/08-21-083-05W4/0	McMurray	3400	Water Disposal	10044H	
100/01-28-083-05W4/0	McMurray	3400	Water Disposal	10044H	•
100/10-15-083-05W4/0	McMurray	3400	Water Disposal	10044H	
102/15-15-083-05W4/0	McMurray	3400	Water Disposal	10044H	
100/08-27-083-05W4/0	McMurray	3400	Water Disposal	10044H	
100/08-23-083-05W4/0	McMurray	3400	Water Disposal	10044H	
100/16-24-083-05W4/0	McMurray	3400	Water Disposal	10044H	
		100/01-28 102/08-21 102/15- 100/01-0	.15	-100/08-27 100 100/08-2 100/10-15	 Clearwater McMurray Keg River Non-Saline Source Water Well Saline Source Water Well Disposal Well O Surmont Pilot
T82	F	100/01-0	04 R5		● Surmont 1 ● Surmont 2 NAD83 UTM Zone 12 0 1 2 3 4 5 km



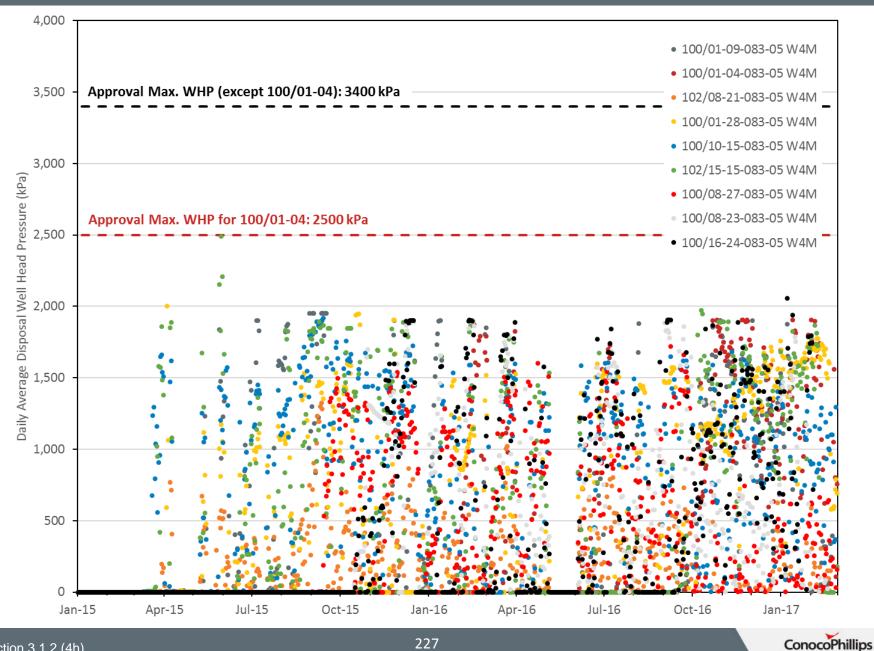
Surmont Water Disposal Wells Injection Rates (McMurray)



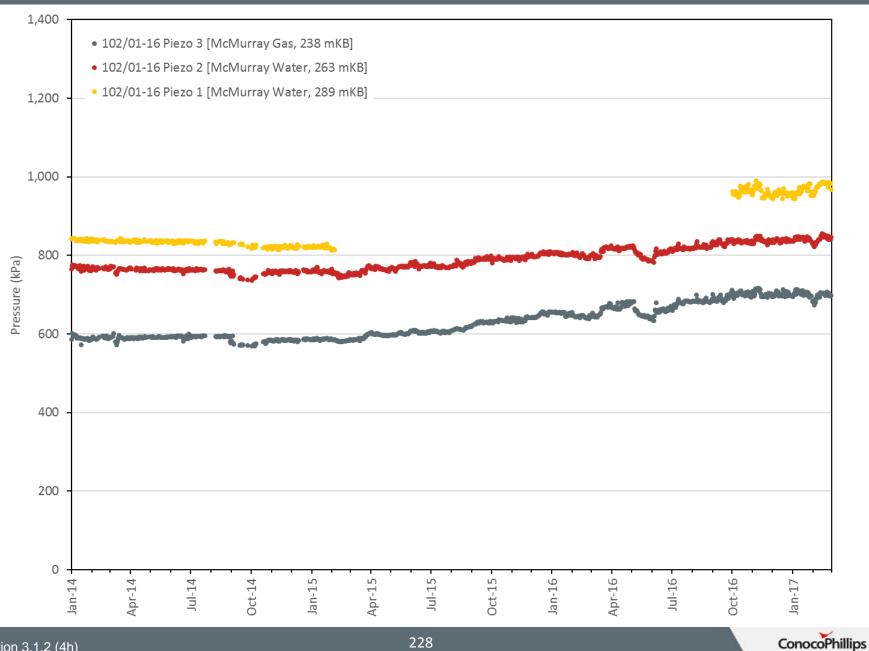
Surmont Phase 1 Water Disposal Wells Well Head Pressure (McMurray)



Surmont Phase 2 Water Disposal Wells Well Head Pressure (McMurray)

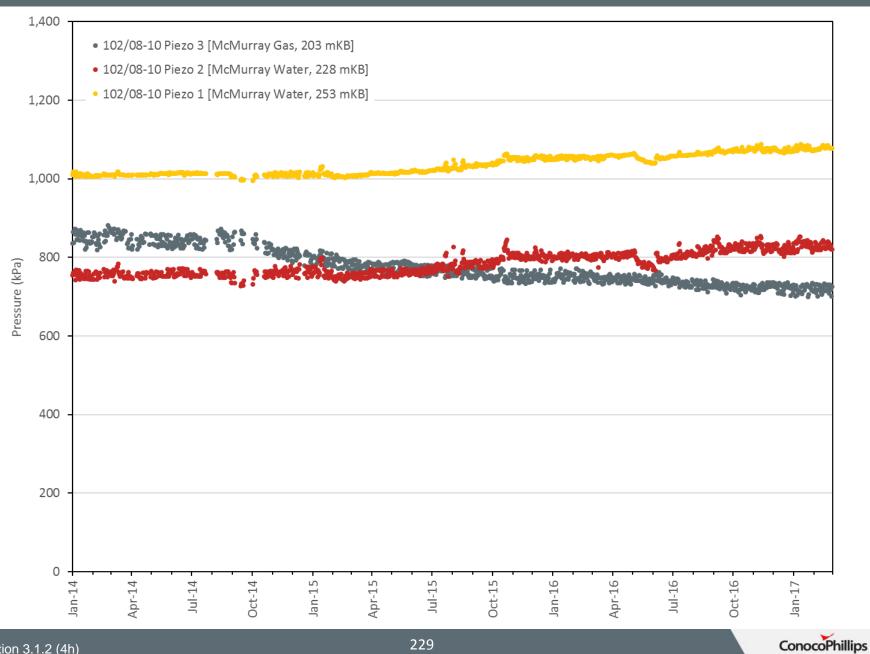


Water Disposal Well 100/01-16-083-05 W4M Observation Well Pressure (McMurray)



Subsection 3.1.2 (4h)

Water Disposal Well 100/08-10-083-05 W4M Observation Well Pressure (McMurray)



Waste Disposal

Waste Description	Disposal Weight (Tonnes)	Disposal Method	
Dangerous Oilfield Waste	63,855		
Hydrocarbon/Emulsion Sludge	4,167	Oilfield Waste Processing Facility	
Crude Oil/Condensate Emulsions	58,463	Oilfield Waste Processing Facility	
Various	1,224	Landfill	
Non-Dangerous Oilfield Waste	27,918		
Lime Sludge	17,633	Landfill	
Various	9,486	Landfill	
Well Fluids	799	Cavern	



Waste Recycling

Waste Description	Disposal Weight (Tonnes)	Disposal Method	
Oil	17	Used Oil Recycler	
Empty Containers	4	Recycling Facility	
Fluorescent Light Tubes	1	Recycling Facility	
Batteries	3	Recycling Facility	



Typical Water Analysis

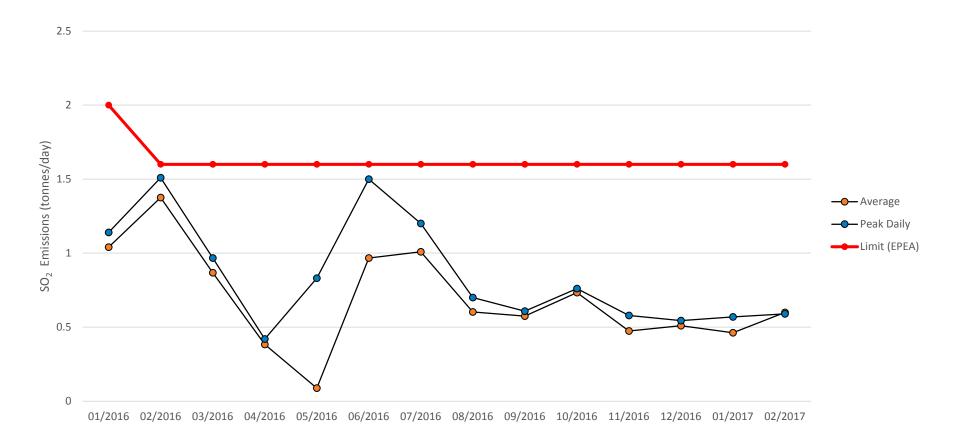
Parameter	Non-Saline Makeup Water (mg/L)	Saline Makeup Water (mg/L)	Produced Water (mg/L)	Disposal Water (mg/L)
рН	8.5	8.2	7.5	11.8
Total Dissolved Solids (TDS)	1,400	8,000	1,800	23,000
Chloride	200	2,800	650	9,500
Hardness as CaCO ₃	<0.5	225	10	5
Alkalinity as CaCO ₃	900	350	250	2,700
Silica	8	7	190	225
Total Boron	6	3.3	40	260
Total Organic Carbon	15	4	500	2,150
Oil Content	<1	<1	65	30



Sulphur Production

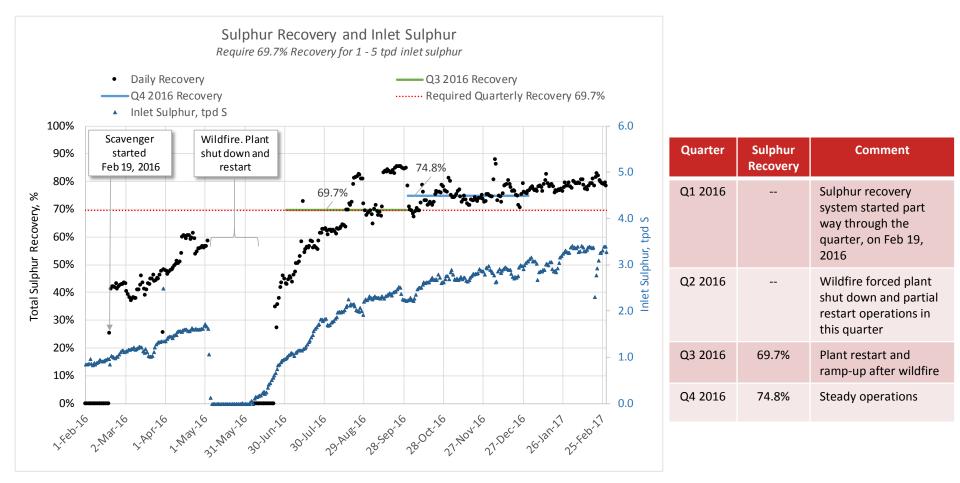
Subsection 3.1.2 (5)

Daily SO₂ Emissions



Subsection 3.1.2 (5c)

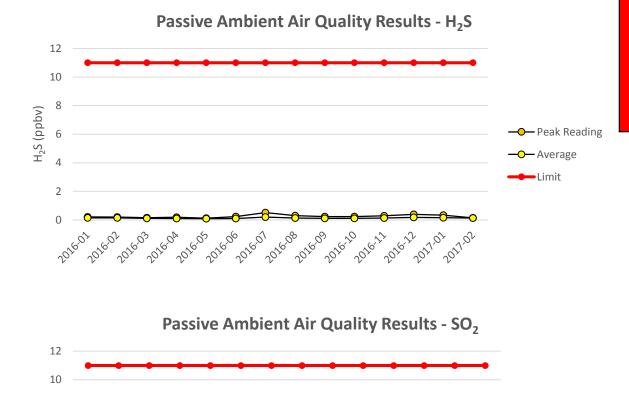
Surmont Project Sulphur Recovery



- Sulphur recovery unit commissioned in Q1 and restarted in Q2
- Sulphur recovery unit met or exceeded 69.7% recovery limit during Q3 and Q4.



Ambient Air Quality Monitoring



2016-08

2016-09

2016-10

2016-11

2016-12

2017.01

 Continuous ambient air monitoring: all Alberta Ambient Air Quality Objectives were met in 2016



2016.02

2016.04

2016.05

2016-06

2016-07

2016-03

8

6

4

2

0

2016-01

SO₂ (ppbv)

2017.02

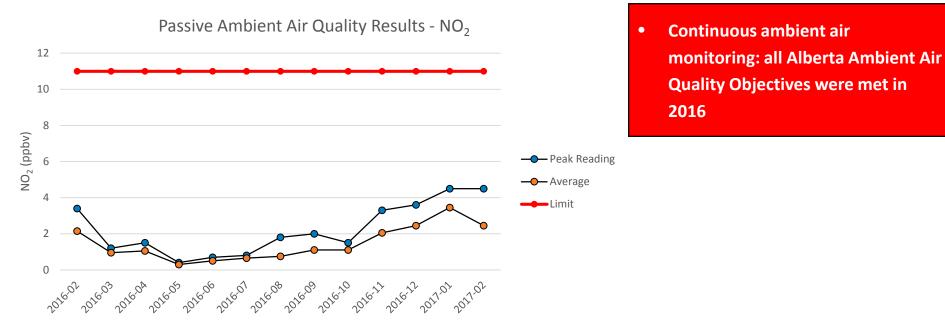
——— Peak Reading

–O— Average

Limit



Ambient Air Quality Monitoring







Environmental Compliance

Subsection 3.1.2 (6)

Environmental Monitoring

- Groundwater Monitoring Program
 - Management triggers introduced as per EPEA approval 48263-01-00.
 - 2016 monitoring results are being analyzed in 2017
 - New monitoring well northeast of the Surmont Phase 1 Storm Pond.
- Wetlands
 - Management triggers introduced as per EPEA approval 48263-01-00.
 - Program revised to focus monitoring on early change detection.
 - 2016 results are within background concentrations.
- Wildlife Monitoring Program
 - Management triggers introduced as per EPEA approval 48263-01-00.
 - Program revised to focus monitoring on early change detection.
 - One vehicle animal collision.
 - No serious nuisance wildlife or human-bear interactions.
- Reclamation Work
 - No final reclamation completed in 2016.
 - A density trial was conducted by planting 44,710 vegetation seedlings at soil stockpile near the Surmont Regional Residence



- Update to the Reclamation Monitoring Program Proposal
 - Per Schedule IX of EPEA Approval number 48263-01-00, as amended, a update to the Reclamation Monitoring Program proposal was due to AEP on or before December 31, 2016.
 - An extension to February 28, 2017 was granted and the updated proposal was submitted.





Compliance Confirmation and Non Compliances

Subsection 3.1.2 (7) + (8)

Compliance Confirmation and Non Compliances

ConocoPhillips Canada is in regulatory compliance for 2016 with the exception of the following:

264-2 I09 Overpressure Event

• Bottomhole pressure exceeded by 100 kPa for 7.5 hours.

Surmont Phase 1 Pond Primary Liner Leak

- A corrective action plan was submitted in 2015 and the action items were completed.
- CPC will be submitting an update to the AER during Q2 2017.

Surmont Phase 2 Storm Pond Certificate of Completion Submitted March 22, 2016

• Certificate of Completion was not submitted within 60 days of completion.

Remote Sump Non-Compliance (33-081-06W4)

• The site entrance was missing a sign, and it has been corrected.

Compliance Confirmation and Non Compliances

AER Investigation into Master Well Valve Failure (264-1 105, January 7, 2017)

- AER investigation is still on-going.
- No non-compliances were identified during clean-up inspections to date.

Air Monitoring Frequency

Continuous Emissions Monitoring System (CEMS) and air monitoring trailer downtime exceedance.





Future Plans

Subsection 3.1.2 (9)

Future Plans – Surmont

Phase 1

- Turn around planned for September 2017
- Upgrade of economizer box on remaining Phase 1 steam generator (OTSG A) to improve steam quality
- Continued monitoring of leaking Pond Primary Liner

Phase 2

- Completion of construction of relocated steam generator and high pressure steam separator, commissioning is targeting Q4 2017
- Design work is ongoing for the installation of an additional steam generator
- Mechanical cleaning of select Boiler Feed Water Pre-heat exchangers for improved heat integration
- Continued work on steam quality enhancement
- Continued ramp-up of Phase 2 production towards plant capacity
- Trial for alternative diluent supply scheduled for Q2 2017

Future Pad Developments

6 Surmont Lease Development Area 84-6W4 84-7W4 Well Pad (existing) Well Pad (planned) Subsurface Drainage Areas 262-1 Planned Subsurface Drainage Areas 262-2 34 32 Pad 266 261-3 881 262-3 263-28 20 263-2 Pad 268 • 267 is the next pad in ad 263 104W Pilot 264 264-2 the queue. 22 • 268 is on hold pending Pad 104 103 further review. Surmont Pad 265 Regional 101N Residence • 104 is second in the 264-3 Pad 267 15 1015 S1 CPF • Third pad in queue: 83-7W4 83-6W4 267-3 Looking at near-CPF S2 CPF 102N ad 102 102S 2 0 4 1 Kilometers

ConocoPhillips



queue.

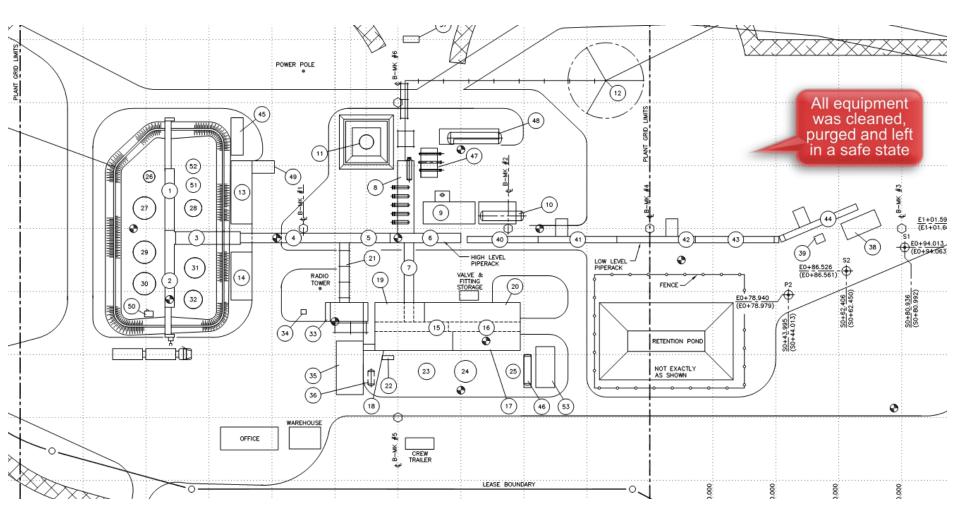
options.



Surface Operations and Compliance Pilot Project Approval 9460

Facilities Subsection 3.1.2 (1)

Site Survey Plan & Facility Modifications





Facility Performance

Subsection 3.1.2 (2)

Pilot Plant Performance Bitumen Production



- Thief zone interaction limiting production
- Cease of production on May 5th

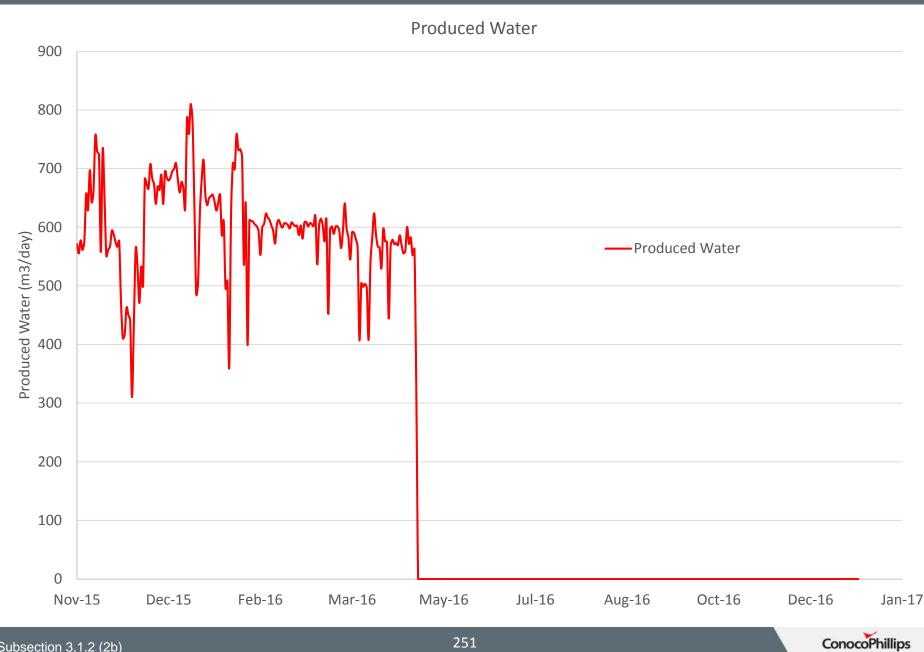
2015 Production = ~352 bbls/day

2016 Production = \sim 163.5 bbls/day

Production Jan – May 2016 = 375.4 bbls/d

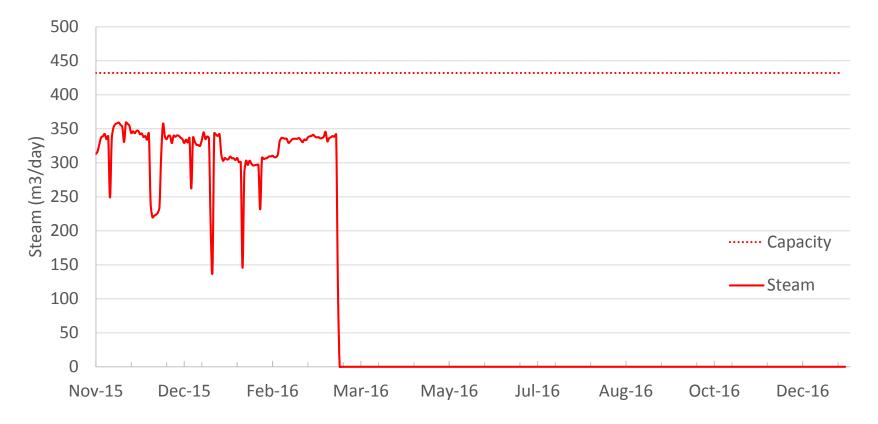


Pilot Plant Performance Produced Water



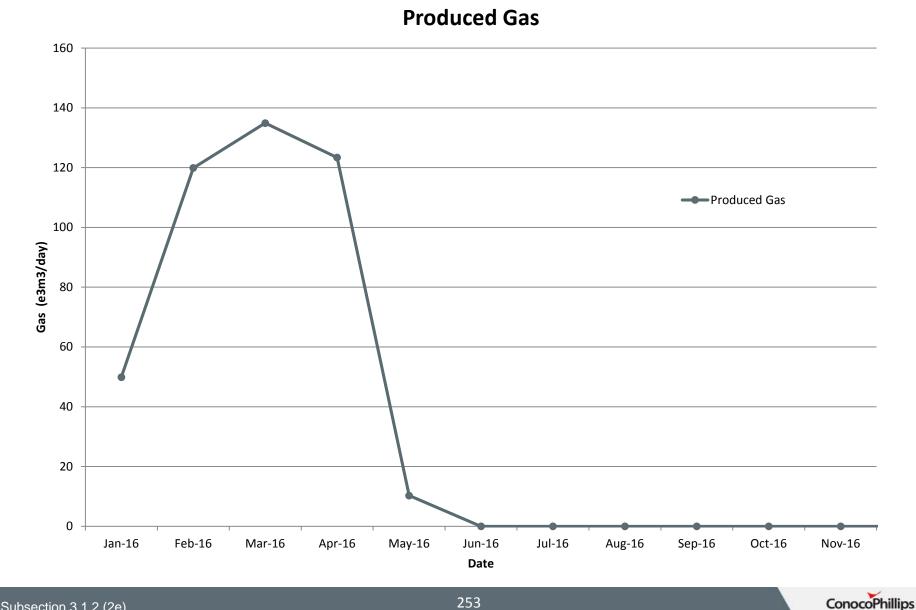
Pilot Plant Performance Steam Generation

Steam Injection



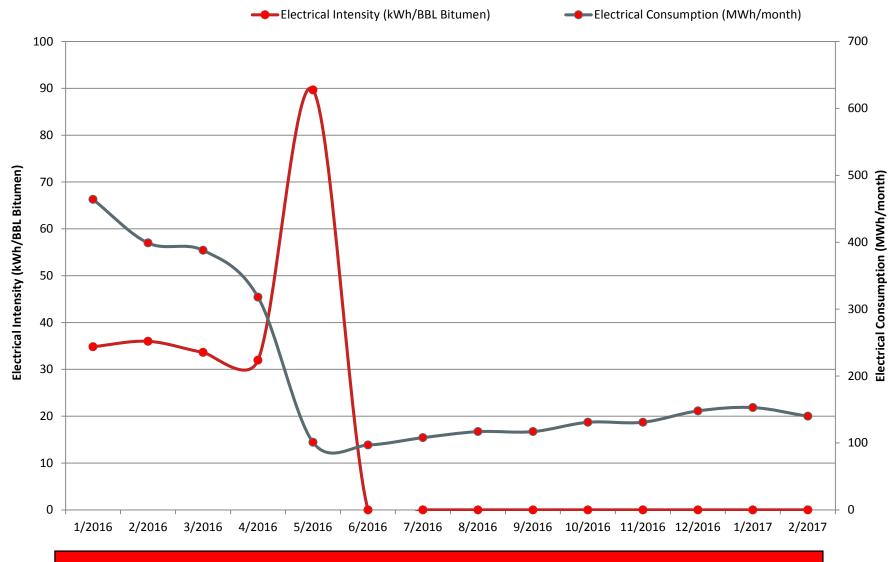
- Steam injection ceased on March 17th, 2016
- Blowdown monitoring began

Pilot Plant Performance Produced Gas



Subsection 3.1.2 (2e)

Facility Performance: Electricity Consumption Surmont Pilot



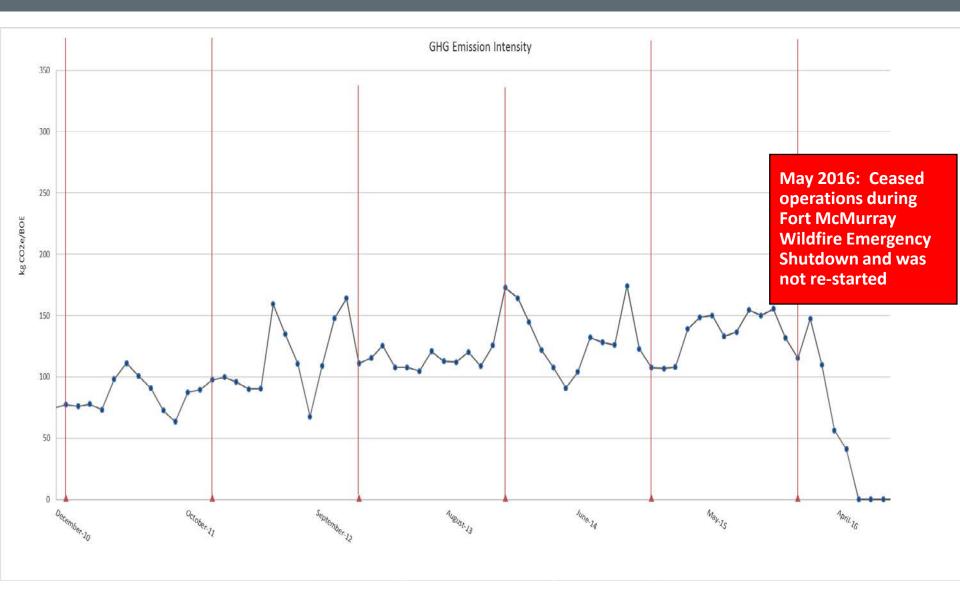
Pilot ceased operations in May due to Fort McMurray Wildfire.

Pilot Plant Performance: Gas Usage

	TCPL Gas Imports (10 ³ m ³)	Produced Gas (10 ³ m ³)	Flared Gas (10 ³ m ³)	% of Produced Gas Recovery
2011	8,068.6	1,339.2	2.4	99.8%
2012	9,727.7	2,947.5	2.5	99.9%
2013	11,828.3	3,229.2	85.4	97.4%
2014	10,511.0	1,152.0	31.7	97.2%
2015	9,228.8	697.4	7.3	99.0%
2016	2,421.6	438.4	204.3	53.4%
2017	-	-	-	

Pilot Plant ceased operations in May 2016. Volume displacement due to decommissioning of the Plant extended to December 2016.

Pilot Plant Performance: Greenhouse Gas

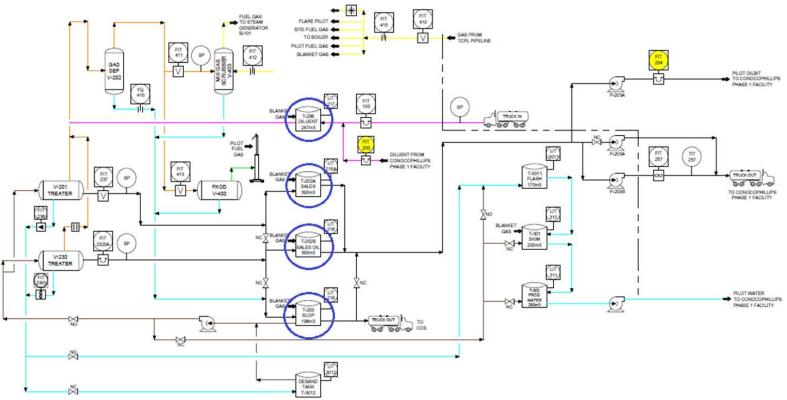




Measurement and Reporting

Subsection 3.1.2 (3)

Bitumen Measurement and Reporting



Battery Actual Bitumen Production:

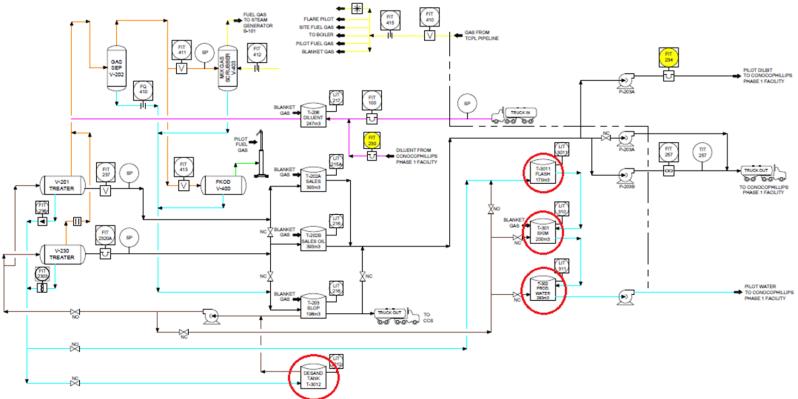
[Closing Inventories – Opening Inventories (Oil portion of Sales and Slop)]/Shrinkage Factor – Diluent Received + [Closing Inventories – Opening Inventories (Diluent)] + [Closing – Opening (Injected Fluids into Producers)] + Sales Shipped to S1 and Trucked Battery Estimated Bitumen Production:

Well bitumen production is calculated from well tests (pro-rated battery)

No changes to accounting formula



Produced Water Measurement and Reporting



Water Production:

[Closing inventories – Opening Inventories (Water portion of Sales, Slop, Flash, Skim and Produced Water)] – Water Content of Received Diluent or Oil + [Closing – Opening (Injected Fluids into Producers)] + Produced Water + Produced Water Truck Tickets + Water Content of Sales Oil **Battery Estimated Water Production:**

Well water production is calculated from well tests (pro-rated battery)

No changes to accounting formula



Measurement and Reporting Methods

Production Gas

- Total battery gas production estimated from inlet of FKOD, Scrubber and P3 usage.
- Well gas production calculated from well oil production and GOR.
- GOR = battery gas production / battery bitumen production.
- Gas proration factor = total battery gas production / well test gas production.

Steam

 Steam injection metered individually at each well and allocated using the group steam injection meter.

Well Testing

- One well on test at a time.
- Target a minimum of two tests per well per month (24 hours in length).
- All well pairs tests regularly tested to meet minimum monthly target.

No changes to accounting formula



2016 Surmont Pilot Plant Highlights and Changes

- Surmont Pilot Plant was operating until the Fort McMurray Wildfire Emergency Shutdown in May 2016.
- In June 2016, a decision was made not to restart the Plant.
- Pilot production volumes displaced continued to be reported until December 2016.

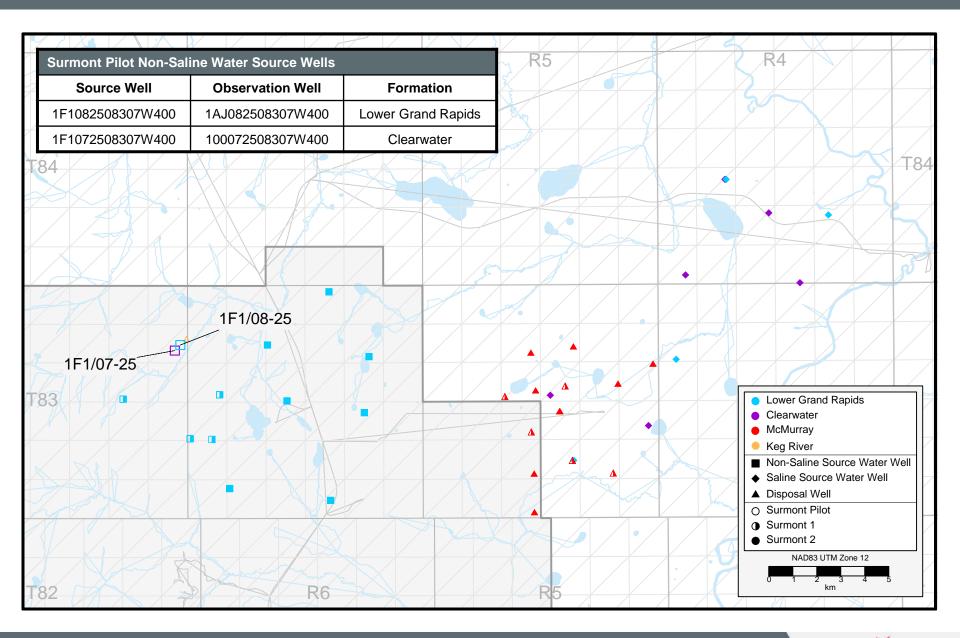




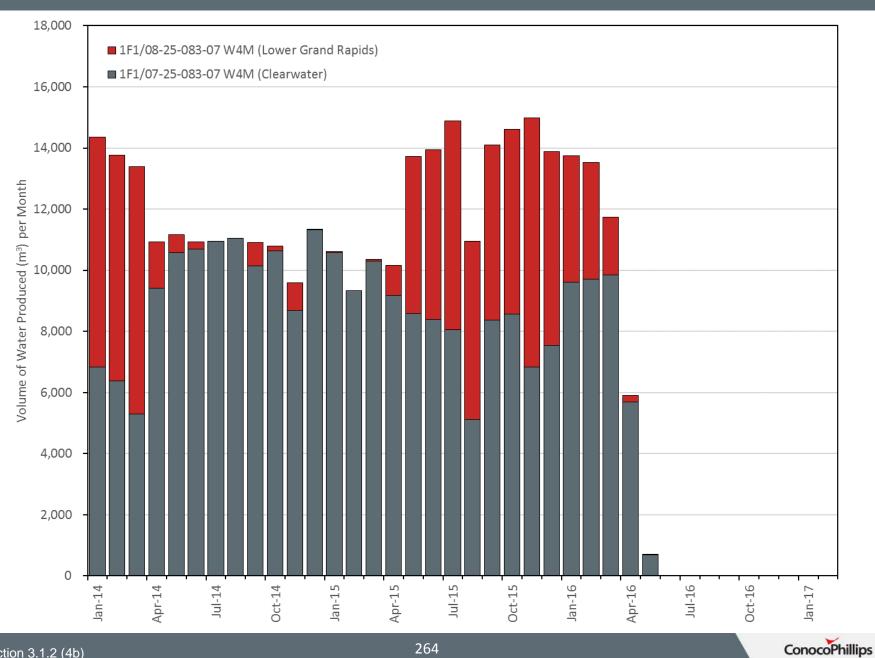
Water Production, Injection, and Uses

Subsection 3.1.2 (4)

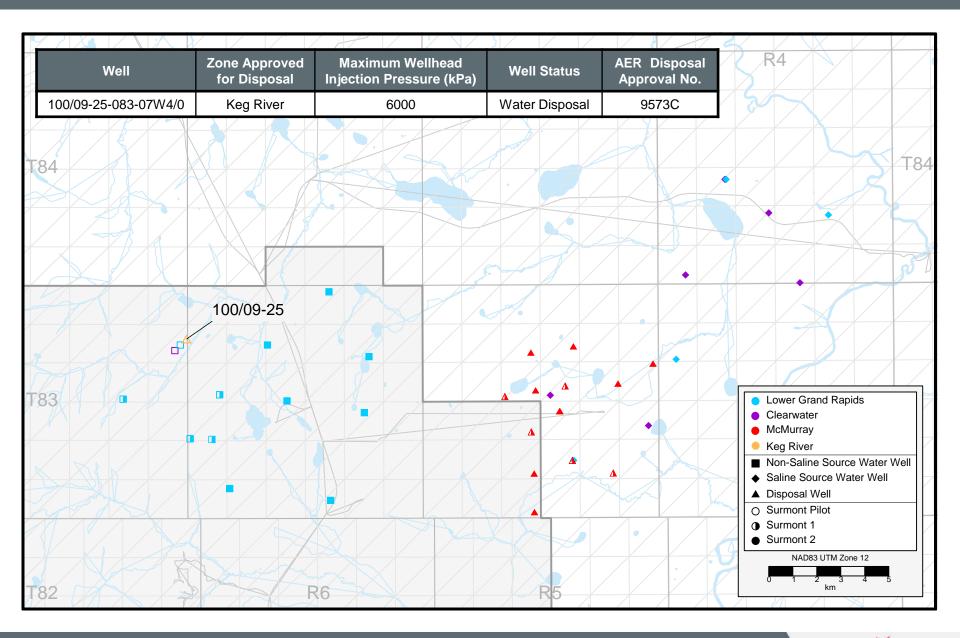
Surmont Pilot Non-Saline Water Source Wells



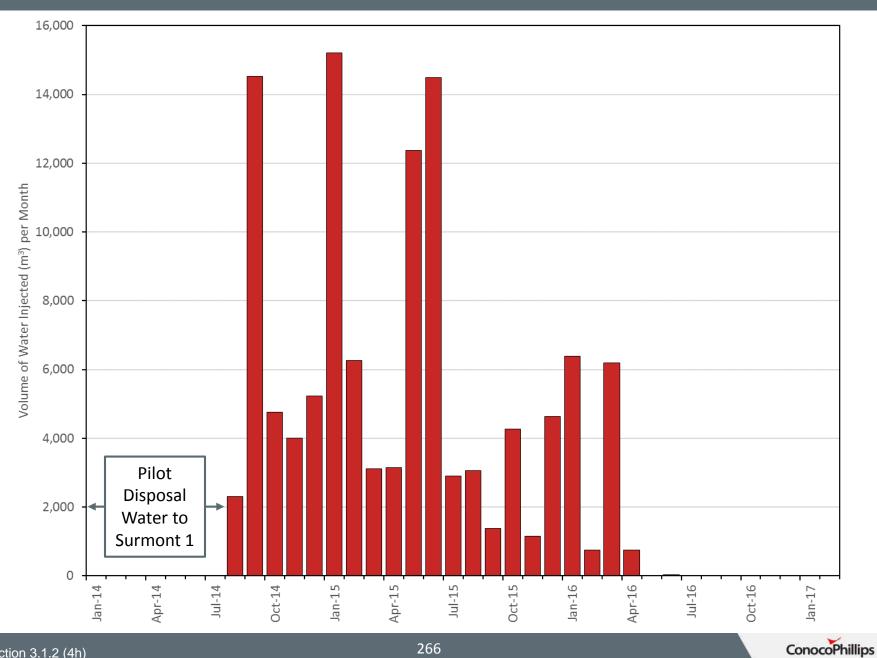
Pilot Water Source Wells Production Volumes



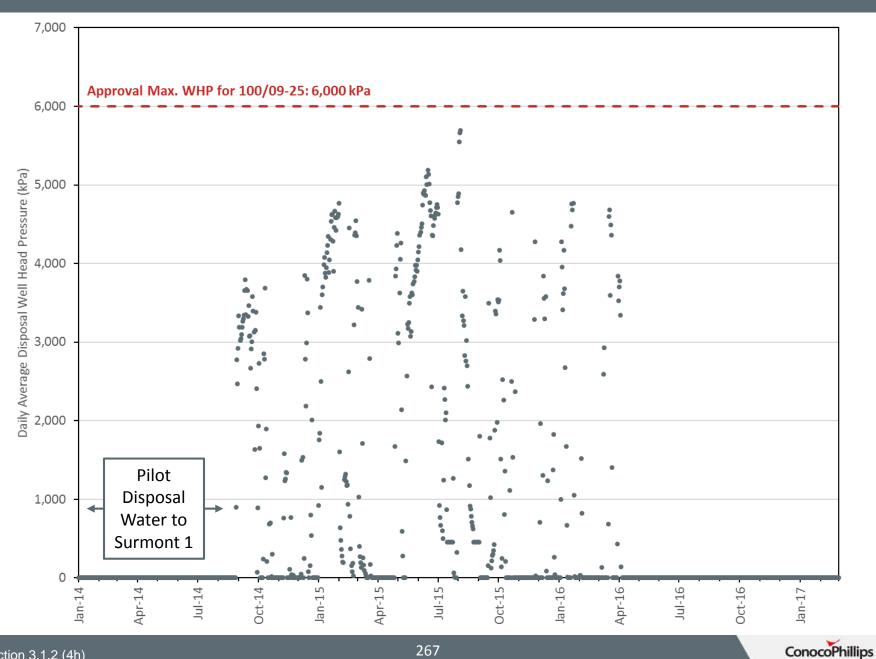
Surmont Pilot Water Disposal Well



Pilot Water Disposal Well 100/09-25-083-07 W4M Injection Rate (Keg River)



Pilot Water Disposal Well 100/09-25-083-07 W4M Well Head Pressure (Keg River)



Waste Disposal & Recycling

Solid Waste

Waste Description	Disposal Weight (kg)	Disposal Method
Recycled Materials	25	Recycled
Dangerous Oilfield Waste	4	Landfill
Non-Dangerous Oilfield Waste	25	Landfill

Fluid Waste

Waste Description	Disposal Volumes (m ³)	Disposal Method
Dangerous Oilfield Waste	208	Cavern
Non-Dangerous Oilfield Waste	1,039	Cavern

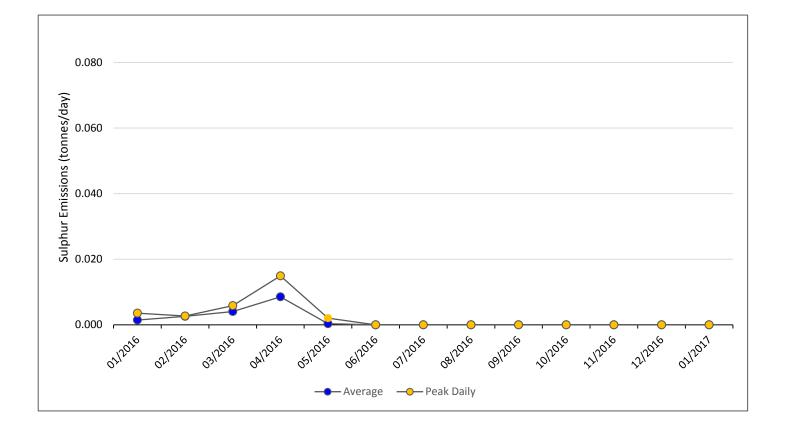




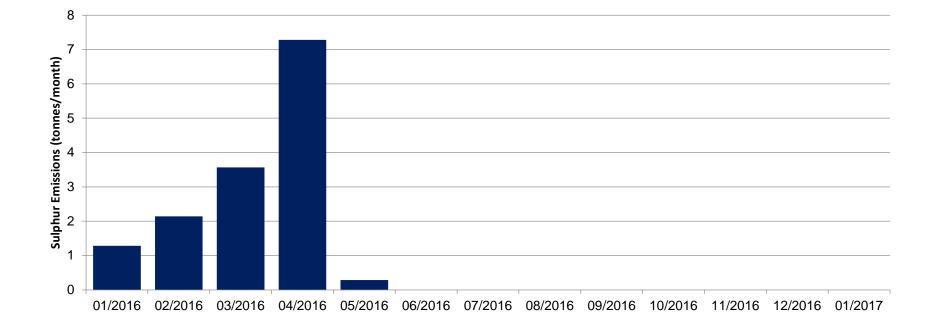
Sulphur Production

Subsection 3.1.2 (5)

Daily Sulphur Emissions



Monthly Sulphur Emissions

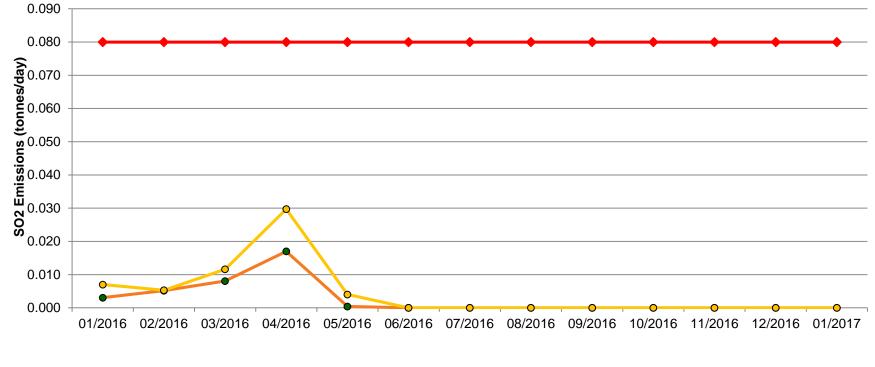






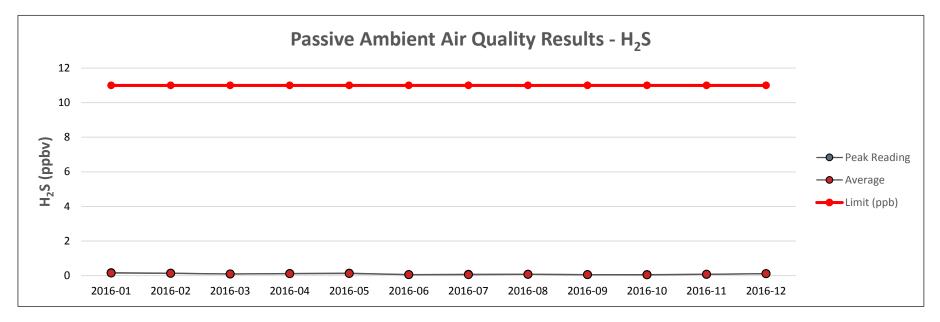


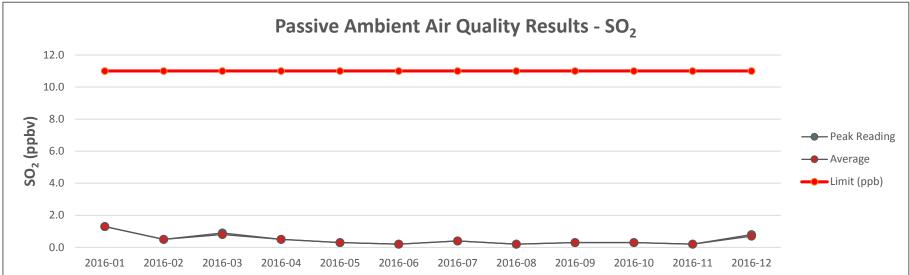
Daily SO₂ Emissions



---- Average ---- Peak Daily ----- Limit

Ambient Air Quality Monitoring









Environmental Compliance

Subsection 3.1.2 (6)

Environmental Compliance

Groundwater Monitoring

• 2016 results have changed from background in some wells. No changes have been observed in downstream surface water chemistry.

Soil Monitoring

• 2016 results within historical/background concentrations.

Reclamation Programs

• No reclamation in 2016





Compliance Confirmation and Non Compliances

Subsection 3.1.2 (7) + (8)

Compliance Confirmation and Non Compliances

ConocoPhillips Canada is in compliance in all areas of the regulations for 2016.

Flaring during Blowdown Phase

- D60 flaring variance application was submitted in March 2016.
- AER responded that an approval letter was not required to flare during blowdown phase.

Notification of Shut-in

- Originally we submitted a notification letter stating a June 15th shut-in.
- Following the wildfires in May, we submitted an update informing that the pilot would not start up post fire.





Future Plans

Subsection 3.1.2 (9)

Future Plans

- Suspension of the Pilot Plant was completed in November 2016 leaving the facility in a safe and secure state.
 - All pipelines were discontinued and have been purged, cleaned and blinded.
 - All 6 wells were downhole suspended.
- A Decommissioning and Land Reclamation Plan was submitted to the AER in December 2016 and approval is pending.
- Logging data will continue to be collected up to 2020.
- Decommissioning and Land Reclamation activities at the Pilot Plant are scheduled to begin in 2020.